

REFERENCES

- Al-Jibbouri, S., Ulrich, J. (2002). The Growth and Dissolution of Sodium Chloride in a Fluidized Bed Crystallizer. Journal of Crystal Growth, 234, 237-246.
- Filippidis, A., Godelitsas, A., Charistos, D., Misaelides, P., Kassoli-Fournaraki, A. (1996). The Chemical Behavior of Natural Zeolites in Aqueous Environments: Interactions Between Low-Silica Zeolites and 1M NaCl Solutions of Different Initial pH-values. Applied Clay Science, 11, 199-209.
- Fogler, H.S. (1999). Elements of Chemical Reaction Engineering. 3rd edition, Prentice-Hall, Inc.
- Fredd, C.N. and Fogler, H.S. (1998). Alternative Stimulation Fluids and Their Impact on Carbonate Acidizing. SPE Journal, 34-41.
- Fredd, C.N. and Fogler, H.S. (1998). The Kinetics of Calcite Dissolution in Acetic Acid Solutions. Chemical Engineering Science, 53(22), 3863-3874.
- Gallup, D. L. (1997). Aluminum Silicate Scale Formation and Inhibition: Scale Characterization and Laboratory Experiments. Geothermics, 26, 483-499.
- Gdanski, R. and Shuchart, C.E. (1995). Newly discovered equilibrium controls HF stoichiometry. Society of Petroleum Engineers, SPE 30456.
- Gdanski, R. (1998). Kinetics of the Tertiary Reactions of HF on Alumino - Silicates. SPE Production & Facilities, 13(2), 75-80.
- Gdanski, R. (1999). Formation Mineral Content Key to Successful Sandstone Acidizing. Oil & Gas Journal, 97(35), 90-95.
- Gdanski, R. (2000). Kinetics of the Secondary Reactions of HF on Alumino - Silicates. SPE Production & Facilities, 14(4), 260-268.
- Gdanski, R. (2000). Kinetics of the Primary Reactions of HF on Alumino - Silicates. SPE Production & Facilities, 15(4), 279-287.
- Golan, M. and Whitson C.H. (1991). Well Performance. 2nd ed. Engle Cliffs, New Jersey: Prentice Hall.
- Kanzaki, N., Onuma, K., Treboux, G., Ito, A. (2002). Dissolution Kinetics of Dicalcium Phosphate Dihydrate under Pseudophysiological Conditions. Journal of Crystal Growth, 235, 465-470.

- Karger, J., Ruthven, D.M. (1992). Diffusion in Zeolites and Other Microporous Solids, New York: John Wiley & Sons, Inc.
- Kline, W.E. and Fogler, H.S. (1981). Dissolution Kinetics: the Nature of the Particle Attack of Layered Silicates in HF. Chemical Engineering Science. 36, 871-884.
- Lasaga, A.C., Luttage, A. (2001). Variation of Crystal Dissolution Rate Based on a Dissolution Stopware Model. Science, 291, 2400-2404.
- Marinovic, V., Despic, A.R. (1997). Hydrogen Evolution from Solutions of Citric Acids. Journal of Electroanalytical Chemistry. 431, 127-132.
- Murphy, W.M., Pabalan, R.T., Prikryl, J.D., Goulet, C.J. (1996). Reaction Kinetics and Thermodynamics of Aqueous Dissolution and Growth of Analcime and Na-Clinoptilolite at 25°C. American Journal of Science, 296, 128-186.
- Rogers, A., Burk, M.K., Stonecipher, S.A. (1998). Designing a Remedial Acid Treatment for Gulf of Mexico Deepwater Turbidite Sands Containing Zeolite Cement. Society of Petroleum Engineers, SPE 39595, 693-702.
- Schechter, R.S. (1992). Oil Well Stimulation. 1st ed. Engle Cliffs, New Jersey: Prentice Hall.
- Scheirs, J. and Kaminsky, W. (1999). Metallocence-based Polyolefins. 1st ed. New York: John Wiley & Sons.
- Shuchart, C. E. (1997). Chemical Study of Organic-HF Blends Leads to Improved Fluids. Society of Petroleum Engineers, SPE 37281, 675-678.
- Underdown, D.R., Hickey, J.J., and Kalra, S.K. (1990). Acidization of Analcime-Cemented Sandstone, Gulf of Mexico. SPE 20624, presented at the 65th Annual Technical Conference and Exhibition of the society of Petroleum Engineers, New Orleans, LA, 97-102.
- Wilkin, R.T., Barnes, H.L. (1998). Solubility and Stability of Zeolites in Aqueous Solution: I. Analcime, Na-, and K-Clinoptilolite. American Mineralogist, 83, 746-761.
- Wilkin, R.T., Barnes, H.L. (2000). Nucleation and Growth Kinetics of Analcime from Precursor Na-Clinoptilolite. American Mineralogist, 85, 1329-1341.
- Yamamoto, S., Sugiyama, S., Matsuoka, O., Kohmura, K., Honda, T., Banno, Y., Nozoye, H. (1996). Dissolution of Zeolite in Acidic and Alkaline Aqueous

Solutions as Revealed by AFM Imaging. Journal of Physical Chemistry, 100, 18474-18482.

Yokel, R.A. (2002). Aluminum Chelation Principles and Recent Advances. Coordination Chemistry Reviews, 228, 97-113.

