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การดูดซับและการแพร่ของ  $H_2$ ,  $N_2$  และ  $H_2/N_2$  ในวัสดุโครงข่ายโลหะอินทรีย์  
ชนิดเลียนแบบซีโอไลต์-67 โดยการคำนวณทางคอมพิวเตอร์ขั้นสูง

Adsorption and diffusion of  $H_2$ ,  $N_2$  and  $H_2/N_2$  in Zeolitic Imidazolate  
Framework-67 by advanced computational calculations

By

Miss Chanunchida Kunsiri

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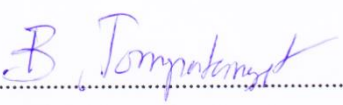
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### บทคัดย่อ

ZIF-67 (Zeolite Imidazolate Frameworks-67) เป็นวัสดุชนิดเลียนแบบซีโอไลต์ที่มีโครงข่ายรูพรุนชนิดหนึ่งซึ่งใช้เป็นตัวเร่งปฏิกิริยาเคมี, วัสดุกักเก็บแก๊ส และใช้ในกระบวนการแยกแก๊ส ZIF-67 ประกอบด้วยโลหะโคบอลต์ (Co) เชื่อมต่อกับสารอินทรีย์เมทิลอิมิดาโซลเลท (MeIM) งานวิจัยนี้ใช้เทคนิคการจำลองแบบกิบบส์ของขอมเปิดมอนติคาร์โล และการจำลองแบบทางพลวัต ศึกษาพฤติกรรมการดูดซับและการแพร่ของแก๊สเดี่ยว  $H_2$  และ  $N_2$  และแก๊สผสม  $H_2/N_2$  ที่ 3 อุณหภูมิ ผลไอโซเทอร์มการดูดซับ ที่ได้จากการจำลองนี้แสดงให้เห็นว่า ZIF-67 สามารถดูดซับ  $N_2$  ได้มากกว่า  $H_2$  และปริมาณการดูดซับจะลดลงเมื่ออุณหภูมิเพิ่มขึ้น และชุดพารามิเตอร์ของโคบอลต์ที่แตกต่างกันไม่ส่งผลต่อการดูดซับอย่างมีนัยสำคัญ จากค่าการคำนวณฟังก์ชันการกระจายเชิงรัศมี ตำแหน่งดูดซับที่ชอบของแก๊ส  $H_2$  และ  $N_2$  อยู่ที่บริเวณส่วนเชื่อมต่อกับอินทรีย์ ซึ่ง  $N_2$  เกาะยึดได้ดีกว่า  $H_2$  เพื่อศึกษาพฤติกรรมเชิงพลวัตของโมเลกุลแก๊สในวัสดุนี้ ซึ่งได้มีการคำนวณค่าสัมประสิทธิ์การแพร่ในตัวเองของแก๊ส พบว่าค่าสัมประสิทธิ์การแพร่ในตัวเองของ  $N_2$  น้อยกว่าค่าสัมประสิทธิ์การแพร่ในตัวเองของ  $H_2$  นั้นหมายความว่า  $N_2$  เคลื่อนที่ได้ช้ากว่า  $H_2$  ทำให้สรุปได้ว่า ZIF-67 มีความเหมาะสมในการคัดแยกแก๊ส  $H_2$  จาก  $N_2$

คำสำคัญ: วัสดุโลหะอินทรีย์ชนิดเลียนแบบซีโอไลต์-67, การดูดซับ, การแพร่, การคำนวณด้วยคอมพิวเตอร์ขั้นสูง

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### Abstract

ZIF-67 (Zeolitic Imidazolate Framework-67) is a class of porous materials which have applications as catalysis, gas storage and gas separation. ZIF-67 consists of Cobalt (Co) connected to Methylimidazolate (MeIM). In this work, Gibbs Ensemble Monte Carlo (GEMC) simulations and Molecular Dynamics (MD) simulations were carried out to study adsorption behavior, structural and dynamics properties of Hydrogen ( $H_2$ ) and Nitrogen ( $N_2$ ) in ZIF-67 at three temperatures. The adsorption isotherms results indicate that ZIF-67 can adsorb  $N_2$  in higher amount than  $H_2$ . The amount adsorbed decreases with the increase in temperatures. The different sets of Co force field parameters do not significantly affect the gas adsorption, except at lower temperatures. From the Radial Distribution Functions (RDFs), the preferential adsorption site for  $H_2$  and  $N_2$  is around the organic linker zone.  $N_2$  binds stronger than  $H_2$ . In order to observe the dynamics behavior of gases, the self-diffusion ( $D_s$ ) was calculated. It was found that  $D_s$  of  $N_2$  is the lower than  $D_s$  of  $H_2$ . That means  $N_2$  moves slower than  $H_2$ . Finally, it can be concluded that ZIF-67 is well suited to separate  $H_2$  from  $N_2$ .

Keywords: Zeolitic Imidazolate Framework-67, Adsorption, Diffusion, Computational Calculations

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# Chapter 1

## Introduction

### 1.1 Background of this study

Currently, the world's energy demand rises. Hydrogen (H<sub>2</sub>) is used as alternative energy for a limited volume and no pollution after using. Energy from H<sub>2</sub> is considered to be energy efficient, clean and environmentally friendly. At the same time, Nitrogen (N<sub>2</sub>) is another type of gas that plays an important role in the petrochemical industry which increase the yield and efficiency of the oil. For this reason, porous materials that have been researched and developed to separate and store gas are Zeolites and Metal Organic Frameworks (MOFs) [1].

In recent years, Zeolite Imidazolate Frameworks (ZIF) have been discovered as metal-organic materials. This is a compound with similar properties to zeolite in terms of stability and similar to the organic metal network material in terms of the ability to modify a variety of structural easily. It also has several outstanding properties, such as strong structure, flexibility, high surface area and can resist heat. This material is used in the industry as a catalyst, gas storage container and in the gas separation process [2], [3], [4].

In 2012, Quen *et al.* [5] have synthesized ZIF-67 for the first time in aqueous solutions at room temperature. They found that ZIF-67 were highly stable up to 350°C. In 2017, Verpoort *et al.* [6] reported that the ZIF-67 was developed from ZIF-8. It consists of Cobalt (Co) connected to Methylimidazolate (MeIM) set to strong crystalline structure, high temperature stability and higher specificity for gas storage than ZIF-8. In addition, Economou *et al.* [7] confirmed that ZIF-67 separated gas better than ZIF-8 for propylene/propane.

This work is interested to studying the behavior of H<sub>2</sub> and N<sub>2</sub> and H<sub>2</sub>/ N<sub>2</sub> gas mixture in ZIF-67. This method can provide information on molecular structure and interaction which is difficult to test experimentally. It also reduces the cost of the experiment. In addition, the knowledge gained will be beneficial for the design and development of ZIF to be effective and suitable for further industrial applications.

## 1.2 Objectives of this study

To study the adsorption behavior of  $H_2$ ,  $N_2$  and  $H_2 / N_2$  gas mixture in the ZIF-67 using Gibbs Ensemble Monte Carlo (GEMC) simulations and Molecular Dynamics (MD) simulations and to study the structural and dynamic properties.

## 1.3 Benefits of this study

To understand gas storage of  $H_2$ ,  $N_2$  and gas separation of  $H_2 / N_2$  mixture in the Zeolitic Imidazolate Framework-67.

## 1.4 Zeolitic Imidazolate Framework-67 (ZIF-67)

ZIF-67 is comprised of  $Co^{2+}$  metal ions and 2-methylimidazole. Its structure is applied from ZIF-8 structure by replacing Zn metal atom with  $Co^{2+}$  as shown in Fig.1.

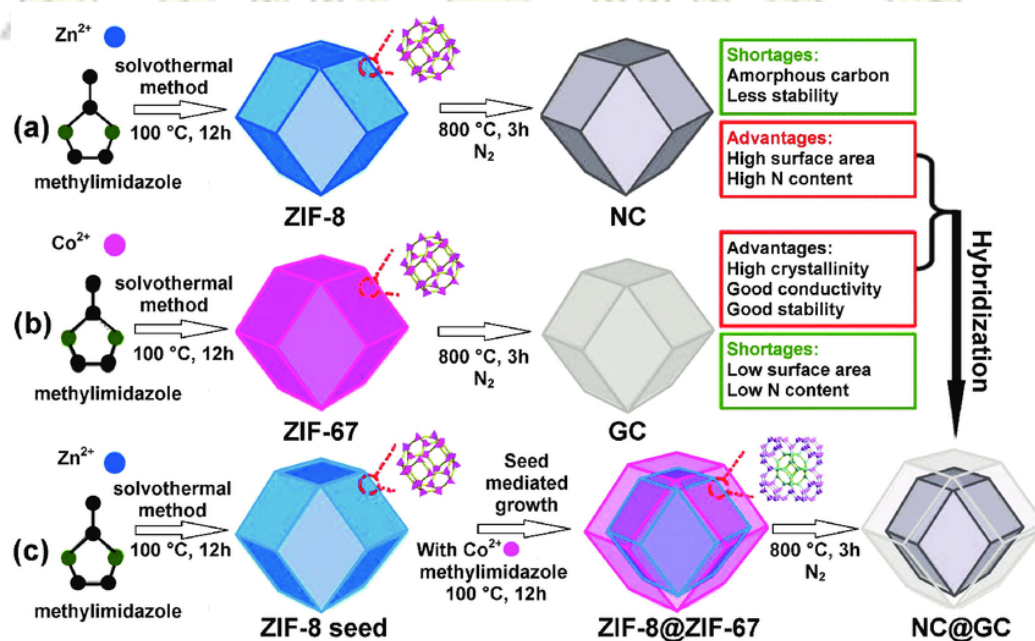


Figure1 Synthesis scheme for the preparation of ZIF-8 and ZIF-67 [8]

### 1.5 Molecular mechanics and Force field parameters

The potential energy of the system in molecular dynamics was described by the force field parameters. The total energy depended on bonded potential and nonbonded potential in Eq.1 [9]

$$E_{\text{total}} = E_{\text{bonded}} + E_{\text{nonbonded}} \quad (\text{Eq.1})$$

The bonded potential was described by bond stretching, angle bending and dihedral angle torsion following Eq.2, while the nonbonded potential was described by the Van Der Waals potential and Coulomb potential following Eq.3.

$$E_{\text{bonded}} = \sum_{\text{bonds}} K_b (r-r_0)^2 + \sum_{\text{angles}} K_\theta (\theta - \theta_0)^2 + \sum_{\text{dihedrals}} K_\phi [1 + \cos(n\phi - \phi_0)] \quad (\text{Eq.2})$$

Where  $K_b, K_\theta, K_\phi$  are the force constants of the bond stretching, angle bending and dihedral angle constant. While  $r_0, \theta_0, \phi_0$  are the equilibrium bond distance, equilibrium angle and equilibrium dihedral angle.

$$E_{\text{nonbonded}} = E_{\text{Van Der Waals}} + E_{\text{Coulomb}} = \sum \frac{q_i q_j}{4\pi\epsilon_0 r_{ij}} + \sum 4\epsilon_{ij} \left[ \left( \frac{\sigma_{ij}}{r_{ij}} \right)^{12} - \left( \frac{\sigma_{ij}}{r_{ij}} \right)^6 \right] \quad (\text{Eq.3})$$

$q_i, q_j$  are the atomic charges of atom i and j,  $\epsilon_0$  is the effective dielectric constant and  $r_{ij}$  is the distance between atom i and j,  $\epsilon_{ij}$  is the potential well depth and  $\sigma_{ij}$  is the distance between atom i and j at the zero potential energy.

