# VERTICAL TWO-PHASE FLOW UNDER THE INFLUENCE OF DIAMETER SIZES AND BENZALKONIUM CHLORIDE SURFACTANTS

Supachai Chootongchai

A Thesis Submitted in Partial Fulfilment of the Requirements
for the Degree of Master of Science

The Petroleum and Petrochemical College, Chulalongkorn University
in Academic Partnership with

The University of Michigan, The University of Oklahoma,
Case Western Reserve University and Institut Français du Pétrole
2007

Thesis Title:

Vertical Two-Phase Flow under the Influence of Diameter

Sizes and Benzalkonium Chloride Surfactants

By:

Mr. Supachai Chootongchai

Program:

Petroleum Technology

Thesis Advisors:

Assoc. Prof. Anuvat Sirivat

Prof. James. O. Wilkes

Accepted by the Petroleum and Petrochemical College, Chulalongkorn University, in partial fulfilment of the requirements for the Degree of Master of Science.

Nantaya Yanumut College Director

(Assoc. Prof. Nantaya Yanumet)

**Thesis Committee:** 

(Assoc. Prof. Anuvat Sirivat)

James Q. Wilkes

Kitipat Siemanord

Pramoch 3

AnivalServis

(Prof. James O. Wilkes)

(Asst. Prof. Kitipat Siemanond)

(Assoc. Prof. Pramoch Rangsunvigit)

#### ABSTRACT

4873015063: Petroleum Technology Program

Supachai Chootongchai: Vertical Two-Phase Flow under the

Influence of Diameter Sizes and Benzalkonium Chloride Surfactants.

Thesis Advisors: Assoc. Prof. Anuvat Sirivat and Prof. James

O. Wilkes 533 pp.

Keywords: Vertical two-phase flow regimes/ Diameter sizes/ Tail length of

surfactants/ Surface tension/ Pressure gradient/ Bubble size/ Bubble

or slug velocity/ Reynolds number

The effects of pipe diameter size and surfactant additive on the two-phase gas/liquid flows regimes, pressure gradients, bubble sizes and velocities were investigated. Experiment were carried out using three vertical transparent tubes with inner diameters of 10.75, 19, and 53.15 mm and the length of 3 m. Water, octylbenzyldimethylammonium chloride solutions (C<sub>8</sub>H<sub>17</sub>-C<sub>9</sub>H<sub>13</sub>NCl) and hexadecylbenzyldimethylammonium chloride solution (C16H33-C9H13NCl) were used as the working fluids. The boundaries of the flow regimes for a given Rewater increase nonlinearly with increasing tube diameter. Adding the surfactant lowers the critical air Reynolds numbers for the bubble-slug flow and the slug flow regimes. The friction factors or the dimensionless pressure gradients are distinctively different depending on diameter and type of liquids used (water, (C<sub>8</sub>H<sub>17</sub>-C<sub>9</sub>H<sub>13</sub>NCl) and (C<sub>16</sub>H<sub>33</sub>-C<sub>9</sub>H<sub>13</sub>NCl)). The normalized bubble or slug dimension for pipe diameter of 10.75 mm is always greater than those of the pipe diameter of 19 mm and 53.15 mm at any Reair and Rewater. The normalized bubble or slug dimension for pure water is greater than those of (C<sub>8</sub>H<sub>17</sub>-C<sub>9</sub>H<sub>13</sub>NCl) solution and (C<sub>16</sub>H<sub>33</sub>-C<sub>9</sub>H<sub>13</sub>NCl) solution. The normalized bubble and slug velocities of pipe diameter 10.75 are always greater than those of pipe diameters of 19 mm and 53.15 mm. The normalized bubble and slug velocity for pure water is lower than those of (C<sub>8</sub>H<sub>17</sub>-C<sub>9</sub>H<sub>13</sub>NCl) solution and (C<sub>16</sub>H<sub>33</sub>-C<sub>9</sub>H<sub>13</sub>NCl) solution due to surface tension effect.