APPENDICES

Appendix A Calculation of Facial Surface Area Equivalent Diameter and Specific Surface Area

1. Calculation of Facial Surface Equivalent Diameter

From the picture from Scanning Scanning Electron Microscope (SEM)

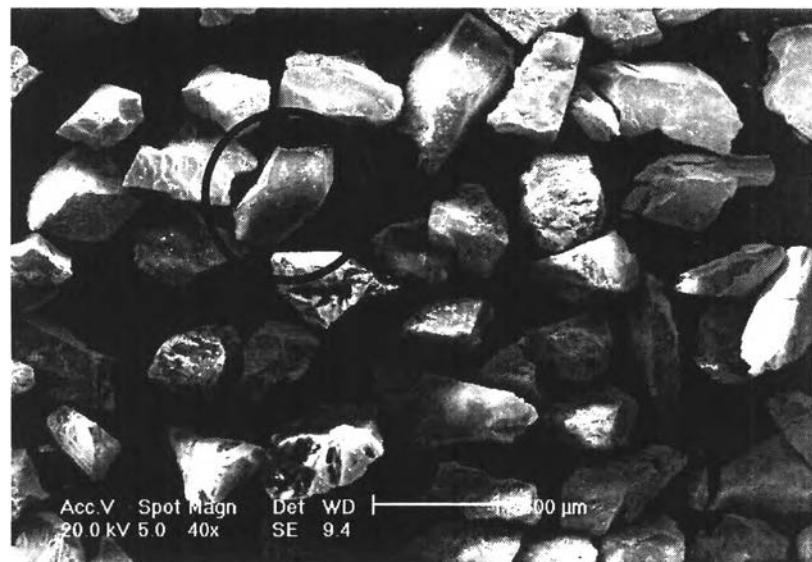


Figure A.1 Analcime particles in the size of 0.212-0.300 mm

Using ImageJ software program, the facial surface area of the labeled particle can be obtained.

$$\text{Facial surface area (Area)} = 183404.50 \mu\text{m}^2$$

The facial surface area equivalent diameter (D_e) is defined as:

$$D_e = \sqrt{\frac{\text{Area}}{\pi}} \quad (\text{A.1})$$

Therefore, the analcime particle with facial surface area of $183404.50 \mu\text{m}^2$ has D_c equal to $241.6184 \mu\text{m}$ or approximately 0.242 mm .

2. Calculation of Specific Surface Area

For analcime in the sieve size $0.71\text{-}1.18 \text{ mm}$,

$$\text{Average actual diameter } (D) = 0.6875 \text{ mm}$$

$$\text{Specific gravity of analcime } (\rho) = 2.26 \times 10^6 \text{ g/mm}^3$$

Assuming analcime particle is spherical,

$$\text{Volume per particle } (V) = \frac{4}{3}\pi r^3 = \frac{\pi D^3}{6} = 0.17 \text{ mm}^3$$

$$\text{Mass per particle } (M) = \rho V = 3.84 \text{ g}$$

$$\text{Surface area per particle} = 4\pi r^2 = \pi D^2 = 1.48 \text{ mm}^2$$

$$\begin{aligned} \text{Specific surface area} &= \text{Surface area per particle / Mass per particle} \\ &= 3.87 \times 10^6 \text{ mm}^2/\text{g} \end{aligned}$$

3. Calculation of ρ_s

$$\text{Amount of analcime } (W) = 1.00615 \text{ g}$$

$$\text{Density of analcime} = 2.255 \text{ g/cm}^3 = 2255 \text{ g/dm}^3$$

$$\text{Volume of analcime} = 4.462 \times 10^{-4} \text{ dm}^3$$

$$\text{Volume of citric acid solution} = 0.15 \text{ dm}^3$$

$$\text{Total volume in system } (V) = 15.0446 \times 10^{-2} \text{ dm}^3$$

$$\rho_s = \frac{W}{V} \quad (\text{A.2})$$

Therefore, ρ_s of 1.00615 g analcime in the size of $0.212\text{-}0.300 \text{ mm}$ is equal to $6.69 \text{ g analcime/ dm}^3$ total volume in system.

Appendix B Kinetics Analysis of Analcime Dissolution in Batch Experiments

Experimental Conditions:

Weight of analcime	= 1.0081 g
Size of analcime	= 0.212-0.300 mm
External surface area	= $1.60 \times 10^3 \text{ dm}^2/\text{g}$
ρ_s	= 6.69 g analcime/dm ³ of total volume
Citric acid concentration	= 0.1M
Volume of citric acid used	= 150 mL
Temperature	= 25°C
Stirring rate	= 250 rpm

The calibration curve of Al for Atomic absorption spectroscopy (AAS) is shown in Figure B.1.

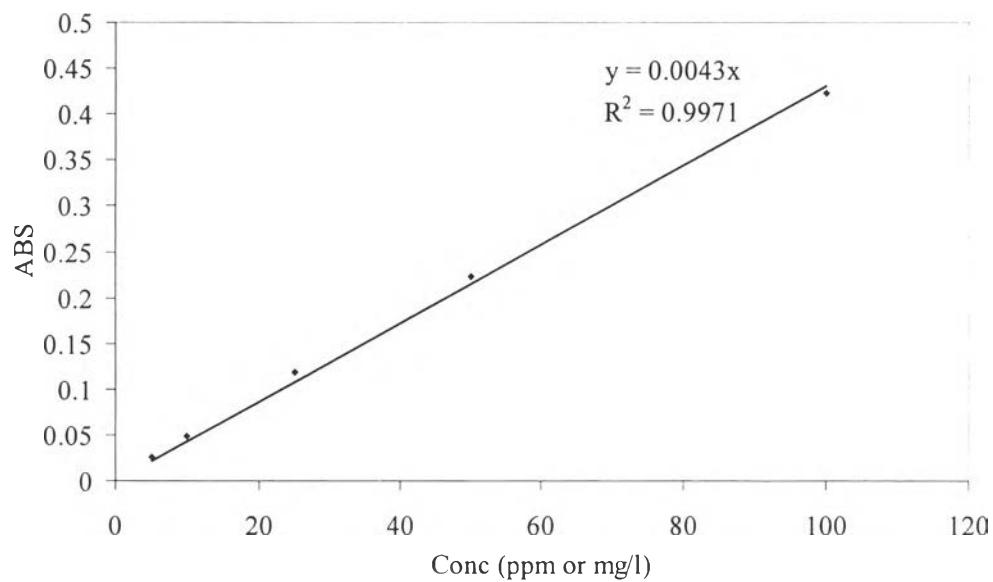


Figure B.1 Calibration curve of Al

Table B.1 Informatin of Al element in sample solution from dissolution experiment in slurry reactor (analcime initial particle size of 0.212-0.300 mm, 0.1M citric acid, 250 rpm, 25°C)