The Van Der Waals interaction between two atoms arises from a balance between repulsive and attractive forces. The van der Waals interaction is most often modeled using the Lennard-Jones potential which expresses the interaction energy using the atom-type dependent constants.

The Coulomb potential represented the electrostatic interaction between a pair of atoms.

The Lennard-Jones potential for diatomic parameters used the Lorentz-Berthelot combining rules following Eq.4 and Eq.5.

$$\sigma_{ij} = \frac{\sigma_i + \sigma_j}{2} \quad (\text{Eq.4})$$

$$\varepsilon_{ij} = \sqrt{\varepsilon_{ii}\varepsilon_{jj}} \quad (\text{Eq.5})$$

### 1.6 Gibbs Ensemble Monte Carlo (GEMC) simulations

Gibbs Ensemble Monte Carlo (GEMC) simulations were performed using homemade software called Gibbon which was already used in [10,12]. This system consisted of two simulation boxes. One box contains bulk gas and another one contains the framework with guest molecules. The particles move within each simulation box. Furthermore, the particles can be swapped between the two boxes and they keep the total number of particles fixed. The chemical potential is equal in both boxes when the system is in equilibrium. The pressure of the system can be chosen by adjustment of the box sizes and the total particles.

### 1.7 Molecular Dynamics (MD) simulations

Molecular dynamics (MD) simulation is the computational calculation which computes the forces acting on each atom using molecular mechanics and force field parameters. In addition, MD updates position and velocity of each atom using Newton's laws of motion following Eq.6 and Eq.7 [13].

$$F_i = m_i a_i \quad (\text{Eq.6})$$

$$F_i = m_i \frac{d^2 r_{it}}{dt^2} \quad (\text{Eq.7})$$

Where  $F_i$  is the force on particle  $i$ ,  $m_i$  is the mass of particle  $i$ ,  $a_i$  is the acceleration on particle  $i$ ,  $r_i$  is the radius of particle  $i$  and  $t$  is the time.

Thermodynamics properties of the system can be described by various ensembles [14].

#### 1.7.1 Microcanonical ensemble

The number of particles ( $N$ ), volume ( $V$ ) and total energy ( $E$ ) are fixed. The system cannot exchange the particles or energy with environment.

#### 1.7.2 Canonical ensemble

The number of particles ( $N$ ), volume ( $V$ ) and temperature ( $T$ ) are fixed. The system can exchange energy with environment.

#### 1.7.3 Grand Canonical ensemble

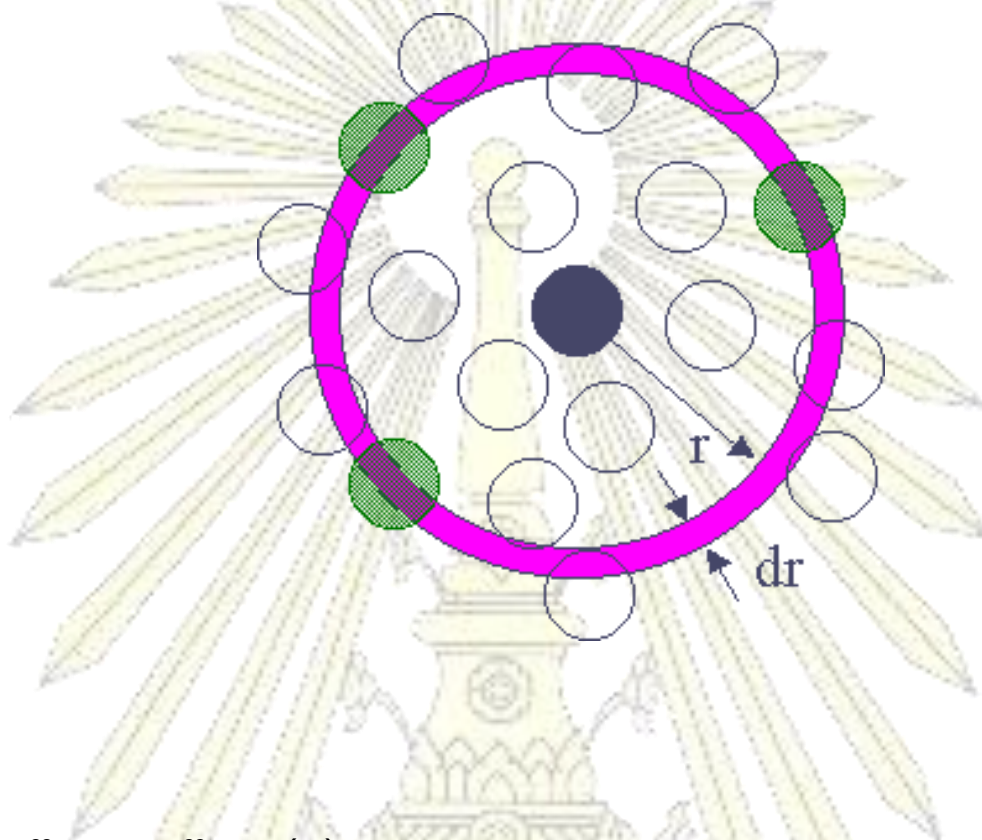
The number of chemical potential ( $\mu$ ), volume ( $V$ ) and temperature ( $T$ ) are fixed. The system can exchange the particles and energy with environment.





### 1.8 Radial Distribution Functions (RDFs)

The radial distribution functions,  $g(r)$  is a tool to describe the structure of a system. It measures the probability to find a particle in the distance ( $r$ ) away from another particle as shown in Fig.2



### 1.9 Self-Diffusion coefficient ( $D_s$ )

The diffusion of the molecules describes the dynamic behavior of guest molecules. Molecular dynamics simulations are used to predict the self-diffusion coefficient by using the Einstein relation [13].

Einstein related the self-diffusion coefficient to the mean square displacement of a particle as a function of observation time.

$$\langle [\vec{r}(t) - \vec{r}(0)]^2 \rangle = 6D_s t \quad (\text{Eq.8})$$

Where  $r$  is the distance at the time  $t$  and  $D$  is diffusion coefficient.

### 1.10 Adsorption, diffusion and membranes selectivities

The effectivity of separation processes can be expressed by the selectivities. They are defined by the following formulas

$$\alpha_{ij}^{adsorption} = \frac{[N_i/N_j]_{adsorbed}}{[N_i/N_j]_{gas}} \quad (\text{Eq.9})$$

$$\alpha_{ij}^{diffusion} = \frac{D_j^{diffusion}}{D_i^{diffusion}} \quad (\text{Eq.10})$$

$$\alpha_{ij}^{membrane} = \alpha_{ij}^{adsorption} \times \alpha_{ij}^{diffusion} \quad (\text{Eq.11})$$

In these formulas  $N_i$  and  $N_j$  denote the total particle numbers of kind  $i$  and  $j$  in the gas phase and in the adsorbed phase, respectively. Their ratio is also the ratio of the concentrations.  $D_i$  and  $D_j$  are the self-diffusion coefficients of kind  $i$  and  $j$ . The membrane selectivity is formed as the product of the adsorption selectivity and the diffusion selectivity [14].

## Chapter 2

### Calculation details

#### 2.1 Simulations

The generated crystal structure of ZIF-67 consists of 64 unit cells ( $4 \times 4 \times 4$ ) and 8 unit cells ( $2 \times 2 \times 2$ ) using for GEMC and MD simulations, respectively. There are seven atom types Co, N, C1, C2, C3, H1 and H2 in the ZIF-67 structure. All positions can be seen in Figure.3