## บทคัดย่อ

ศุภชัย ชูธงชัย: ขอบเขตของการ ใหลในแนวคิ่งแบบสองเฟส ภายใต้อิทธิพลของความ แตกต่างของขนาดท่อ และสารลดแรงตึงผิว benzalkonium chloride (Vertical Two-Phase Flow under the Influence of Diameter Sizes and Benzalkonium Chloride Surfactants) อ.ที่ปรึกษา: รศ.คร. อนุวัฒน์ ศิริวัฒน์ และ ศ. เจมส์ โอวิลค์ 533 หน้า

อิทธิพลของขนาดท่อและสารลดแรงตึงผิวที่เติมลงไปในระบบการไหลแบบสองเฟสใน ท่อแนวคิ่ง ได้ถูกนำมาศึกษาหาความแตกต่างของ ความคัน ขนาดของฟองอากาศ และความเร็ว ของฟองอากาศ อุปกรณ์ในการทคลองประกอบด้วยท่อใส 3 ขนาด (ขนาค 10.75 มิลลิเมตร, ขนาด 19 มิลลิเมตร และ ขนาด 53.15 มิลลิเมตร) ความยาวของท่อทั้งสาม คือ 3 เมตร น้ำ, สารละลาย octylbenzyldimethylammonium chloride และ สารละลาย hexadecylbenzyldimethyl ammonium chloride ถูกใช้เป็นของไหลในการศึกษา ขอบเขตการไหลของน้ำ เพิ่มขึ้นเมื่อเพิ่มขนาคของท่อ และเมื่อใส่สารลคแรงตึงผิว ขอบเขตการไหลจะลคลงในช่วง การ ใหลแบบฟองอากาศและแบบกระสุน เมื่อความคันถูก normalized แล้วก็จะสามารถนำมา เปรียบเทียบอิทธิพลของขนาคท่อและสารลดแรงตึงผิวได้ โดยจะพบว่าความคันที่แตกต่างกันนั้น เป็นเพราะ ขนาดของฟองอากาศ, Eotvos number และ property parameter, Y เมื่อทำการ normalized ขนาคของฟองอากาศแล้วจะพบว่า ขนาคของฟองอากาศของน้ำจะใหญ่กว่าของสาร ลดแรงตึงผิว (C<sub>8</sub>H<sub>17</sub>-C<sub>9</sub>H<sub>13</sub>NCl) และ (C<sub>16</sub>H<sub>33</sub>-C<sub>9</sub>H<sub>13</sub>NCl) เพราะว่าสารลดแรงตึงผิวสามารถ ชะลอการรวมตัวของฟองอากาศได้ เมื่อ normalized ความเร็วของฟองอากาศจะพบว่าความเร็ว ของฟองอากาศในท่อขนาด 10.75 มิลลิเมตรจะเร็วว่าท่อ 19 มิลลิเมตร และท่อ 53.15 มิลลิเมตร เสมอ และพบอีกว่า ความเร็วฟองอากาศของน้ำจะช้ำกว่าความเร็วฟองอากาศของ สารลดแรงตึง ผิว (C8H17-C9H13NCl) และ (C16H33-C9H13NCl)

#### ACKNOWLEDGEMENTS

This thesis work is funded by the Petroleum and Petrochemical College; and the National Excellence Center for Petroleum, Petrochemicals, and Advanced Materials, Thailand.

First of all, I am very grateful to Assoc. Prof. Anuvat Sirivat and Prof. James O. Wilkes for entrusting with this challenging topic, supporting my work over the year, and especially giving me the uncountable things beyond their duty as well as providing the financial.

I would like to give my thankfulness to Assoc. Prof. Pramoch Rangsunvigit and Asst. Prof. Kitipat Siemanond who are my thesis committee for their well-intentioned suggestions and comments is greatly acknowledged. And also, unforgettable thanks are forwarded to Mr. Tanabordee Duangprasert and Ph.D students of the Petroleum and Petrochemical College, who gave me a lot of helpful advice and technical knowledge.

I wish to extend my thanks to K.Panarut Ratanapruksakul (Assistant Manager Sale & Marketing 2 Chemicals Business Kao Industrial (Thailand) Co.,Ltd) who supported surfactants for this research.

And above all, my greatest debt of gratitude lines with all the members in my family who have filled my life with daily love and endless encouragement, making the frustration from my extended research effort easier to handle. And vice versa, it is surely my family who are most grateful that this research work is finally completed.