Time (hr)	ABS	Conc. Of Al		Volume of solution in reactor (l)	Al/intial analcime $\times 10^3$ (mole/g)	Al/surface area of intial analcime $\times 10^7$ (mole/dm ²)
		mg/l	mmole/dm ³			
0.000	-	-	-	0.150	-	-
0.017	0.004	3.72	0.1379	0.146	0.0206	0.129
0.033	0.005	4.65	0.1724	0.142	0.0258	0.161
0.050	0.007	6.51	0.2414	0.138	0.0361	0.226
0.067	0.009	8.37	0.3103	0.134	0.0464	0.290
0.083	0.011	10.23	0.3793	0.130	0.0567	0.354
0.100	0.013	12.09	0.4482	0.126	0.0670	0.419
0.117	0.015	13.95	0.5172	0.122	0.0773	0.483
0.133	0.016	14.88	0.5517	0.118	0.0825	0.516
0.150	0.019	17.67	0.6551	0.114	0.0980	0.612

To calculate the initial dissolution rate of Al, plot graph between Al concentration (mole/g and mole/dm²) and time (hr)

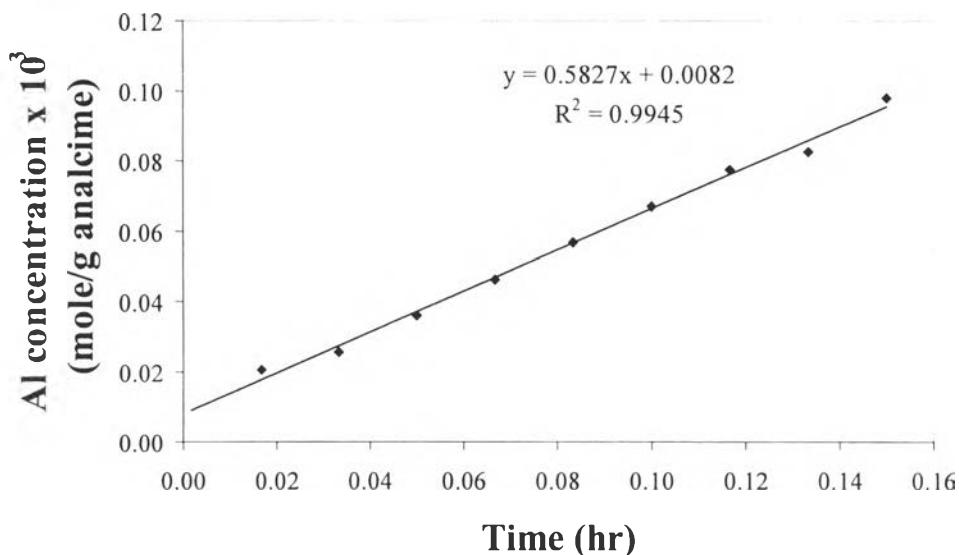


Figure B.2 Al concentration per g of initial analcime as a function of time

Initial dissolution rate of aluminum = 0.5827 mole Al/g.hr

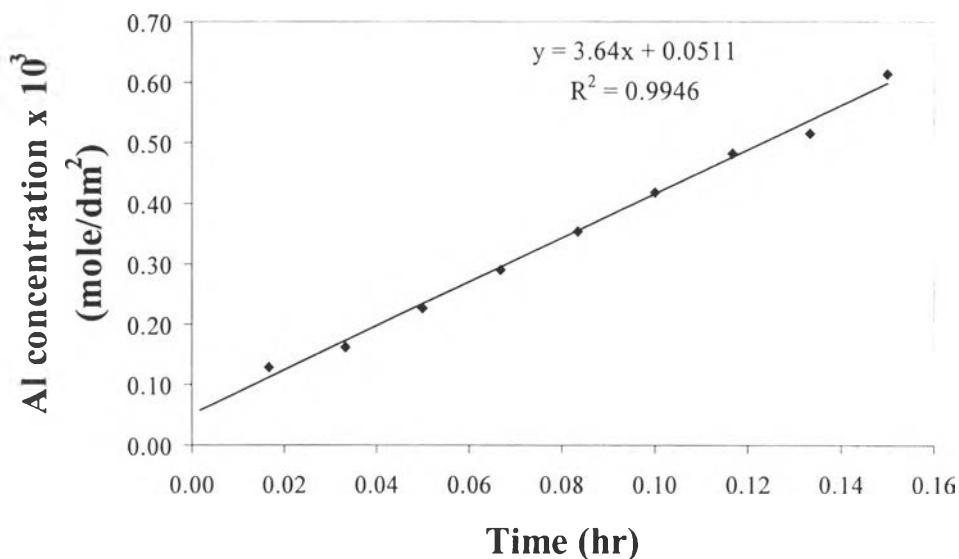


Figure B.3 Al concentration per external surface area of initial analcime as a function of time

Initial dissolution rate of aluminum = 3.64 mole/dm².hr

For Si and Na, initial dissolution rates can be obtained in the same manner.