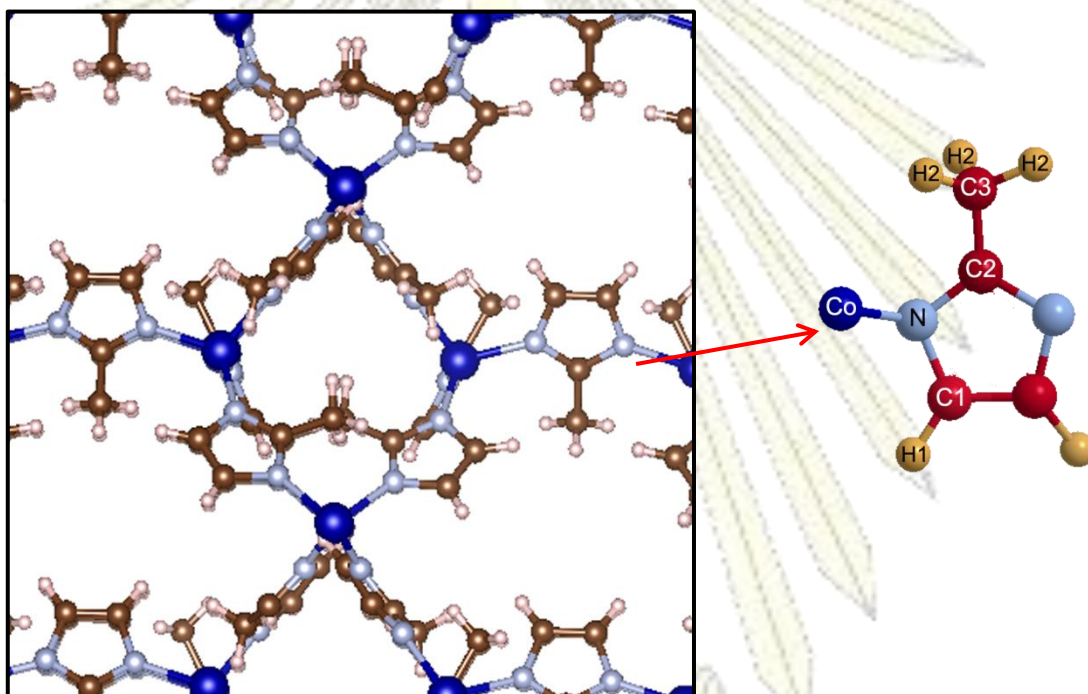


Figure 3 The structure of ZIF-67

### 2.1.1 Force Fields

The force field parameters describe the potential energy of the systems that means bonded and nonbonded interactions. The nonbonded can be described by Coulombic and Lennard-Jones potentials (LJ)

The force field parameters of each atom type in ZIF-67 were taken from AMBER [15] whereas the parameters of Co were taken from two sources AMBER [15] and Li, P. *et. al.* [16] as shown in Table1.

**Table 1** The Lennard-Jones potential parameters of ZIF-67 [15]

Atom type	$\epsilon$ in kcal/mol	$\sigma$ in Å
Co	1.196	2.499
	0.0286 [16]	2.185 [16]
N	0.1700	2.650
C1	0.0860	3.400
C2	0.0860	3.400
H1	0.0150	2.511
C3	0.1094	3.400
H2	0.0157	2.650

The partial charge of atoms in ZIF-67 was taken from Krokidas, P. *et. al.* [17]. The total sum of charges is not equal zero so we adjust charge of some atoms to make the sum to be zero as shown in Table2.

**Table 2** Partial charge of each atom types in ZIF-67

Atom type	Partial charge (q) [17]	Adjust partial charge(q)
Co	1.3497	1.3500
N	-0.6956	-0.6956
C1	-0.0581	-0.0581
C2	0.7846	0.7846
H1	0.0910	0.0910
C3	-0.3094	-0.3094
H2	0.0584	0.0584

The structures of H<sub>2</sub> and N<sub>2</sub> were modeled as united atom. The parameters of H<sub>2</sub> including charge were taken from Hertag, L *et. al.* [3]. While the parameters of N<sub>2</sub> were taken from TraPPE, Potoff *et. al.* [18] with bond length of 1.097 Å.

**Table 3** The Lennard-Jones potential parameters of H<sub>2</sub> and N<sub>2</sub>

	$\sigma$ (Å <sup>o</sup> )	$\epsilon$ (kcal/mol)	q
H <sub>2</sub>	3.314	0.00147	0
N of N <sub>2</sub>	3.310	0.2993	-0.482
X of N <sub>2</sub> (ghost atom)	0	0	0.964
N of N <sub>2</sub>	3.310	0.2993	-0.482

### 2.1.2 Gibbs Ensemble Monte Carlo (GEMC) simulations details

GEMC simulations were used to study adsorption behavior of gas molecules in ZIF. [16] In this work, we applied Gibbs Ensemble Monte Carlo (GEMC) simulations using the so called Gibbon software which was used in many works. This system consisted of 2 simulations boxes. The first box and second box contained the guest molecules and the material and guest molecules, respectively. The molecules can be swapped between 2 boxes and temperatures are equal for each. The pressure can be chosen by adjustment of the size of the boxes and the total number of particles. When the system is in equilibrium, the energy of each box is equal to each other. After equilibrium was reached, the pressures were calculated by the Peng-Robinson equation. Adsorption isotherms of Hydrogen and Nitrogen in ZIF-67 were compared to investigate adsorption behavior and the most suitable Co force fields for the system.



### 2.1.3 Molecular Dynamics (MD) simulations details

MD simulations were used to calculate structure and dynamics properties using DL\_POLY software. The Lorentz-Berthelot mixing rules were used for LJ cross parameters. In this work, we simulated in canonical ensemble (NVT) in which the number of particles in the system (N), volume (V) and temperature are fixed for rigid framework. The simulations were carried out at 3 temperatures (233K, 263K and 303K). The cutoff was chosen to be 12 Å for rigid framework. The self-diffusion coefficient and radial distribution function are discussed in the results part.

**Table 4** The number of particles for each system in MD simulations

Co parameter	Temperature	Number of H <sub>2</sub> particles	Number of N <sub>2</sub> particles
1	233	67	67
	263	37	37
	303	20	20
2	233	53	53
	263	29	29
	303	16	16

## Chapter 3

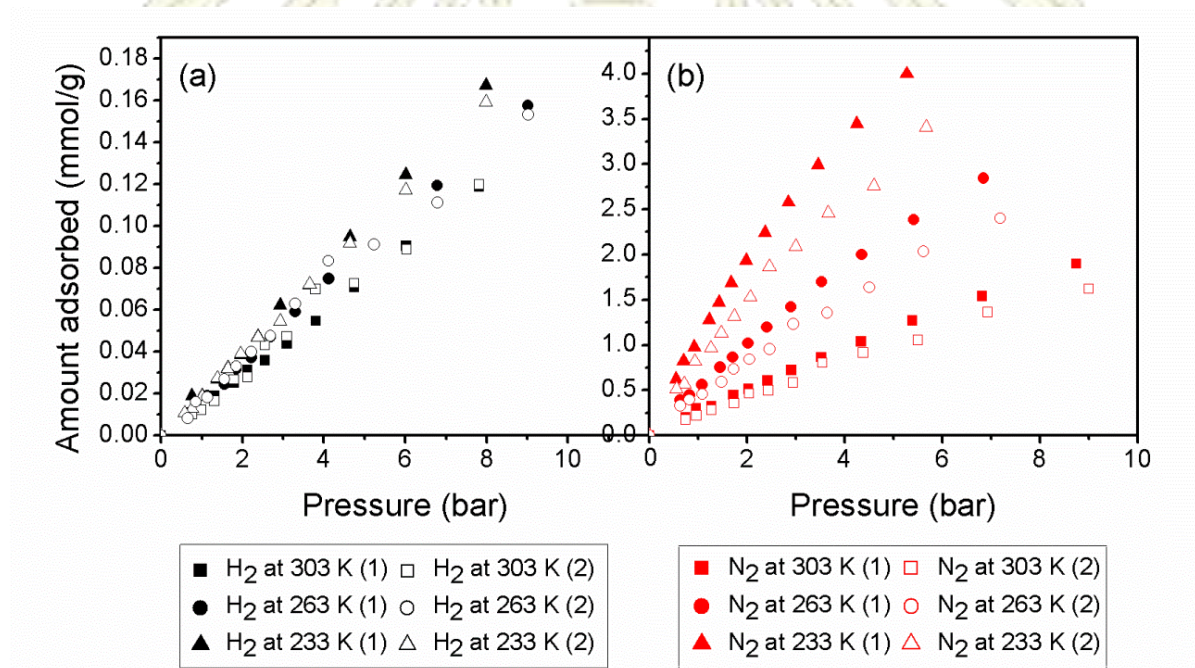
### Results and Discussion

#### 3.1 Gibbon Ensemble Monte Carlo (GEMC)

The adsorption experiments have been done at 233K, 263K and 303K. GEMC simulations were performed for test parameters. The force field parameters of ZIF-67 were taken from AMBER and Li, P. *et. al.* The Co (1) refers to Co parameters taken from AMBER while Co (2) refers to Co parameters taken from Li, P. *et. al.* The parameters of H<sub>2</sub> and N<sub>2</sub> were taken from Hertag, L. *et. al.* and TraPPE, Potoff *et. al.*, respectively. These parameters have been used in MD simulations. The results from GEMC will show the effect of temperature and different Co force field parameters.

#### 3.1.1 Adsorption Isotherm

##### 3.1.1.1 Single gases



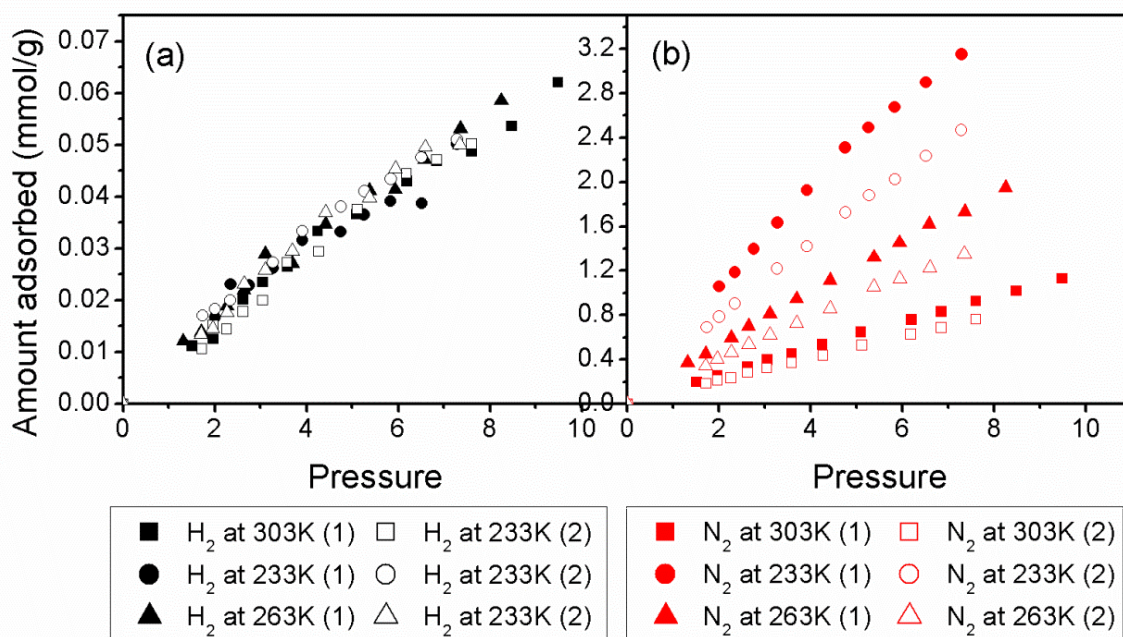
**Figure 4** Adsorption isotherms for single gas (a) H<sub>2</sub> and (b) N<sub>2</sub> at 233K, 263K and 303K in ZIF-67

The results of H<sub>2</sub> and N<sub>2</sub> adsorption isotherms show that force field parameters of H<sub>2</sub> and N<sub>2</sub> can produce the adsorption isotherms. N<sub>2</sub> has the greater amount adsorbed than H<sub>2</sub>.