## TABLE OF CONTENTS

		PAGE
Title	Page	i
Abst	tract (in English)	iii
Abst	tract (in Thai)	iv
Ack	nowledgements	v
Tabl	e of Contents	vi
List	of Tables	xi
List	of Figures	xii
СНАРТЕ	R	
I	INTRODUCTION	1
П	BACKGROUND AND LITERATURE SURVEY	3
	2.1 Theoretical Background	3
	2.1.1 Determination of Flow Regime	5
	2.1.2 Bubble Flow Regime	6
	2.1.3 Slug Flow Regime	8
	2.1.4 Churn or Froth Flow Regime	14
	2.1.5 Annular-Mist Flow Regime	14
	2.2 Literature Survey	16
Ш	EXPERIMENTAL	22
	3.1 Materials Preparation	22
	3.2 Experimental Apparatus	22
	3.2.1 Design and Experimental Setup of	
	Two-Phase Flow	22
	3.3 Methodology	25

CHAPTE	2		PAGI
	3.3.1 Parameters		25
	3.3.1.1 Co	entrolled Parameters of	
	Tv	vo-Phase Flow	25
	3.3.1.2 Va	riable Parameters of	
	Tv	vo-Phase Flow	25
	3.3.1.3 M	easured Parameters of	
	Tv	vo-Phase Flow	26
	3.3.2 Experimen	ntal Procedures	26
	3.3.2.1 De	etermination the Density of	
	Sc	lution by using Syringe (SGE,	
	Au	ustralia)	26
	3.3.2.2 De	etermination the Viscosity of	
	Sc	lution by Cannon-Ubbelohde	
	Vi	scometer	27
	3.3.2.3 De	etermination of Pressure Drops	
	in	the Column	28
	3.3.2.4 De	etermination of Bubble and	
	SI	ug Size in The Column	28
	3.3.2.5 De	etermination of Bubble and Slug	
	Ve	elocity in the Column	28
IV	VERTICAL TWO-P	PHASE FLOW REGIMES	
	AND PRESSURE G	RADIENTS UNDER THE	
	INFLUENCE OF DI	AMETER SIZES	29
	4.1 Abstract		29
	4.2 Introduction		30
	4.3 Experimental App	paratus	32
	4.4 Results and Discu	ssion	33
	4.5 Conclusions		37
	4.6 Acknowledgemen	nts	38

HAPTER		PAGE	
		4.7 References	38
,	v	VERTICAL TWO-PHASE FLOW REGIMES	
		AND PRESSURE GRADIENTS UNDER THE	
		INFLUENCE OF BENZALKONIUM	
		CHLORIDE SURFACTANTS	58
		5.1 Abstract	58
		5.2 Introduction	59
		5.3 Experimental Apparatus	61
		5.4 Results and Discussion	62
		5.5 Conclusions	72
		5.6 Acknowledgements	73
		5.7 References	74
	VI	CONCLUSIONS	97
		REFERENCES	99
		APPENDICES	101
		Appendix A Water-Air Flow for the Pipe Diameter	
		of 19 mm	101
		Appendix B Water-Air Flow for the Pipe Diameter	
		of 53.15 mm	152
		Appendix C Water-Air Flow for the Pipe diameter	
		of 10.75 mm	198
		Appendix D Comparison the Experimental Data	
		Between Pipe Diameter of 10.75 mm,	
		19 mm and 53.15 mm	246
		Appendix E Physical Properties of	
		Octylbenzyldimethylammonium	