Appendix C Calculation Method for Deprotonation Curve of Citric Acid

1. Equilibrium Acid Constant

The equilibrium acid constant is defined in terms of the activity of product species divided by reactant species as shown below:

Consider the following reaction:



The equilibrium acid constant is expressed as:

$$Ka = \frac{a_{H_3O^+} a_{A^-}}{a_{HA}} \quad (C.1)$$

where ' a ' denotes the activities of the hydrated species

Rearranging Eq. (C.1):

$$a_{H_3O^+} = \frac{(Ka)(a_{HA})}{a_{A^-}} \quad (C.2)$$

Taking the logarithms both sides of Eq. (C.2):

$$-\log a_{H_3O^+} = -\log \left[\frac{(Ka)(a_{HA})}{a_{A^-}} \right] \quad (C.3)$$

Rearranging Eq. (C.3):

$$-\log a_{H_3O^+} = -\left[\log Ka - \log \frac{a_{A^-}}{a_{HA}} \right] \quad (C.4)$$

where $pH = -\log a_{H_3O^+}$ and $pKa = -\log Ka$

Therefore, Eq. (C.4) becomes:

$$pH = pKa + \log \left[\frac{a_A}{a_{H_A}} \right] \quad (C.5)$$

or

$$pH = pKa + \log \left[\frac{a_{base species}}{a_{acid species}} \right] \quad (C.6)$$

2. Activity

The activity is defined as:

$$a_i = C_i f_i \quad (C.7)$$

where C_i = Molar concentration (M)

f_i = Activity coefficient

Substituting Eq. (C.7) into Eq. (C.1)

$$Ka = \frac{(C_{H_3O^+} f_{H_3O^+})(C_A f_A)}{(C_{H_A} f_{H_A})} \quad (C.8)$$

Rearranging Eq. (C.8):

$$Ka = \frac{C_{H_3O^+} C_A}{C_{H_A}} \cdot \frac{f_{H_3O^+} f_A}{f_{H_A}} \quad (C.9)$$

$$K\alpha = K\alpha' \frac{f_{H_3O^+} f_A}{f_{HA}} \quad (\text{C.10})$$

where $K\alpha' = \frac{C_{H_3O^+} C_A}{C_{HA}}$

Rearranging Eq. (C.10):

$$K\alpha' = K\alpha \frac{f_{HA}}{f_{H_3O^+} f_A} = f(T, f_r) \quad (\text{C.11})$$

The Eq. (C.6) is normally used in terms of molar concentration unit (M), therefore the Eq. (C.6) is expressed as:

$$pH = pK\alpha' + \log \left[\frac{C_{\text{basic species}}}{C_{\text{acid species}}} \right] \quad (\text{C.12})$$

In general, the equilibrium reaction of acid is shown as:



From Eq. (C.13), Eq. (C.12) becomes:

$$pH = pK\alpha' + \log \left[\frac{C_{H_{n-1} A^{(n-1)-}}}{C_{H_n A^{(n-1)-}}} \right] \quad (\text{C.14})$$

From Eq. (11), it is illustrated that $K\alpha'$ is a function of temperature (T) and activity coefficient (f_r), nevertheless the activity coefficient is also depended upon the ionic strength (I) as shown by the Debye-Hückel equation. The Debye-Hückel equation for dilute solution can be expressed as:

$$\log f_i = -\frac{AZ^2 I^{0.5}}{1 + I^{0.5}} + 0.1Z^2 I \quad (\text{C.15})$$

where f_i = Activity coefficient

I = Ionic strength (M)

Z = Charge

A = Temperature-dependent constant (at 25°C: $A = 0.512$)

Coupling Eq. (C.15) with Eq. (C.14), Eq. (C.14) becomes:

$$pH = pK_a - \frac{(2x+1)AI^{0.5}}{(1+I^{0.5})} + 0.1(2x+1)I + \log \left[\frac{C_{H_n A^{(A+1)}}}{C_{H_n A^A}} \right] \quad (\text{C.16})$$

where

$$pK_a' = pK_a - \frac{(2x+1)AI^{0.5}}{(1+I^{0.5})} + 0.1(2x+1)I \quad (\text{C.17})$$

3. Calculation Method for Deprotonation Curves

Citric acid is a polyprotic acid which dissociates in three steps depended upon the number of ionizable protons containing in the molecules as shown below:



The dissociation of citric acid can be expressed in terms of three equilibrium acid constants as shown by the following equations:

$$K_{a_1} = \frac{[C_6H_7O_7^-][H^+]}{[C_6H_8O_7]} \quad (\text{C.18})$$

$$K_{a_2} = \frac{[C_6H_5O_7^{3-}] \cdot [H^+]}{[C_6H_6O_7^{2-}]} \quad (C.19)$$

$$K_{a_2} = \frac{[C_6H_5O_7^{3-}] \cdot [H^+]}{[C_6H_6O_7^{2-}]} \quad (C.20)$$

The total citric acid concentration is the summation of all citric acid species:

$$Citric\ acid_{total} = [C_6H_5O_7^{3-}] + [C_6H_6O_7^{2-}] + [C_6H_7O_7^-] + [C_6H_8O_7] \quad (C.21)$$

From the equilibrium reaction indicating the several deprotonation steps of citric acid, the concentration of each deprotonated species can be expressed as:

$$[C_6H_8O_7] = \frac{[C_6H_7O_7^-] \cdot [H^+]}{K_{a_1}} \quad (C.22)$$

$$[C_6H_7O_7^-] = \frac{[C_6H_6O_7^{2-}] \cdot [H^+]}{K_{a_2}} \quad (C.23)$$

$$[C_6H_6O_7^{2-}] = \frac{[C_6H_5O_7^{3-}] \cdot [H^+]}{K_{a_3}} \quad (C.24)$$

From Eq. (C.16) and (C.17), all deprotonated species can be rewritten in terms of pH and $pK_{a'}$ as shown below:

$$[C_6H_8O_7] = [C_6H_7O_7^-] \cdot 10^{pK_{a'1}-pH} \quad (C.25)$$

$$[C_6H_7O_7^-] = [C_6H_6O_7^{2-}] \cdot 10^{pK_{a'2}-pH} \quad (C.26)$$

$$[C_6H_6O_7^{2-}] = [C_6H_5O_7^{3-}] \cdot 10^{pK_{a'3}-pH} \quad (C.27)$$

where

$$pK\alpha'_1 = pK\alpha_1 - \frac{AI^{0.5}}{(1+I^{0.5})} + 0.1I \quad (\text{C.28})$$

$$pK\alpha'_2 = pK\alpha_2 - \frac{3AI^{0.5}}{(1+I^{0.5})} + 0.3I \quad (\text{C.29})$$

$$pK\alpha'_3 = pK\alpha_3 - \frac{5AI^{0.5}}{(1+I^{0.5})} + 0.5I \quad (\text{C.30})$$