The temperature effects to adsorption of gases. The amount adsorbed decreases with the increase of temperatures. For the effect of Co force field parameters in  $H_2$ , the amounts adsorbed are not much large. On the other hand, the amounts adsorbed of  $N_2$  in Co (1) are slightly higher.

### 3.1.1.2 Mixtures $H_2/N_2$

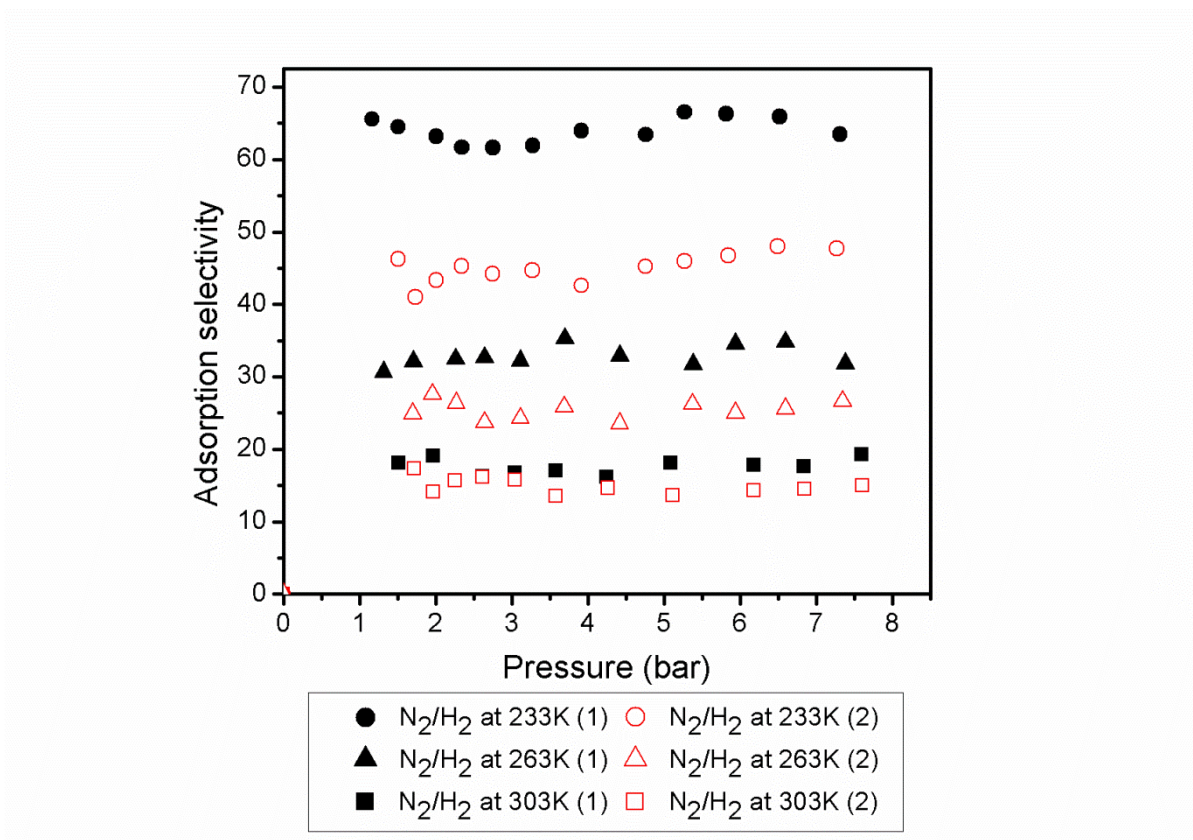


**Figure 5** Adsorption isotherms for mixtures (a)  $H_2$  and (b)  $N_2$  at 233K, 263K and 303K in ZIF-67

From the mixture adsorption isotherms confirms that  $N_2$  adsorbed more than  $H_2$  in ZIF-67. The maximum amount adsorbed for  $H_2$  is 0.0621 mmol/g at 303K while the maximum amount adsorbed for  $N_2$  is 3.1508 mmol/g at 233K. In addition, the temperature and different parameters trend are the same with single gas.

The different parameters trend is the same with single gases that Co (1) and Co (2) do not affect  $H_2$  too large but Co (1) affect  $N_2$  to can be adsorbed slightly more than Co (2).

### 3.1.2 Adsorption Selectivity



**Figure 6** Adsorption selectivity for mixtures N<sub>2</sub>/H<sub>2</sub> at 233K, 263K and 303 K in ZIF-67

We calculated the N<sub>2</sub>/H<sub>2</sub> adsorption selectivity and present to the results in Fig.6. The selectivity varies between 10 and 65, indicating that at all the pressures studied N<sub>2</sub> is preferentially adsorbed in ZIF-67 compared to H<sub>2</sub>. We found that the adsorption selectivity decreases with increasing temperature.

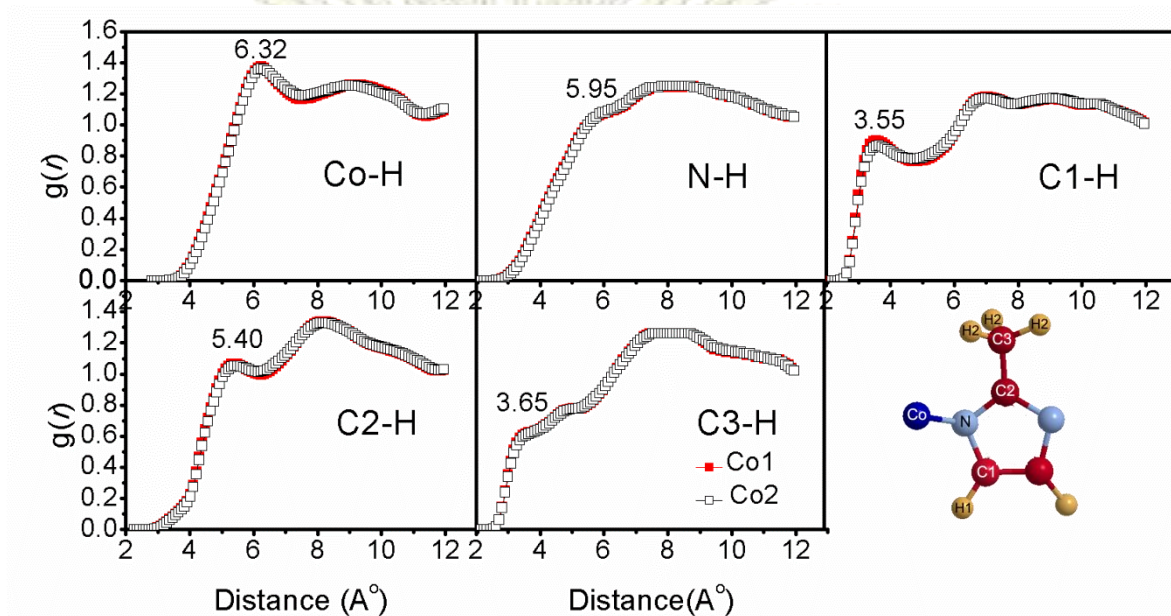
The equilibrium pressures are around 7 bar but rather different. We have taken the particle numbers for MD simulations from the results of the GEMC simulations at around 7 bar. As H<sub>2</sub> can be adsorbed very few amounts so we have chosen the equal particle numbers to N<sub>2</sub>. These particles numbers are: (Co1) 67 H<sub>2</sub> and N<sub>2</sub> at 233K, 37 H<sub>2</sub> and N<sub>2</sub> at 263K, 20 H<sub>2</sub> and N<sub>2</sub> at 303K (Co2) 53 H<sub>2</sub> and N<sub>2</sub> at 233K, 29 H<sub>2</sub> and N<sub>2</sub> at 263K, 16 H<sub>2</sub> and N<sub>2</sub> at 303K, respectively.

## 3.2 Molecular Dynamics (MD) Simulations

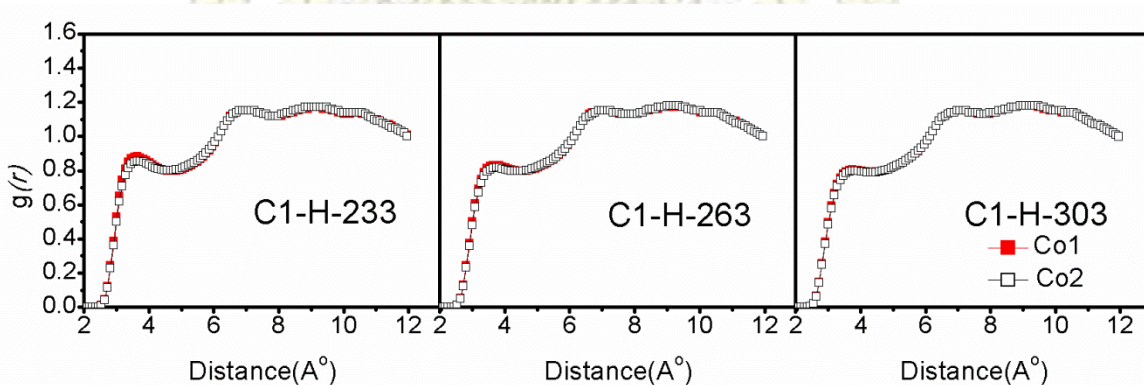
### 3.2.1 Radial Distribution Functions (RDFs)

The Radial Distribution Functions (RDFs) of guest molecules was analyzed to locate the adsorption sites of guest molecules.