CHAPTER		PAGE
	Chloride Surfactant	
	$(C_8H_{17}-N^+(CH_3)_2-CH_2-C_6H_5C\Gamma)$	298
	Appendix F Physical Properties of	
	Dodecylbenzyldimethylammonium	
	Chloride Surfactant	
	$(C_{12}H_{25}-N^{+}(CH_{3})_{2}-CH_{2}-C_{6}H_{5}C\Gamma)$	309
	Appendix G Physical Properties of	
	Hexadecylbenzyldimethylammonium	
	Chloride Surfactant	
	$(C_{16}H_{33}-N^{+}(CH_{3})_{2}-CH_{2}-C_{6}H_{5}C\Gamma)$	320
	Appendix H Octylbenzyldimethylammonium Chloride	
	Surfactant (1CMC) - Air Flow for the	
	Pipe Diameter of 19 mm	331
	Appendix I Octylbenzyldimethylammonium Chloride	
	Surfactant (2CMC) - Air Flow for the	
	Pipe Diameter of 19 mm	388
	Appendix J Octylbenzyldimethylammonium Chloride	
	Surfactant (3CMC) – Air Flow for the	
	Pipe Diameter of 19 mm	419
	Appendix K Hexadecylbenzyldimethylammonium	
	Chloride Surfactant (1CMC) - Air Flow	
	for the Pipe Diameter of 19 mm	450
	Appendix L Comparison the Experimental Data of	
	Octylbenzyldimethylammonium Chloride	
	Solution (1, 2 and 3 CMC) by Using the	
	Pipe Diameter of 19 mm	481
	Appendix M Comparison the Experimental Data of	
	Octylbenzyldimethylammonium	
	Chloride Solution (1CMC) and	
	Hexadecylbenzyldimethylammonium	

CHAPTER	PAG
Chloride S	olution (1CMC) by Using
the Pipe D	ameter of 19 mm 509
CURRICULUM VITAI	53

# LIST OF TABLES

TABL	E	PAG
	CHAPTER II	
2.1	Model variables for Sylvester theory	11
	CHAPTER III	
3.1	Physical properties of the gas and the liquids used in the	
J.1	experiment	25
	CHAPTER IV	
4.1	Physical properties of the gas and the liquid used in the	41
4.2	The critical Reynolds numbers (Reair)critical of various	
7.2	regimes of 3 pipe diameters: 10.75, 19, and 53.15 mm	42
	CHAPTER V	
5.1	Physical properties of the gas and the liquids used in the	
	experiment	77
5.2	The critical Reynolds numbers (Reair)critical of various	
	regimes of octylbenzyldimethylammonium chloride	
	solution (1CMC)	78
5.3	The critical Reynolds numbers (Reair)critical of various	
	regimes by using water and octylbenzyldimethyl-	
	ammonium chloride solution (1, 2 and 3 CMC)	79
5.4	And the second s	
	regimes by using octylbenzyldimethylammonium chloride	
	solution (1 CMC) hexadecylbenzyldimethylammonium	00
	chloride solution (1 CMC)	80

## LIST OF FIGURES

F	IGUR	EE.	PAGE
		CHAPTER II	
	2.1	Modeling flow pattern transitions for steady upward gas-	
		liquid flow in vertical tube.	4
	2.2	Two-phase flow regimes in a vertical tube.	4
	2.3	Bubble flow.	6
	2.4	Two-phase slug flow in a vertical pipe.	8
	2.5	Slug unit.	10
	2.6	Vertical annular two-phase flow.	15
		CHAPTER III	
	3.1	Schematic diagram of the experimental setup.	24
	3.2	Schematic diagram of Cannon-Ubbelohde viscometer.	27
		CHAPTER IV	
	4.1	Schematic diagram of the experimental apparatus.	43
	4.2	Effect of pipe diameter on dynamic pressure gradient: a)	
		$Re_{water} = 0$ ; b) $Re_{water} = 1079$ , 1010 and 1028; c) $Re_{water} =$	
		2727 and 2740.	45
	4.3	Effect of pipe diameter on dimensionless pressure	
		gradient: a) $Re_{water} = 1079$ , 1010 and 1028; b) $Re_{water} =$	
		2727 and 2740.	47
	4.4	Photographs of bubbles in the bubble flow regime at	
		Rewater = 0: a) Reair = 3.41, pipe diameter of 10.75 mm, Eo	
		= 15.83; b) $Re_{air}$ = 3.17, pipe diameter of 19 mm, Eo =	
		49.44; c) $Re_{air} = 2.9$ , pipe diameter of 53.15 mm, Eo =	
		387.	49