Substituting Eq. (C.25) - (C.27) in Eq. (C.21) and rearranging:

$$[C_6H_5O_7^{3-}] = [C_6H_5O_7^{3-}] \left(1 + 10^{pK\alpha_1 - pH} + 10^{pK\alpha'_2 + pK\alpha'_3 - 2pH} + 10^{pK\alpha'_3 + pK\alpha'_2 + pK\alpha'_1 - 3pH} \right) \quad (\text{C.31})$$

Defining:

$$A = (1 + 10^{pK\alpha_1 - pH} + 10^{pK\alpha'_2 + pK\alpha'_3 - 2pH} + 10^{pK\alpha'_3 + pK\alpha'_2 + pK\alpha'_1 - 3pH}) \quad (\text{C.32})$$

Substituting Eq. (C.32) in Eq. (C.31), Eq. (C.31) becomes:

$$[C_6H_5O_7^{3-}] = \frac{[C_6H_5O_7^{3-}]}{A} \quad (\text{C.33})$$

Therefore, the fraction of all deprotonated species can be calculated from the following equation:

$$\text{Fraction of } [C_6H_5O_7^{3-}] \text{ species} = \frac{[C_6H_5O_7^{3-}]}{[C_6H_5O_7^{3-}] + [C_6H_5O_7^{2-}] + [C_6H_5O_7^{-}] + [C_6H_5O_7^{3-}]} = \frac{1}{A} \quad (\text{C.34})$$

$$\text{Fraction of } [C_6H_6O_7^{2-}] \text{ species} = \frac{10^{pK_a'_{1-} - pH}}{A} \quad (\text{C.35})$$

$$\text{Fraction of } [C_6H_7O_7^-] \text{ species} = \frac{10^{pK_a'_{1-} + pK_a'_{2-} - pH}}{A} \quad (\text{C.35})$$

$$\text{Fraction of } [C_6H_8O_7] \text{ species} = \frac{10^{pK_a'_{1-} + pK_a'_{2-} + pK_a'_{3-} - pH}}{A} \quad (\text{C.36})$$

Substituting the values of $pK_a'_{1-}$ to $pK_a'_{3-}$ from Eq. (C.28) – (C.30) in Eq. (C.34) – (C.36), the fraction of all deprotonated species of citric acid is subsequently attained.

Appendix D Experimental Data

1. The Initial Rates of the Dissolution Reaction of Analcime

Table D.1 The initial rates of Si, Al and Na for each experiment

No	Analcime Size	Acid	Conc.	Initial Rate x 10 ³ (mole/g/hr)		
				Si	Al	Na
1	0.71-1.18	Citric acid	0.1	0.53	0.20	0.23
2	0.212-0.300	Citric acid	0.1	0.62	0.60	0.56
3	0.150-0.180	Citric acid	0.1	1.35	1.00	1.43
4	0.045-0.075	Citric acid	0.1	4.95	3.34	3.18
5	0.71-1.18	HCl	0.047	0.15	0.11	0.18
6	0.71-1.18	HCl	0.1	0.23	0.16	0.05
7	0.71-1.18	HCl	0.2	0.69	0.44	0.71

Note: Experiment 1 was performed in a batch reactor with 2 g of analcime and 500 dm³ of citric acid

Experiment 2-4 were performed in a batch reactor with 1 g of analcime and 150 dm³ of citric acid

Experiment 5-7 were performed in vials

2. Size Distribution of Analcime Particles as a Function of Time

Table D.2 The size distribution of analcime (0.045-0.075 mm) before the reaction

Size of Particle (mm)	Number of Particle (%)		
	Dry	Wet (immediately)	Wet (24hr)
0-0.01	35.2	27.1	2.6
0.01-0.02	23.9	14.6	0.0
0.02-0.03	15.5	22.9	30.8
0.03-0.04	14.1	25.0	41.0
0.04-0.05	8.5	10.4	20.5
0.05-0.06	2.8	0.0	5.1

Table D.3 The size distribution of analcime (0.045-0.075 mm) after the dissolution reaction in 3M citric acid (series 1)

Size of Particle (mm)	Number of Particle (%)		
	2min	9min	15min
0-0.01	61.8	51.7	54.0
0.01-0.02	14.7	21.7	23.3
0.02-0.03	12.5	14.2	13.6
0.03-0.04	7.4	9.2	6.3
0.04-0.05	2.2	3.3	1.7
0.05-0.06	1.5	0.0	1.1

Table D.4 The size distribution of analcime (0.045-0.075 mm) after the dissolution reaction in 3M citric acid (series 2)

Size of Particle (mm)	Number of Particle (%)		
	2min	9min	15min
0-0.01	65.2	63.6	46.4
0.01-0.02	21.3	22.6	26.3
0.02-0.03	7.9	7.2	10.3
0.03-0.04	4.9	4.6	12.4
0.04-0.05	0.6	1.5	4.6
0.05-0.06	0.0	0.5	0.0

Table D.5 The size distribution of analcime (0.045-0.075 mm) after the dissolution reaction in 0.1M HCl (series 1)