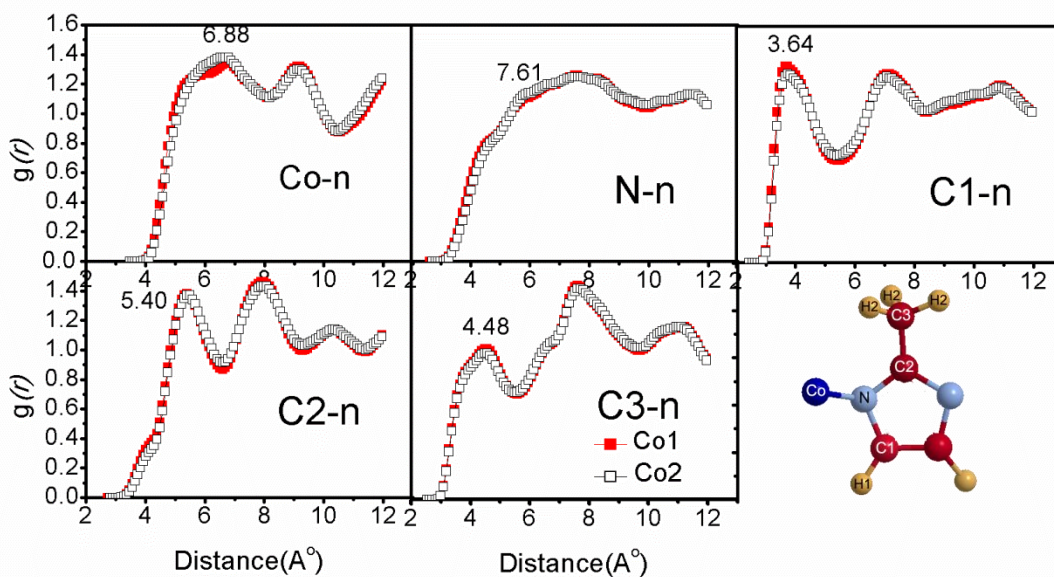
#### 3.2.1.1 Single gases ( $H_2$ and $N_2$ )



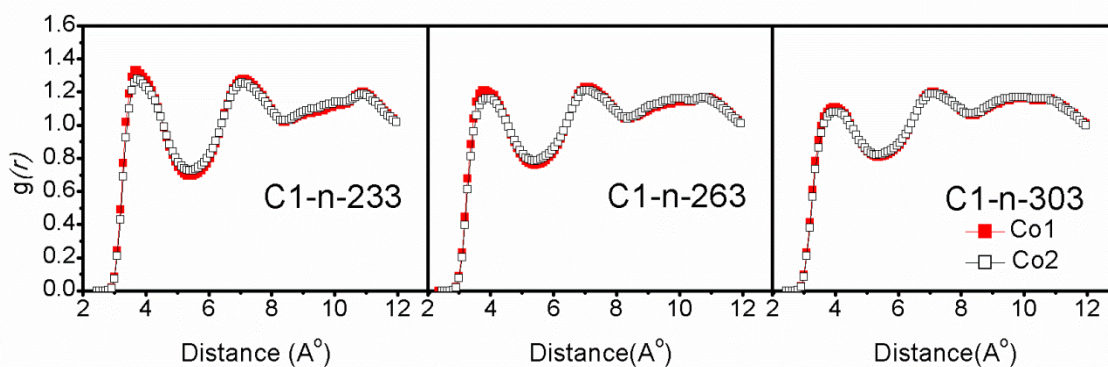
**Figure 7** Radial Distribution Functions (RDFs) between Hydrogen of  $H_2$  and 5 atom types (Co, N, C1, C2, C3) of ZIF-67 at 233K



**Figure 8** Radial Distribution Functions (RDFs) between adsorption site (C1) and Hydrogen of  $H_2$  at 233K, 263K and 303K



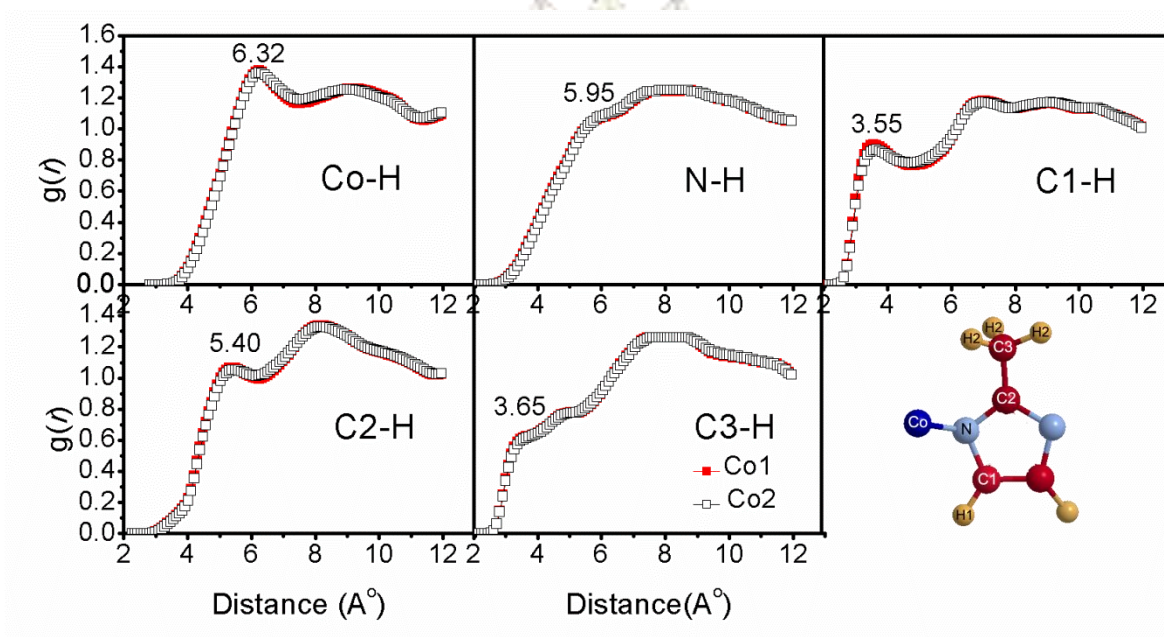
**Figure 9** Radial Distribution Functions (RDFs) between Nitrogen of  $N_2$  and 5 atom types (Co, N, C1, C2, C3) of ZIF-67 at 233K



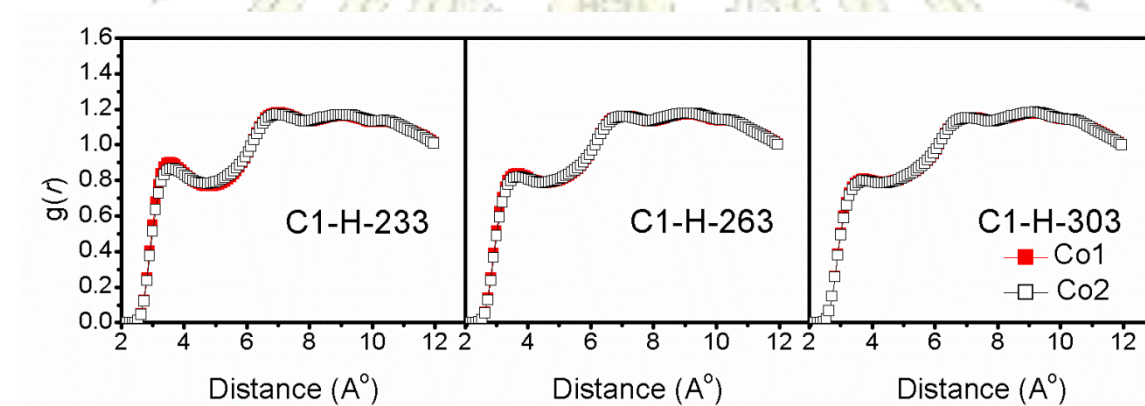
**Figure 10** Radial Distribution Functions (RDFs) between adsorption site (C1) and Nitrogen of  $N_2$  at 233K, 263K and 303K

RDFs of all atom types in ZIF-67 (Co, N, C1, C2, and C3) at 233K were plotted as shown in Fig. 7 and Fig.9. The result shows that C1 was the adsorption site of both ( $H_2$  and  $N_2$ ) which was the shortest distance of all atom types. In addition, the peak between  $N_2$  and C1 was higher than  $H_2$  and C1. That means  $N_2$  shows the stronger contact peaks with C1.

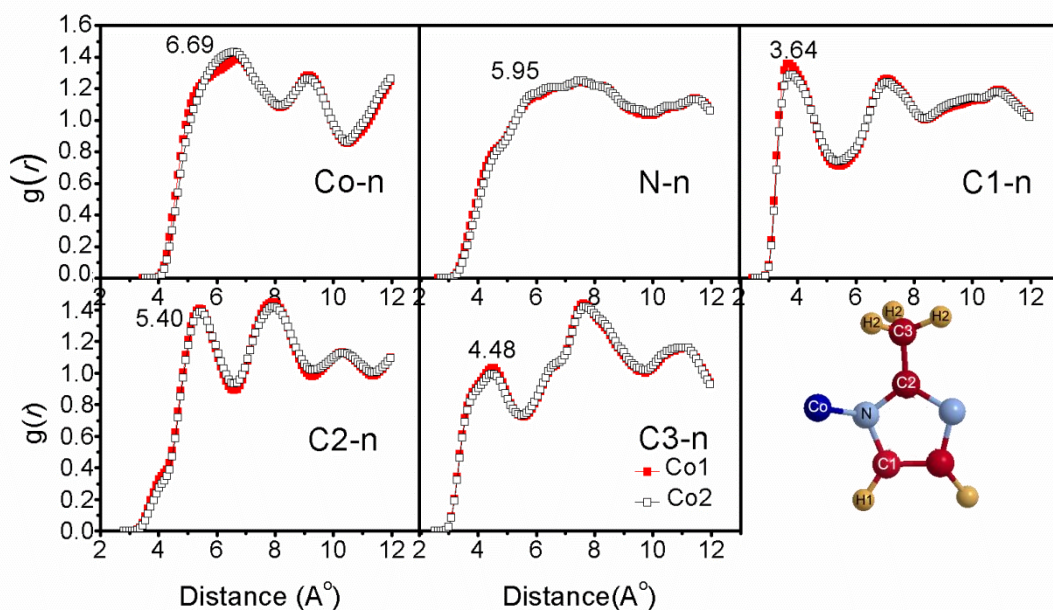
For the effect of different Co force fields parameter, RDFs was not much large. The temperatures did not affect RDFs of  $H_2$  as shown in Fig.8. While Fig. 10 shows a bit effect of temperature on the adsorption sites of  $N_2$ . At the 233K, the adsorption sites had the strong peak more than other temperatures.

