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**APPENDIX**



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## **APPENDIX A**

### **The Method of Controlling Oxygen Pressure Using CO/CO<sub>2</sub> Gas Mixtures.**

The oxygen pressure in the experimented furnace was controlled by using the CO/CO<sub>2</sub> gas mixtures. A controlled oxygen pressure can be obtained by mixing various quantities of CO and CO<sub>2</sub> to maintain constant oxygen pressure. The method of calculating the CO/CO<sub>2</sub> ratio is based on;

- I. The Gibbs Free Energy of CO, CO<sub>2</sub> gas mixture;
- II. Dalton's Law;
- III. Le Chatelier's Principle.

#### **I. The Gibb Free Energy of CO/CO<sub>2</sub> Gas Mixtures**

The reaction of mixture of CO, O<sub>2</sub> and CO<sub>2</sub> at constant pressure and temperature can be written, as in equation (A1)



The standard Gibbs free-energy change for this reaction is represented as follows;

$$\Delta G^\circ = -RT \ln [P^2_{CO_2} / (P^2_{CO} \cdot P_{O_2})] \quad (A2)$$

$$= -135000 + 41.4T \quad \text{Calories} \quad (A3)$$

The oxygen pressure can be determined from equation [A4]

$$\mu(O_2) = RT \ln [P_{O_2}] \quad (A4)$$

( $\mu(O_2)$  is a oxygen potential, Kcal)

Floyd *et al* (1979) and Kemori (1986) have studied the oxygen pressure in flash furnace and indicated that the oxygen pressure occurring in flash furnace are between -60 to -40 Kcal. Therefore, the oxygen potential equal -60, -50, -40 Kcal were selected and used for the study.

## II. Dalton's Law

The sum of the partial pressure  $P_i$  of the components in the system is equal to the total pressure  $P_T$ .

$$P_T = P_i + P_{ii} + \dots + P_{ith} \quad (A5)$$

### III. Le Chatelier's principle

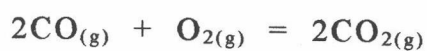
Consider a closed system in which a reversible reaction is taking place at constant pressure and temperature. Whenever a system at equilibrium is subjected to a change in one of the variables, temperature or pressure, the system will shift the composition of the equilibrium in the direction in which there is a decrease in the number of molecules.

For the reversible reaction  $2\text{CO}_{(g)} + \text{O}_{2(g)} = 2\text{CO}_{2(g)}$ , if initially the gases mixture consists of  $x$  g.mole of CO,  $y$  g.mole of  $\text{CO}_2$  and  $y > x$ . Let  $\xi$  represents the number of gram-moles of  $\text{CO}_2$  that decompose at equilibrium. Therefore, equation (A1) can be written as;



From the Gibbs free energy, Dalton's Law, and Le Chatelier's principle, the ratio of  $P_{\text{CO}}/P_{\text{CO}_2}$  can be determined as follows;

The equilibrium of CO,  $\text{CO}_2$  and  $\text{O}_2$  can be written as;



$$\Delta G^\circ_{[C1]} = -135,000 + 41.4T \quad \text{Calories}$$



$$\Delta G^\circ_{[C1]} = -RT \ln[P^2_{CO_2} / (P^2_{CO} \cdot P_{O_2})]$$

Thus,

$$RT \ln[P^2_{CO_2} / (P^2_{CO} \cdot P_{O_2})] = 135,000 - 41.4T$$

$$RT \ln[P^2_{CO_2} / (P^2_{CO})] = 135,000 - 41.4T + \mu(O_2)$$

$$P_{CO_2} / P_{CO} = \sqrt{e^{(135,000 - 41.4T + \mu(O_2))/RT}} \quad (A7)$$

Thus, the composition of CO, CO<sub>2</sub> and O<sub>2</sub> can be determined by using equations (A5), (A7) and substituting  $\mu(O_2) = -40, -50, \text{ and } -60$  Kcal,  $T = 298$  K in equation (A7).

Since the increment of temperature affects the composition of initial equilibrium, the composition of the new equilibrium at a higher temperature can be calculated by using equations (A3) and (A6) to determine  $\xi$ . The initial and equilibrium composition,  $\xi$  and oxygen potential at given temperature (1350, 1400, and 1450 °C) are shown in Table A1. The composition of CO and CO<sub>2</sub> at given temperatures were selected to control oxygen pressure in the furnace.

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Table A1 The composition of CO and CO<sub>2</sub> gas mixtures at ambient and given temperature and oxygen pressure.

