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## NOMENCLATURES

Dimension are given in terms of mass(M), length(L) and time(T).

a	: Constant	
A	: Area	(L <sup>2</sup> )
c	: Constant	
C	: Constant	
C <sub>f</sub>	: Final concentration	(ML <sup>-3</sup> )
C <sub>o</sub>	: Initial concentration	(ML <sup>-3</sup> )
C <sub>S</sub>	: Saturation concentration	(ML <sup>-3</sup> )
$\bar{d}_p$	: Average particle diameter	(L)
d <sub>p</sub>	: Particle diameter	(L)
D <sub>a</sub>	: Impeller diameter	(L)
D <sub>AB</sub> , D <sub>V</sub>	: Diffusion coefficient	(L <sup>2</sup> T <sup>-1</sup> )
g	: Gravitational acceleration	(LT <sup>-2</sup> )
H	: Height of liquid in the vessel	(L)
k	: Mass transfer coefficient	(LT <sup>-1</sup> )
m <sub>1</sub> , m <sub>2</sub>	: Weight of α-naphthol pellets	(M)
ΔM	: α -naphthol weight lost during diffusion	(M)
M <sub>A</sub> , M <sub>B</sub>	: Molecular weight of species A and B	(M mole <sup>-1</sup> )
n	: Number of particles	
n <sub>c</sub>	: Number of baffled	



$n_p$	:	Number of blades of agitator	
$N$	:	Rotation speed	$(T^{-1})$
$N_c$	:	Critical speed of rotation	$(T^{-1})$
$p, q$	:	Exponents	
$P$	:	Power	$(ML^2T^{-3})$
$t$	:	Time	$(T)$
$T$	:	Tank diameter	$(L)$
$V$	:	Volume of liquid in the vessel	$(L^3)$
$V_\omega$	:	Velocity of fluid relative to impeller blade tip	$(LT^{-1})$
$V_c$	:	Fluid velocity leaving impeller periphery	$(LT^{-1})$
$V_r$	:	Radial component of fluid velocity	$(LT^{-1})$
$V_p$	:	Peripheral impeller velocity	$(LT^{-1})$
$\gamma$	:	Angle between the plane of an inclined impeller blade and the plane in which the impellers rotation	
$\beta$	:	Angle between the plane of an inclined impeller blade and the plane in which the impeller rotates.	
$\delta$	:	Film thickness	$(L)$
$\theta$	:	Temperature	$(\theta)$
$\mu$	:	Liquid viscosity	$ML^{-1}T^{-1}$
$\nu$	:	Kinematic viscosity	$(L^2T^{-1})$
$\rho_l$	:	Liquid density	$(ML^{-3})$
$\rho_s$	:	Solid density	$(ML^{-3})$
$\omega$	:	angular velocity	$(T^{-1})$

## Commonly used Dimensionless Groups

$Re_p$  : Reynolds number refer to solid particle ( $d_p \frac{T\omega\rho}{\mu}$ )

$Re_a$  : Reynolds number refer to agitator ( $D_a^2 \frac{\omega\rho}{\mu}$ )

$Re_T$  : Reynolds number refer to tank ( $T^2 \frac{\omega\rho}{\mu}$ )

$Sc$  : Schmidt number ( $\frac{\mu}{\rho_l D_v}$ )

$Sh_p$  : Sherwood number ( $\frac{kd_p}{D_v}$ )

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## APPENDIX 1

## DETERMINATION OF DENSITY

In this work the density of  $\alpha$ -naphthol is measured at room temperature ( $27^{\circ}\text{C}$ ) using water displacement principle, as follows : The dry empty pycnometer is weighed. Ten pellets of  $\alpha$ -naphthol of known weight are carefully dropped into the filled pycnometer and the water displacement of  $\alpha$ -naphthol pellets which over flowed from the pycnometer is wiped off using a clean towel. The final weight of the pycnometer with  $\alpha$ -naphthol pellets and water is determined. The density value can then be easily calculated, as follows

Weight of empty pycnometer, $m_1$	=	13.6151 g.
Weight of pycnometer + water, $m_2$	=	24.0421 g.
Weight of $\alpha$ -naphthol pellets, $m_3$	=	1.4345 g.
Weight of pycnometer + water + $\alpha$ -naphthol pellets, $m_4$	=	24.3519 g.
Density of water	=	1.0000 g/cc
Volume of $\alpha$ -naphthol measured by water displacement, $m_2 - (m_4 - m_3)$	=	1.1247 g.
Density of $\alpha$ -naphthol	=	$m/V$
	=	$1.4345/1.1247$
	=	1.2754 g/cc

The density value obtained from twenty experimental results of which the error is within  $\pm 0.005\%$

## APPENDIX 2

## DIMENSIONAL ANALYSIS OF MASS TRANSFER CORRELATION

In solid-liquid agitation the entire mass transfer relation can be expressed by five independent variables as follows :

$$k = f(d_p, \mu, \rho, D_V, \omega)$$

where  $D_V$  is the diffusion coefficient of a solid in liquid

$\omega$  is the rotation speed of the agitator.

$$\text{Let } k = C d_p^a \mu^b \rho^c D_V^d \omega^e$$

where  $C$  is a constant. The dimensions of each term may be expressed in term of Mass  $M$ , length  $L$ , and time  $T$  units.

Equate the exponents for mass, length and time, respectively, to give

$$(LT^{-1}) = (L)^a (ML^{-1}T^{-1})^b (ML^{-3})^c (L^2T^{-1})^d (T^{-1})^e$$

therefore,

$$M : 0 = b+c$$

$$L : 1 = a-b-3c+2d$$

$$T : -1 = -b-d-e$$

therefore

$$b = -c$$

$$d = 1-b-e$$

$$a = -1+2e$$



Express the  $k$  in term of the exponents derived above to give

$$k = C d_p^{(-1+2e)} \mu^{-c} \rho^c D_V^{(1+c-e)} \omega^e$$

therefore,

$$k = C d_p^{-1} D_V^{+1} \left( \frac{d_p^2 \omega \rho}{\mu} \right)^e \left( \frac{\mu}{D_V} \right)^e \left( \frac{\rho D_V}{\mu} \right)^c$$

Rearrange the term to give

$$\frac{k d_p}{D_V} = C \left( \frac{d_p^2 \omega \rho}{\mu} \right)^e \left( \frac{\mu}{\rho D_V} \right)^{e-c}$$

Let  $p = e$ ,  $q = e-c$ , and rewrite equation as

$$\frac{k d_p}{D_V} = C \left( \frac{d_p^2 \omega \rho}{\mu} \right)^p \left( \frac{\mu}{\rho D_V} \right)^q$$

therefore,

$$Sh = f(Re_p, Sc)$$

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