3.2.1.2 Mixtures H<sub>2</sub>/N<sub>2</sub>

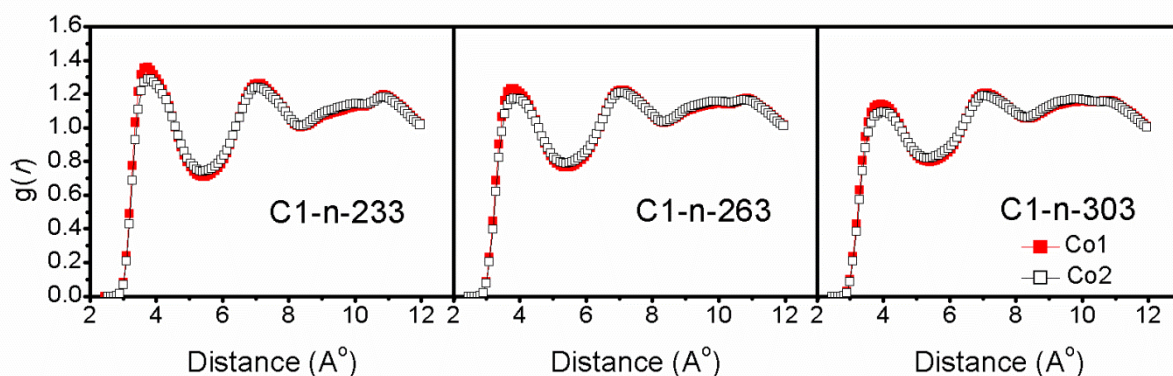
**Figure 11** Radial Distribution Functions (RDFs) between Hydrogen of H<sub>2</sub> in mixtures H<sub>2</sub>/N<sub>2</sub> and 5 atom types (Co, N, C1, C2, C3) of ZIF-67 at 233K



**Figure 12** Radial Distribution Functions (RDFs) between adsorption site (C1) and Hydrogen of H<sub>2</sub> in mixtures H<sub>2</sub>/N<sub>2</sub> in ZIF-67 at 233K, 263K and 303K



**Figure 13** Radial Distribution Functions (RDFs) between Nitrogen of  $N_2$  in mixtures  $H_2/N_2$  and 5 atom types (Co, N, C1, C2, C3) of ZIF-67 at 233K



**Figure 14** Radial Distribution Functions (RDFs) between adsorption site (C1) and Nitrogen of  $N_2$  in mixtures  $H_2/N_2$  in ZIF-67 at 233K, 263K and 303K

RDFs of all atom types in ZIF-67 (Co, N, C1, C2, and C3) at 233K were plotted as shown in Fig.11 and Fig.13. The result shows that C1 was the adsorption site of  $N_2$  of mixtures which produced dominant peaks more than other atom types. For the effect of temperatures and different Co force fields parameter, RDFs were not much different.

The RDFs results showed the same trends of single gases and mixtures. C1 was the preferential adsorption site for both. In addition, the peak between  $N_2$  and C1 was higher than  $H_2$  and C1. That means  $N_2$  shows stronger contact peaks with C1 than  $H_2$ . The RDFs were related to the adsorption isotherms which ZIF-67 can adsorb  $N_2$  more than  $H_2$ .

## 3.2.2 Self-diffusion

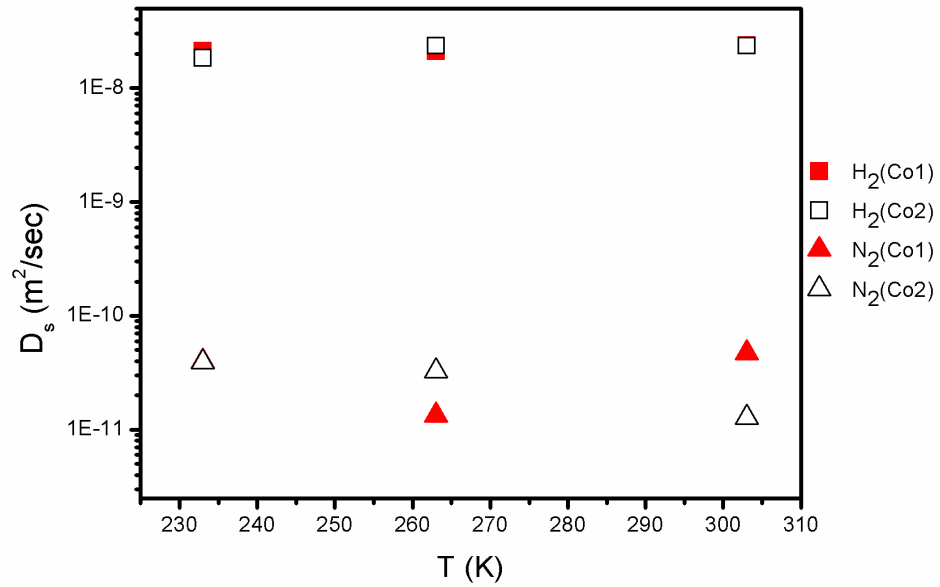


Figure 15 Temperature dependence of the self-diffusion coefficient with  $\ln(D_s)$  versus  $T$  for single gases ( $\text{H}_2$  and  $\text{N}_2$ )

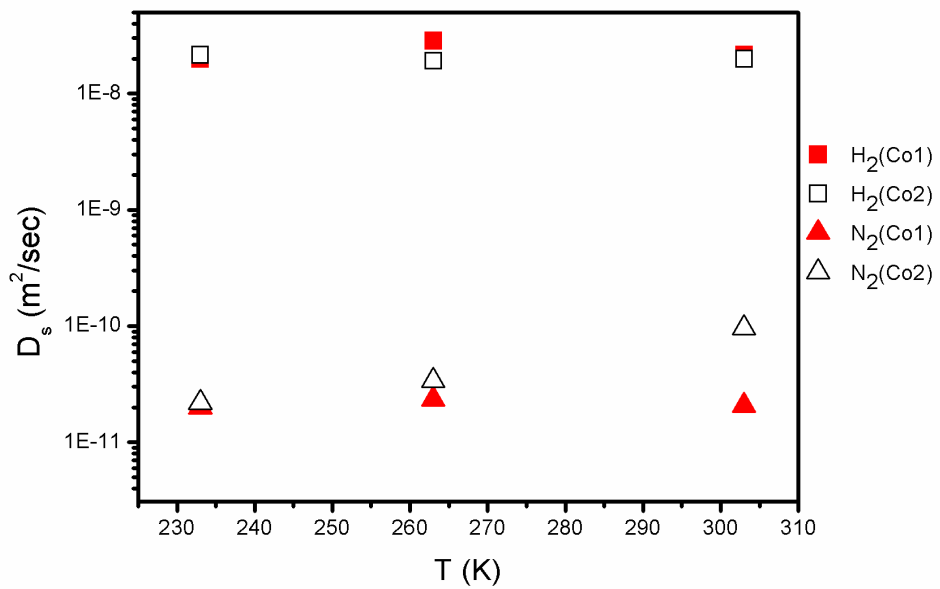


Figure 16 Temperature dependence of the self-diffusion coefficient with  $\ln(D_s)$  versus  $T$  for mixtures  $\text{H}_2/\text{N}_2$

The self-diffusion coefficient ( $D_s$ ) was calculated by the slope of MSD plot. The  $D_s$  of  $H_2$  was higher than the  $D_s$  of  $N_2$  both single gases and mixtures. The results agreed with the theory of diffusion. That is the lower mass can move faster so  $H_2$  move faster than  $N_2$ .

For single gases, the highest  $D_s$  of  $H_2$  is  $2.39 \times 10^{-8} \text{ m}^2/\text{sec}$  at 303K and the highest  $D_s$  of  $N_2$  is  $4.74 \times 10^{-11} \text{ m}^2/\text{sec}$  at 303K. On the site of mixtures, the highest  $D_s$  of  $H_2$  is  $2.86 \times 10^{-8} \text{ m}^2/\text{sec}$  at 263K where the highest  $D_s$  of  $N_2$  is  $9.68 \times 10^{-11} \text{ m}^2/\text{sec}$  at 303K. This results show the higher temperature can move faster that is in line with kinetic energy.

From the  $D_s$  results show the related results of  $D_s$ , RDFs and adsorption isotherms. That was  $N_2$  can be adsorbed more than  $H_2$  in ZIF-67. So it shows the stronger contact with the sharper peak in RDFs and it shows the slower motion with the higher  $D_s$  than  $H_2$ .





### 3.2.3 Adsorption, diffusion and membrane selectivity

The adsorption, diffusion and membrane selectivity were calculated using the Eq.9 , 10 and 11 as shown on page 17.

**Table 5** The adsorption selectivity, diffusion selectivity and membrane selectivity of the N<sub>2</sub>/H<sub>2</sub> mixture in ZIF-67 using Co (1)

T (K)	Pressure (bar)	Adsorption selectivity ( $\alpha_{ij}^{adsorption}$ )	Diffusion selectivity ( $\alpha_{ij}^{diffusion}$ )	Membrane selectivity ( $\alpha_{ij}^{membrane}$ )
233	7.2907	63.46	0.001000	0.06346
263	7.3604	31.842	0.000822	0.02616
303	7.5982	19.299	0.000967	0.01867

**Table 6** The adsorption selectivity, diffusion selectivity and membrane selectivity of the N<sub>2</sub>/H<sub>2</sub> mixture in ZIF-67 using Co (2)

T (K)	Pressure (bar)	Adsorption selectivity ( $\alpha_{ij}^{adsorption}$ )	Diffusion selectivity ( $\alpha_{ij}^{diffusion}$ )	Membrane selectivity ( $\alpha_{ij}^{membrane}$ )
233	7.2662	47.722	0.001014	0.04838
263	7.3467	26.606	0.001776	0.04725
303	7.6036	14.967	0.004864	0.07280

The results of Table 7 and 8 show the same trends for two Co parameter sources. The separation at lower temperature is more effective. The adsorption selectivity is somewhat larger than the membrane selectivity. So we can predict that ZIF-67 is well suited to separate H<sub>2</sub> from N<sub>2</sub>.