T° C	%CO <sub>2ini</sub>	%CO <sub>ini</sub>	ξ	%CO <sub>2T</sub>	%CO <sub>T</sub>	μ(O <sub>2</sub> ) Kcal
1350	0.1	99.9	1.64x10 <sup>-7</sup>	0.1	99.9	-41.91
1350	0.5	99.5	6.48x10 <sup>-9</sup>	0.5	99.5	-50.57
1350	2	98	3.94x10 <sup>-10</sup>	2	98	-58.08
1350	15	85	5.3x10 <sup>-12</sup>	15	85	-69.64
1400	0.2	99.8	2.46x10 <sup>-7</sup>	0.2	99.8	-42.33
1400	0.6	99.6	9.67x10 <sup>-9</sup>	0.6	99.6	-51.34
1400	5	95	3.56x10 <sup>-10</sup>	5	95	-60.52
1400	7	93	1.58x10 <sup>-11</sup>	7	93	-69.18
1450	1	99	5.16x10 <sup>-8</sup>	1	99	-48.34
1450	7	93	9.28x10 <sup>-10</sup>	7	93	-59.92
1450	8	92	6.96x10 <sup>-10</sup>	8	92	-60.75
1450	30	70	2.86x10 <sup>-11</sup>	30	70	-69.94

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## APPENDIX B

### Microstructure of Accretions.



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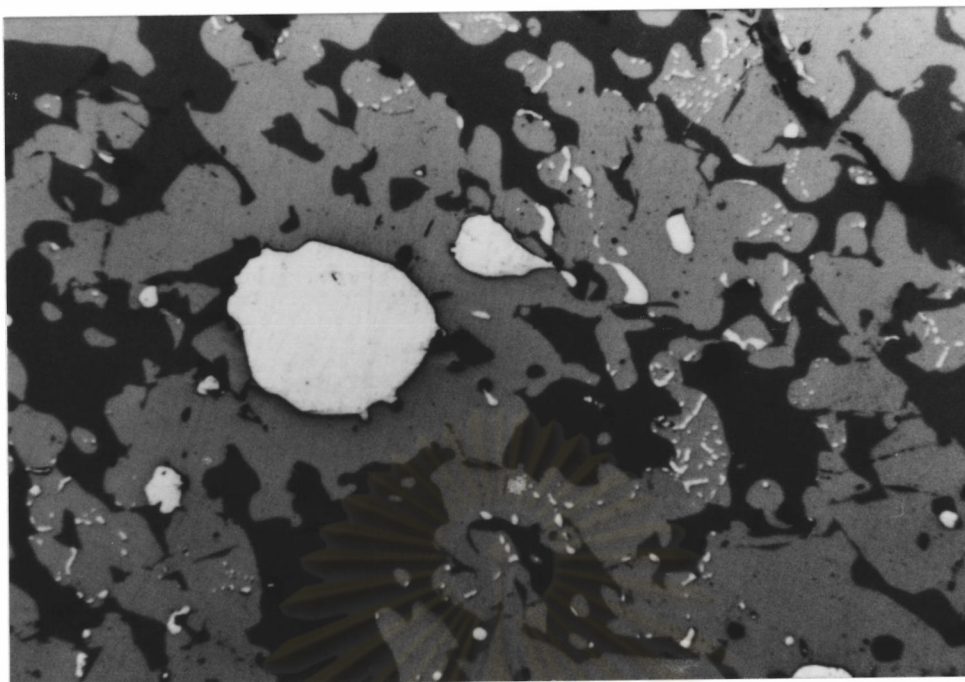


Figure B1 Microstructure of G-3 sample shows the large spherical particle of nickel sulphide, nickel metal formed rim around  $\text{Fe}_3\text{O}_4$  spinel, x200.

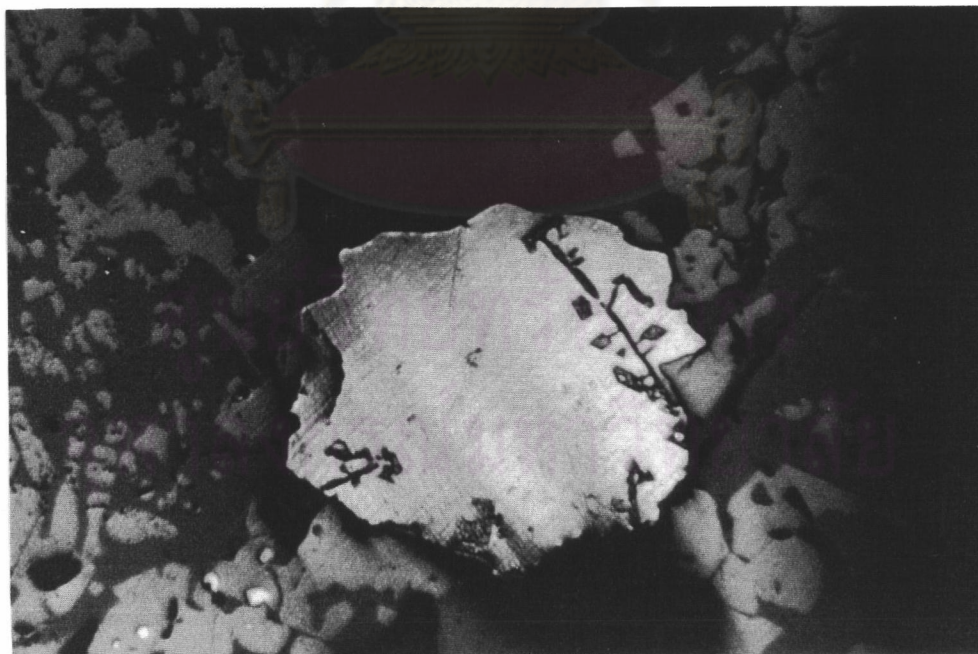


Figure B2 Nickel metal formed in the nickel sulphide of G-3 sample, x200.