Size of Particle (mm)	Number of Particle (%)					
	2min	9min	15min	30min	45min	60min
0-0.01	69.9	77.6	72.5	86.4	85.7	84
0.01-0.02	16.4	9.2	5.0	9.9	11.1	4
0.02-0.03	8.2	6.6	12.5	1.2	1.6	8
0.03-0.04	2.7	2.6	10.0	1.2	1.6	4
0.04-0.05	1.4	2.6	0.0	1.2	0.0	0
0.05-0.06	1.4	1.3	0.0	0.0	0.0	0

Table D.6 The size distribution of analcime (0.045-0.075 mm) after the dissolution reaction in 0.1M HCl (series 2)

Size of Particle (mm)	Number of Particle (%)					
	2min	9min	15min	30min	45min	60min
0-0.01	14.3	27.6	25.0	13.9	38.6	34.5
0.01-0.02	7.1	19.0	12.5	19.4	18.2	14.3
0.02-0.03	23.8	22.4	39.6	19.4	18.2	21.4
0.03-0.04	38.1	13.8	10.4	27.8	11.4	15.5
0.04-0.05	7.1	15.5	12.5	16.7	11.4	13.1
0.05-0.06	9.5	1.7	0.0	2.8	2.3	1.2

Table D.7 The size distribution of analcime (0.71-1.18 mm) before the reaction

Size of Particle (mm)	Number of Particle (%)		
	Dry	Wet (immediately)	Wet (24hr)
0-0.1	46.7	28.6	26.1
0.1-0.2	0.0	0.0	0.0
0.2-0.3	0.0	0.0	0.0
0.3-0.4	0.0	0.0	0.0
0.4-0.5	0.0	7.1	0.0
0.5-0.6	13.3	21.4	4.3
0.6-0.7	20.0	14.3	4.3
0.7-0.8	6.7	0.0	13.0
0.8-0.9	13.3	7.1	4.3
0.9-1.0	0.0	7.1	4.3
1.0-1.1	0.0	14.3	13.0
1.1-1.2	0.0	0.0	8.7
1.2-1.3	0.0	0.0	8.7

Table D.7 (Cont.)

Size of Particle (mm)	Number of Particle (%)		
	Dry	Wet (immediately)	Wet (24hr)
1.3-1.4	0.0	0.0	4.3
1.4-1.5	0.0	0.0	0.0
1.5-1.6	0.0	0.0	0.0
1.6-1.7	0.0	0.0	8.7

Table D.8 The size distribution of analcime (0.71-1.18 mm) after the dissolution reaction in 3M citric acid (series 1)

Size of Particle (mm)	Number of Particle (%)		
	2min	9min	15min
0-0.1	61.5	89.2	93.1
0.1-0.2	1.5	1.2	0.0
0.2-0.3	0.0	0.0	0.0
0.3-0.4	3.1	0.6	0.0
0.4-0.5	1.5	1.2	0.0
0.5-0.6	6.2	1.2	1.4
0.6-0.7	9.2	4.2	1.4
0.7-0.8	10.8	0.6	1.4
0.8-0.9	4.6	0.6	2.8
0.9-1.0	1.5	0.6	0.0
1.0-1.1	0.0	0.6	0.0
1.1-1.2	0.0	0.0	0.0
1.2-1.3	0.0	0.0	0.0
1.3-1.4	0.0	0.0	0.0

Table D.9 The size distribution of analcime (0.71-1.18 mm) after the dissolution reaction in 3M citric acid (series 2)

Size of Particle (mm)	Number of Particle (%)		
	2min	9min	15min
0-0.1	72.9	75.7	89.3
0.1-0.2	0.0	0.0	0.0
0.2-0.3	1.2	0.0	0.0
0.3-0.4	1.2	0.0	0.0
0.4-0.5	5.9	1.4	1.3
0.5-0.6	9.4	5.7	0.0
0.6-0.7	1.2	11.4	5.3
0.7-0.8	4.7	4.3	2.7
0.8-0.9	2.4	0.0	1.3
0.9-1.0	0.0	1.4	0.0
1.0-1.1	1.2	0.0	0.0
1.1-1.2	0.0	0.0	0.0
1.2-1.3	0.0	0.0	0.0
1.3-1.4	0.0	0.0	0.0

Table D.10 The size distribution of analcime (0.71-1.18 mm) after the dissolution reaction in 0.1M HCl (series 1)

Size of Particle (mm)	Number of Particle (%)						
	2min	9min	15min	60min	180min	240min	24hr
0-0.1	0.0	43.5	81.1	93.2	93.9	89.3	98.9
0.1-0.2	0.0	0.0	0.0	0.0	0.9	1.0	0.0
0.2-0.3	0.0	0.0	0.0	0.0	0.0	1.0	0.0
0.3-0.4	10.0	4.3	0.0	0.0	0.0	1.9	0.0

Table D.10 (Cont.)

Size of Particle (mm)	Number of Particle (%)						
	2min	9min	15min	60min	180min	240min	24hr
0.4-0.5	0.0	13.0	2.7	0.0	1.8	2.9	0.0
0.5-0.6	30.0	8.7	2.7	2.3	0.9	1.0	1.1
0.6-0.7	40.0	13.0	10.8	2.3	1.8	1.9	0.0
0.7-0.8	0.0	13.0	2.7	2.3	0.0	0.0	0.0
0.8-0.9	10.0	4.3	0.0	0.0	0.0	1.0	0.0
0.9-1.0	0.0	0.0	0.0	0.0	0.9	0.0	0.0
1.0-1.1	10.0	0.0	0.0	0.0	0.0	0.0	0.0
1.1-1.2	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1.2-1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1.3-1.4	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1.4-1.5	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1.5-1.6	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1.6-1.7	0.0	0.0	0.0	0.0	0.0	0.0	0.0

Table D.11 The size distribution of analcime (0.71-1.18 mm) after the dissolution reaction in 0.1M HCl (series 2)

Size of Particle (mm)	Number of Particle (%)					
	2min	9min	15min	60min	180min	240min
0-0.1	38.9	52.2	65.1	91.9	99.0	98.4
0.1-0.2	0.0	0.0	0.0	0.0	0.0	0.8
0.2-0.3	5.6	0.0	0.0	0.0	0.0	0.0
0.3-0.4	11.1	0.0	4.7	0.0	0.0	0.0
0.4-0.5	11.1	4.3	14.0	0.0	0.0	0.0
0.5-0.6	22.2	21.7	9.3	2.7	0.0	0.8

Table D.11 (Cont.)