## Chapter 4

### Conclusions

Adsorption and diffusion of single gases ( $H_2$  and  $N_2$ ) and  $H_2/N_2$  mixtures in rigid ZIF-67 was examined by Gibbs Ensemble Monte Carlo (GEMC) simulations and Molecular Dynamics (MD) simulations at three temperatures. Our adsorption isotherms results indicate that ZIF-67 can adsorb  $N_2$  in higher amount than  $H_2$ . The amount adsorbed decreases with the increase in temperatures. The different Co force field parameters do not affect significantly the gas absorption, except at lower temperatures. The selectivity decreases with increasing temperature. From the Radial Distribution Functions (RDFs), the shortest distance between the gas molecule and ZIF-67 was found at C1 position of ZIF-67 around 3.55 Å. It can be summarized that C1 was the preferential adsorption site. In addition, the RDFs peak between  $N_2$  and C1 were higher than  $H_2$  and C1. This suggests that  $N_2$  shows stronger contact peaks with C1 than  $H_2$ . In order to observe the dynamics behavior of gases, the self-diffusion ( $D_s$ ) was calculated. It was found that  $N_2$  had the lower  $D_s$  than  $H_2$ . That means  $N_2$  moves slower than  $H_2$ . Finally, it can be concluded that ZIF-67 is well suited to separate  $H_2$  from  $N_2$ , especially at lower temperature.

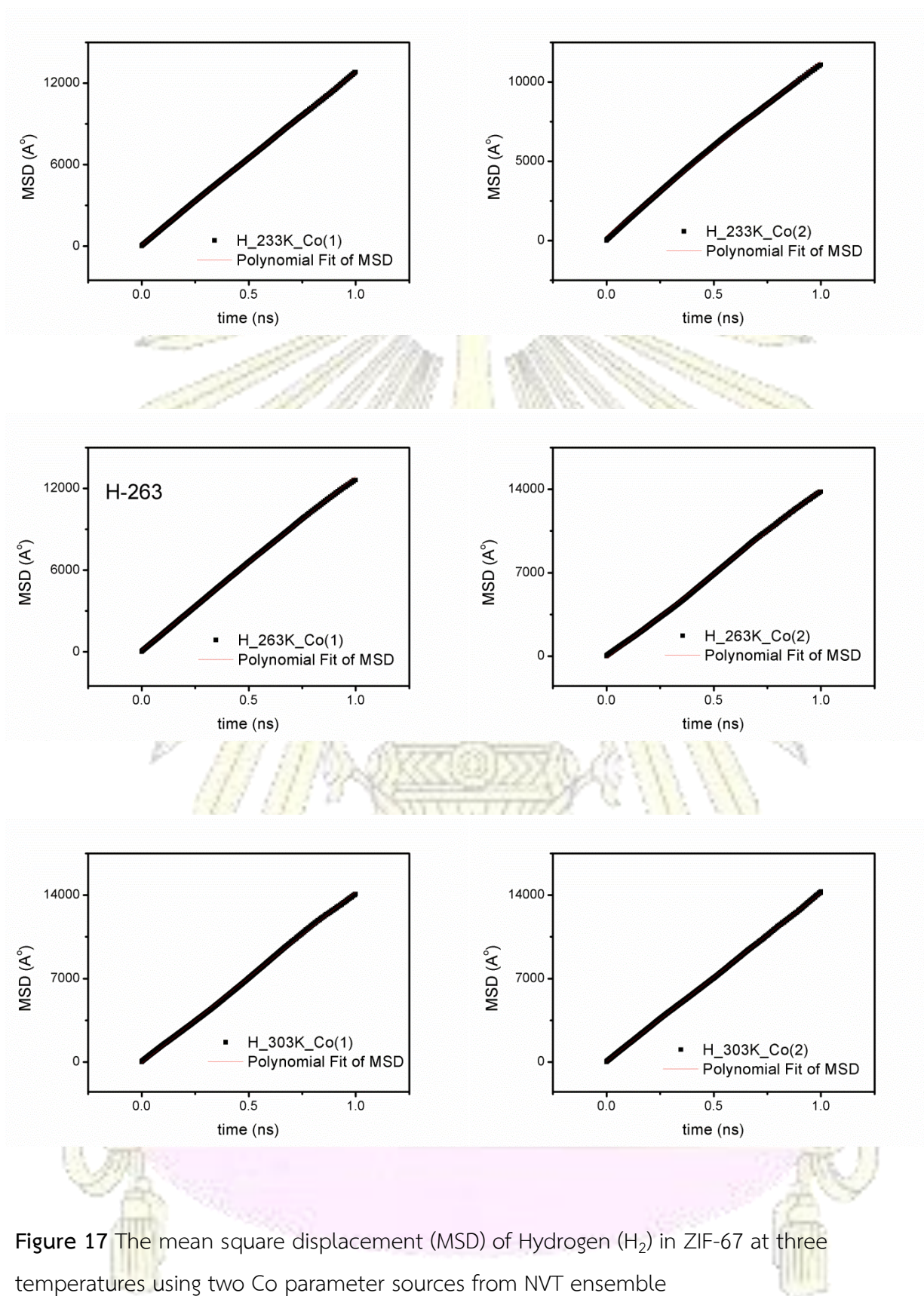


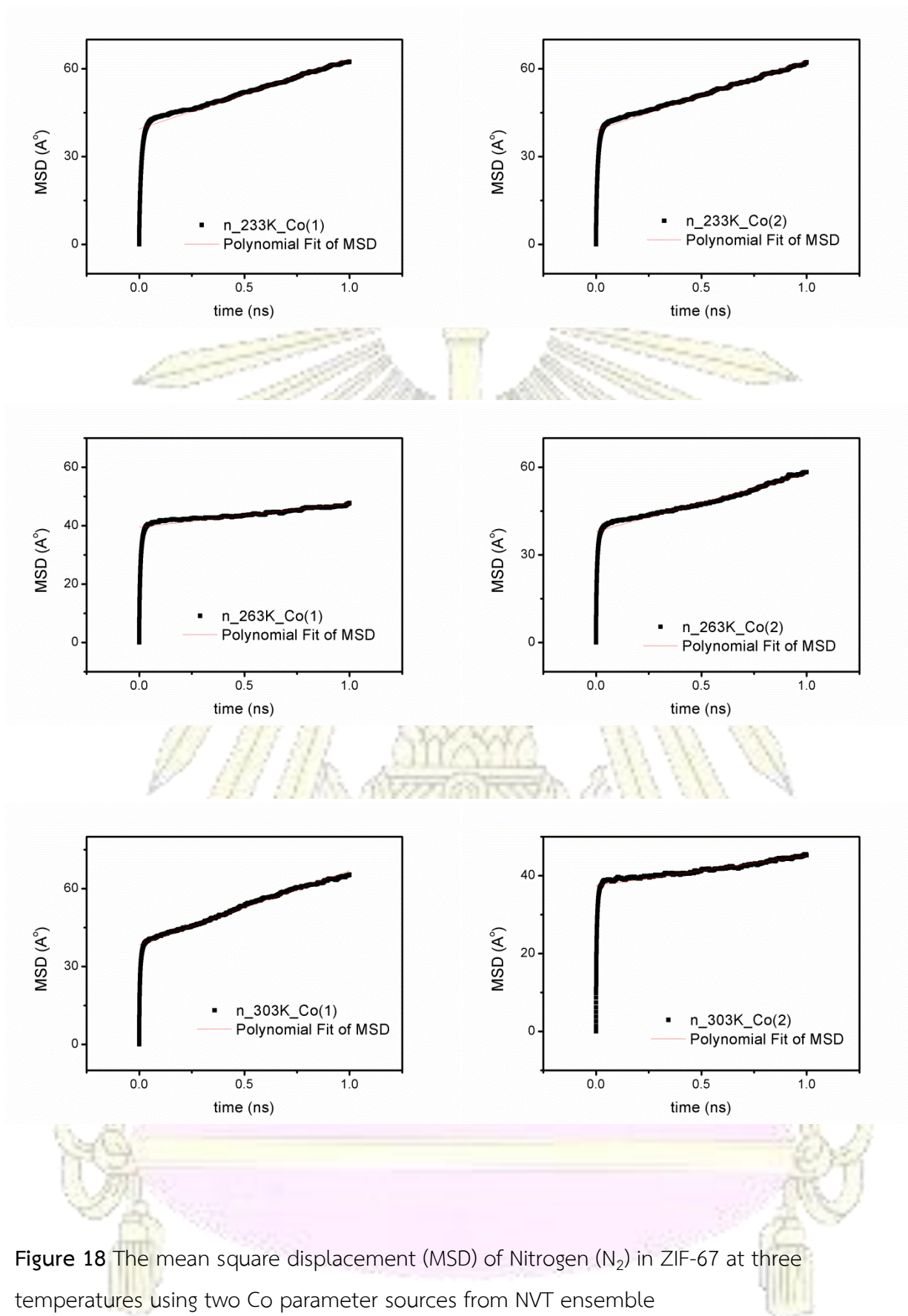
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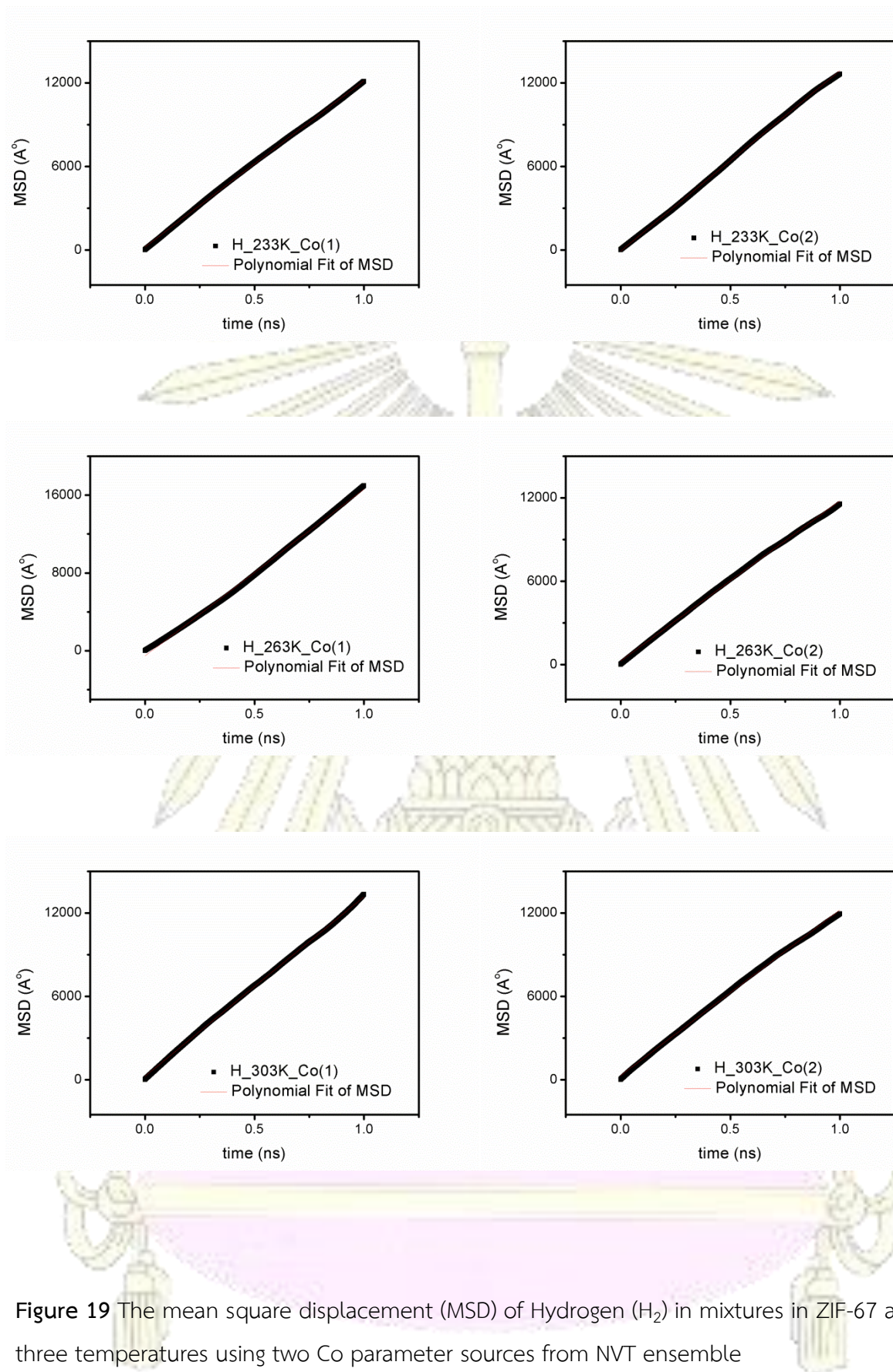
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## Appendix