TIGURE		
4.5	Effect of pipe diameter on bubble width: a) Re <sub>water</sub> = 0; b)	
1.5	$Re_{water} = 1079$ , 1010 and 1028; c) $Re_{water} = 2727$ and 2740.	51
4.6	Effect of pipe diameter on bubble height: a) Re <sub>water</sub> = 0; b)	
	$Re_{water} = 1079$ , 1010 and 1028; c) $Re_{water} = 2727$ and 2740.	53
4.7	Effect of pipe diameter on slug height: a) Re <sub>water</sub> = 0; b)	
	$Re_{water} = 1079$ , 1010 and 1028; c) $Re_{water} = 2727$ and 2740.	55
4.8	Effect of pipe diameter on bubble or slug velocity: a)	
	$Re_{water} = 0$ ; b) $Re_{water} = 1079$ , 1010 and 1028; c) $Re_{water} =$	
	2727 and 2740.	57
	CHAPTER V	
5.1	Schematic diagram of the experimental apparatus.	81
5.2	Dynamic pressure gradient vs. air Reynolds number: a)	
	Effect of $Re_{liquid}$ = 0, 1001 and 2749, Eo = 115, Y	
	=3.06×10 <sup>-10</sup> ; b) Effect of concentration, Re <sub>liquid</sub> = 2749,	
	2731, 2735 and 2740; c) Tail length effect, Reliquid= 2749,	
	2741 and 2740.	83
5.3	Dimensionless pressure gradient vs. air Reynolds number:	
	a) Effect of $Re_{liquid}$ = 1001 and 2749, Eo = 115, Y	
	=3.06×10 <sup>-10</sup> ; b) Effect of concentration, Re <sub>liquid</sub> = 2749,	
	2731, 2735 and 2740; c) Tail length effect, Reliquid= 2749,	
	2741 and 2740.	85
5.4	Photographs of bubbles in the bubble flow regime: a)	
	Octylbenzyldimethylammonium chloride (1CMC), Reair =	
	28.08, $Re_{liquid} = 2749$ , Eo = 115, Y = 3.06×10 <sup>-10</sup> ; b)	
	Octylbenzyldimethylammonium chloride (2CMC), Reair =	
	28.08, Re <sub>liquid</sub> = 2731, Eo = 104, Y = $5.06 \times 10^{-10}$ ; c)	
	Octylbenzyldimethylammonium chloride (3CMC), Reair =	
	28.08 Reviewed = 2735. For = 98.62, $Y = 6.42 \times 10^{-10}$ ; d)	

FIGUE	RE	PAGI
	Hexadecylbenzyldimethylammonium chloride (1CMC),	
	$Re_{air} = 28.08$ , $Re_{liquid} = 2741$ , Eo = 113, Y = 4.74×10 <sup>-10</sup> ; e)	
	Pure water, $Re_{air} = 28.08$ , $Re_{liquid} = 2740$ , $Eo = 49.44$ , $Y =$	
	1.41×10 <sup>-11</sup> .	88
5.5	Bubble width vs. air Reynolds number: a) Effect of	
	Re <sub>liquid</sub> = 0, 1001 and 2749, Eo = 115, Y = $3.06 \times 10^{-10}$ ; b)	
	Effect of concentration, Reliquid= 2749, 2731, 2735 and	
	2740; c) Tail length effect, Reliquid = 2749, 2741 and 2740.	90
5.6	Bubble height vs. air Reynolds number: a) Effect of	
	Re <sub>liquid</sub> = 0, 1001 and 2749, Eo = 115, Y = $3.06 \times 10^{-10}$ ; b)	
	Effect of concentration, Reliquid= 2749, 2731, 2735 and	
	2740; c) Tail length effect, Reliquid= 2749, 2741 and 2740.	92
5.7	Slug height vs. air Reynolds number: a) Effect of Reliquid=	
	0, 1001 and 2749, Eo = 115, Y = $3.06 \times 10^{-10}$ ; b) Effect of	
	concentration, Reliquid= 2749, 2731, 2735 and 2740; c) Tail	
	length effect, Reliquid= 2749, 2741 and 2740.	94
5.8	Bubble or slug velocity vs. air Reynolds number: a) Effect	4.
	of Re <sub>liquid</sub> = 0, 1001 and 2749, Eo = 115, Y = $3.06 \times 10^{-10}$ ;	
	b) Effect of concentration, Re <sub>liquid</sub> = 2749, 2731, 2735 and	
	2740; c) Tail length effect, Re <sub>liquid</sub> = 2749, 2741 and 2740.	96