Size of Particle (mm)	Number of Particle (%)					
	2min	9min	15min	60min	180min	240min
0.6-0.7	5.6	8.7	4.7	5.4	0.0	0.0
0.7-0.8	5.6	4.3	2.3	0.0	1.0	0.0
0.8-0.9	0.0	8.7	0.0	0.0	0.0	0.0
0.9-1.0	0.0	0.0	0.0	0.0	0.0	0.0
1.0-1.1	0.0	0.0	0.0	0.0	0.0	0.0
1.1-1.2	0.0	0.0	0.0	0.0	0.0	0.0
1.2-1.3	0.0	0.0	0.0	0.0	0.0	0.0
1.3-1.4	0.0	0.0	0.0	0.0	0.0	0.0
1.4-1.5	0.0	0.0	0.0	0.0	0.0	0.0
1.5-1.6	0.0	0.0	0.0	0.0	0.0	0.0
1.6-1.7	0.0	0.0	0.0	0.0	0.0	0.0

Table D.12 The size distribution of analcime (0.71-1.18 mm) after the dissolution reaction in 0.2 HCl (series 1)

Size of Particle (mm)	Number of Particle (%)						
	2min	9min	15min	60min	120min	240min	24hr
0-0.1	23.5	0.0	40.0	37.7	80.4	75.0	53.3
0.1-0.2	7.8	0.0	17.1	22.6	8.9	13.3	15.6
0.2-0.3	3.9	0.0	11.4	3.8	1.8	3.3	15.6
0.3-0.4	11.8	0.0	0.0	1.9	0.0	3.3	6.7
0.4-0.5	27.5	3.6	2.9	5.7	1.8	1.7	0.0
0.5-0.6	11.8	17.9	0.0	0.0	1.8	0.0	0.0
0.6-0.7	7.8	3.6	0.0	0.0	0.0	0.0	2.2
0.7-0.8	3.9	0.0	0.0	0.0	1.8	0.0	2.2

Table D.12 (Cont.)

Size of Particle (mm)	Number of Particle (%)						
	2min	9min	15min	60min	120min	240min	24hr
0.8-0.9	2.0	7.1	0.0	0.0	0.0	0.0	0.0
0.9-1.0	0.0	3.6	0.0	0.0	0.0	0.0	0.0
1.0-2.0	0.0	0.0	8.6	0.0	1.8	0.0	2.2
2.0-3.0	0.0	46.4	20.0	15.1	1.8	1.7	0.0
3.0-4.0	0.0	17.9	0.0	11.3	0.0	1.7	2.2
4.0-5.0	0.0	0.0	0.0	1.9	0.0	0.0	0.0

Table D.13 The size distribution of analcime (0.71-1.18 mm) after the dissolution reaction in 0.2 HCl (series 2)

Size of Particle (mm)	Number of Particle (%)						
	2min	9min	15min	60min	120min	240min	24hr
0-0.1	33.3	39.1	81.1	94.0	93.5	98.5	99.2
0.1-0.2	0.0	2.2	0.0	0.0	0.0	0.7	0.8
0.2-0.3	0.0	0.0	0.0	1.0	0.0	0.0	0.0
0.3-0.4	8.9	6.5	2.5	2.0	0.8	0.0	0.0
0.4-0.5	6.7	17.4	7.4	1.0	1.6	0.7	0.0
0.5-0.6	28.9	17.4	4.9	1.0	2.4	0.0	0.0
0.6-0.7	11.1	6.5	1.6	1.0	0.8	0.0	0.0
0.7-0.8	8.9	6.5	1.6	0.0	0.8	0.0	0.0
0.8-0.9	2.2	2.2	0.8	0.0	0.0	0.0	0.0
0.9-1.0	0.0	2.2	0.0	0.0	0.0	0.0	0.0
1.0-2.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
2.0-3.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

Table D.13 (Cont.)

Size of Particle (mm)	Number of Particle (%)						
	2min	9min	15min	60min	120min	240min	24hr
3.0-4.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
4.0-5.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

3. Mass Balance for Experiment Performed in Vials**Table D.14** Mass balance for the experiment of analcime (0.045-0.075 mm) with 3M citric acid

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass Lost
0.03	1	0.094	12.551	0.063	10.314	12.645	10.377	2.268
0.15	1	0.099	11.907	0.044	9.901	12.006	9.945	2.061
0.25	1	0.092	11.852	0.039	10.268	11.9442	10.308	1.637
0.03	2	0.096	11.897	0.061	9.786	11.9927	9.846	2.146
0.15	2	0.092	11.872	0.047	10.555	11.9636	10.603	1.361
0.25	2	0.093	11.720	0.042	10.106	11.8132	10.149	1.665

Table D.15 Mass balance for the experiment of analcime (0.045-0.075 mm) with 0.047M HCl