**Figure 18** The mean square displacement (MSD) of Nitrogen ( $N_2$ ) in ZIF-67 at three temperatures using two Co parameter sources from NVT ensemble



**Figure 19** The mean square displacement (MSD) of Hydrogen ( $H_2$ ) in mixtures in ZIF-67 at three temperatures using two Co parameter sources from NVT ensemble

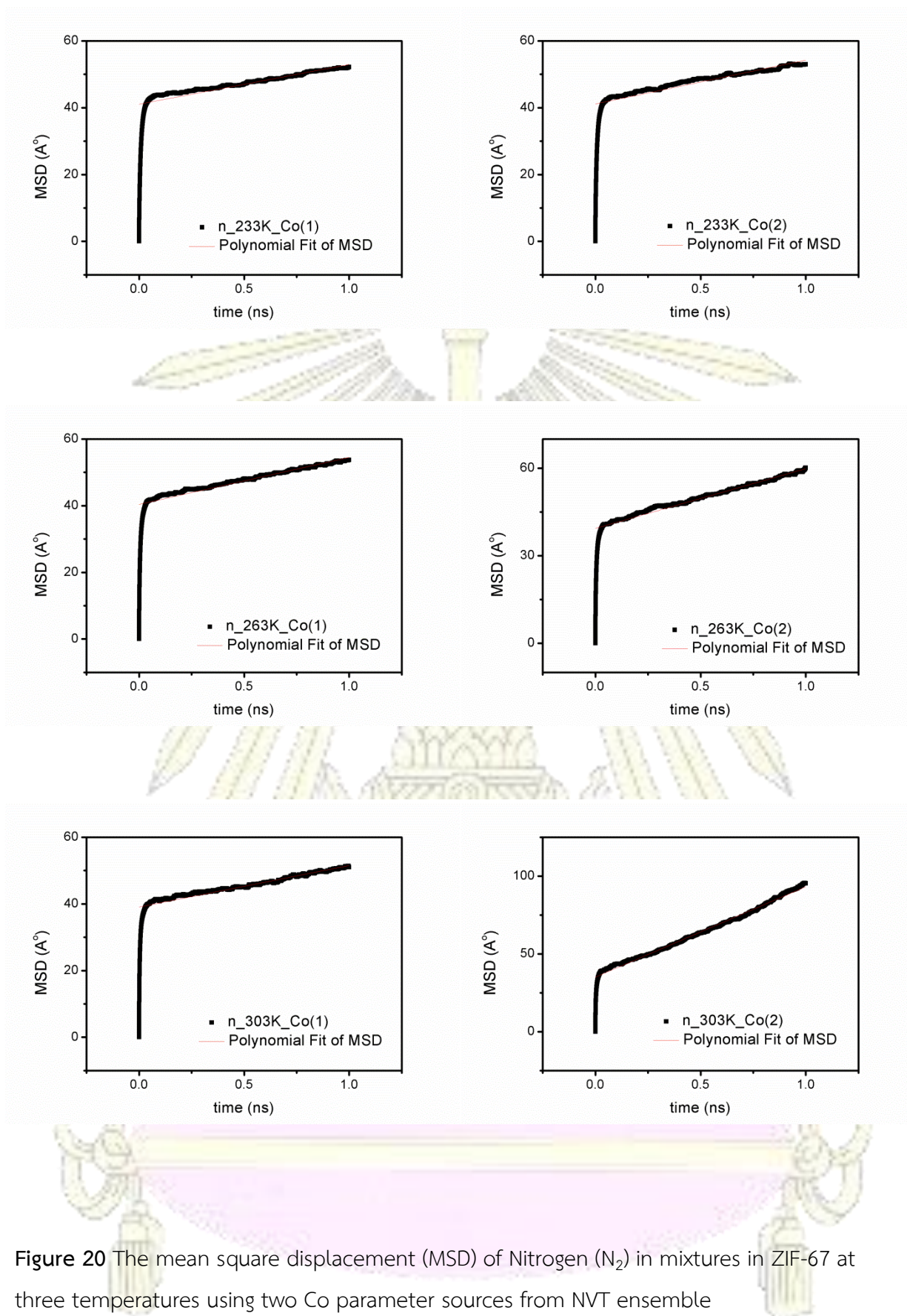


Figure 20 The mean square displacement (MSD) of Nitrogen ( $N_2$ ) in mixtures in ZIF-67 at three temperatures using two Co parameter sources from NVT ensemble



**Table 7** The self-diffusion coefficient ( $D_s$ ) of single gases ( $H_2$  and  $N_2$ ) in ZIF-67 at three temperatures

T(K)	Co parameter	Pressure(bar)	$D_s$ of $H_2$ ( $m^2/sec$ )	$D_s$ of $N_2$ ( $m^2/sec$ )
233	1	7.2907	$2.12 \times 10^{-8}$	$3.99 \times 10^{-11}$
	2	7.2662	$1.84 \times 10^{-8}$	$3.92 \times 10^{-11}$
263	1	7.3604	$2.12 \times 10^{-8}$	$1.34 \times 10^{-11}$
	2	7.3467	$2.36 \times 10^{-8}$	$3.28 \times 10^{-11}$
303	1	7.5982	$2.39 \times 10^{-8}$	$4.74 \times 10^{-11}$
	2	7.6036	$2.36 \times 10^{-8}$	$1.28 \times 10^{-11}$

**Table 8** The self-diffusion coefficient ( $D_s$ ) of mixtures in ZIF-67 at three temperatures

T(K)	Co parameter	Pressure(bar)	$D_s$ of $H_2$	$D_s$ of $N_2$ ( $m^2/sec$ )
233	1	7.2907	$1.99 \times 10^{-8}$	$1.99 \times 10^{-11}$
	2	7.2662	$2.16 \times 10^{-8}$	$2.19 \times 10^{-11}$
263	1	7.3604	$2.86 \times 10^{-8}$	$2.35 \times 10^{-11}$
	2	7.3467	$1.92 \times 10^{-8}$	$3.41 \times 10^{-11}$
303	1	7.5982	$2.15 \times 10^{-8}$	$2.08 \times 10^{-11}$
	2	7.6036	$1.99 \times 10^{-8}$	$9.68 \times 10^{-11}$

## Curriculum Vitae

Miss Chanunchida Kunsiri was born on December 3<sup>rd</sup>, 1995 in Suphanburi, Thailand. In 2013, she graduated from Mathematics-Science program from Kannasootsuksalai School, Suphanburi, Thailand. In 2014, she was admitted to a Bachelor's degree program: major in Chemistry, Faculty of Science and minor in Faculty of Communication Arts, Chulalongkorn University. She would complete the program in 2018. Her address is 77 Moo 13, Tambon Hnong-ong, Amphoe U-Thong, Suphanburi 72160.