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass Lost
0.03	1	0.091	9.763	0.085	8.650	9.854	8.735	1.119
0.15	1	0.094	9.750	0.083	8.477	9.844	8.561	1.283
0.25	1	0.092	9.747	0.081	8.442	9.838	8.523	1.316
0.03	2	0.095	9.761	0.087	9.246	9.856	9.333	0.523
0.13	2	0.093	9.765	0.084	8.883	9.858	8.967	0.892
0.25	2	0.094	9.752	0.085	8.598	9.845	8.684	1.162

Table D.16 Mass balance for the experiment of analcime (0.045-0.075 mm) with 0.1M HCl

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass lost
0.03	1	0.094	9.857	0.418	8.178	9.951	8.595	1.356
0.15	1	0.091	9.842	0.414	8.355	9.933	8.769	1.164
0.25	1	0.092	9.880	0.079	8.700	9.973	8.779	1.194
0.50	1	0.095	10.102	0.073	8.521	10.197	8.594	1.603
0.75	1	0.096	10.075	0.069	8.432	10.171	8.501	1.670
1.00	1	0.095	10.231	0.061	8.128	10.325	8.188	2.137
0.03	2	0.092	9.809	0.087	9.054	9.901	9.141	0.760
0.15	2	0.092	9.758	0.081	9.205	9.850	9.286	0.564
0.25	2	0.092	9.768	0.080	8.218	9.860	8.298	1.563
0.50	2	0.095	9.814	0.074	8.777	9.909	8.851	1.058
0.75	2	0.092	9.779	0.066	8.086	9.871	8.152	1.719

Table D.16 (Cont.)

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass lost
1.00	2	0.094	9.754	0.066	8.745	9.847	8.811	1.036

Table D.17 Mass balance for the experiment of analcime (0.71-1.18 mm) with 3M citric acid

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass Lost
0.03	1	0.100	11.839	0.099	9.175	11.939	9.273	2.666
0.15	1	0.093	12.064	0.091	9.226	12.156	9.317	2.840
0.25	1	0.095	12.071	0.092	9.259	12.166	9.350	2.816
0.03	2	0.098	12.539	0.099	9.788	12.637	9.886	2.751
0.15	2	0.094	12.524	0.093	9.657	12.618	9.750	2.87
0.25	2	0.099	12.514	0.098	9.946	12.613	10.044	2.569

Table D.18 Mass balance for the experiment of analcime (0.71-1.18 mm) with 0.047M HCl

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass Lost
0.03	1	0.100	9.866	0.100	8.123	9.967	8.223	1.743
0.15	1	0.098	10.249	0.094	8.537	10.347	8.631	1.716
0.25	1	0.095	10.228	0.095	8.824	10.324	8.919	1.405

Table D.18 (Cont.)

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass Lost
0.03	2	0.092	9.768	0.091	8.331	9.860	8.422	1.438
0.15	2	0.098	9.786	0.096	7.737	9.883	7.832	2.051
0.25	2	0.092	9.749	0.090	8.201	9.841	8.291	1.551

Table D.19 Mass balance for the experiment of analcime (0.71-1.18 mm) with 0.1M HCl

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass Lost
0.03	1	0.092	10.318	0.090	8.615	10.409	8.706	1.704
0.15	1	0.098	10.269	0.091	8.675	10.367	8.766	1.601
0.25	1	0.092	10.273	0.092	8.551	10.365	8.643	1.722
1.00	1	0.094	9.808	0.085	8.724	9.901	8.808	1.093
2.00	1	0.096	9.782	0.082	8.719	9.877	8.800	1.077
3.00	1	0.091	9.802	0.075	8.447	9.893	8.523	1.370
4.00	1	0.104	9.779	0.074	8.421	9.883	8.495	1.388
24.00	1	0.099	10.298	0.026	7.996	10.397	8.022	2.375
18.00	1	0.092	9.792	0.043	8.127	9.884	8.170	1.714
0.03	2	0.096	9.785	0.095	8.479	9.881	8.574	1.307
0.15	2	0.094	9.708	0.092	8.465	9.802	8.556	1.246
0.25	2	0.095	9.713	0.094	8.857	9.808	8.951	0.857
1.00	2	0.098	9.794	0.092	8.288	9.892	8.380	1.512
2.00	2	0.095	9.800	0.083	8.306	9.894	8.389	1.505

Table D.19 (Cont.)

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass Lost
3.00	2	0.093	9.768	0.076	8.547	9.861	8.623	1.238
4.00	2	0.093	9.762	0.068	9.037	9.855	9.105	0.749

Table D.20 Mass balance for the experiment of analcime (0.71-1.18 mm) with 0.2M HCl

Time (hr)	#	Initial wt. (g)		Final wt. (g)		Total wt. (g)		
		Solid	Solution	Solid	Filtrate	Initial	Final	Mass Lost
0.03	1	0.101	9.836	0.099	8.254	9.938	8.353	1.585
0.15	1	0.105	9.740	0.104	8.578	9.845	8.682	1.163
0.25	1	0.092	9.739	0.090	8.382	9.831	8.472	1.359
1.00	1	0.095	9.736	0.085	8.426	9.831	8.511	1.320
2.00	1	0.102	9.757	0.080	8.516	9.859	8.596	1.263
4.00	1	0.100	9.746	0.062	8.410	9.846	8.472	1.374
24.00	1	0.092	9.753	0.014	8.112	9.845	8.125	1.719
0.03	2	0.094	9.748	0.094	8.977	9.842	9.071	0.771
0.15	2	0.099	9.726	0.097	8.734	9.825	8.831	0.994
0.25	2	0.105	9.802	0.103	8.582	9.907	8.684	1.222
1.00	2	0.092	9.809	0.086	8.586	9.901	8.672	1.229
2.00	2	0.093	9.769	0.071	8.606	9.862	8.677	1.185
4.00	2	0.097	9.764	0.069	8.377	9.861	8.446	1.415
24.00	2	0.099	9.779	0.015	8.356	9.877	8.371	1.506

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