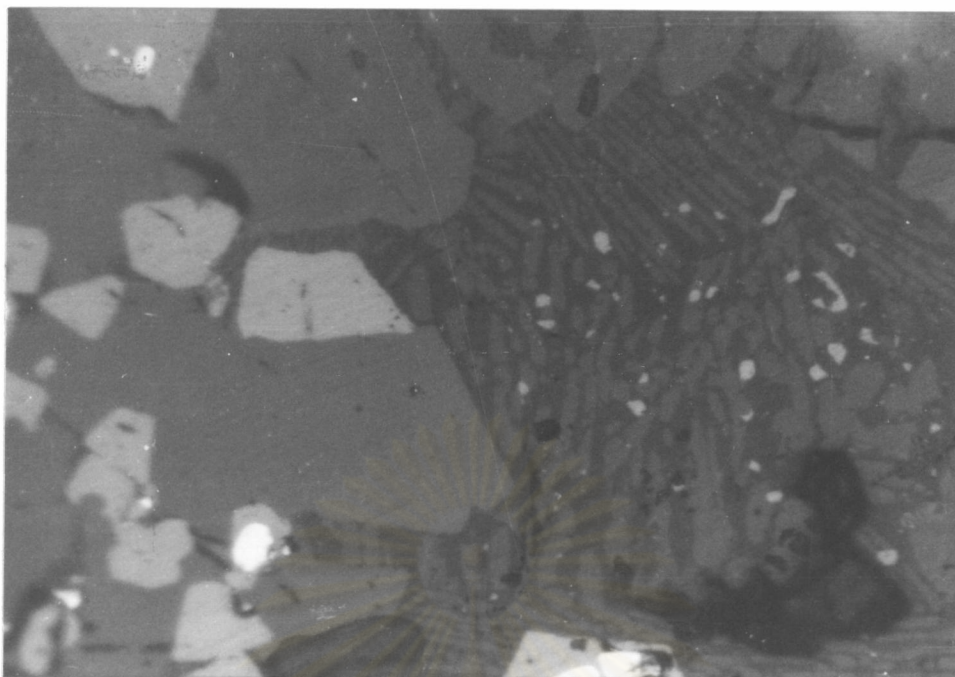


Figure B3 Microstructure of G-3 sample shows the lamellar Structure, large grain of nickel sulphide, small particle of nickel metal, x200.

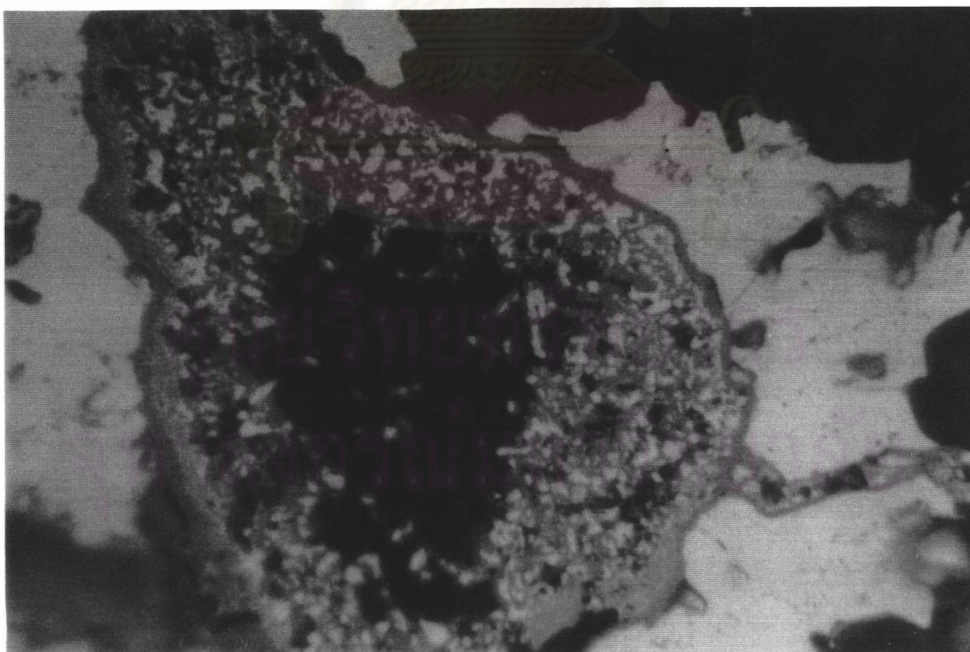


Figure B4 Unknown structure was found in G-4 sample, 500.



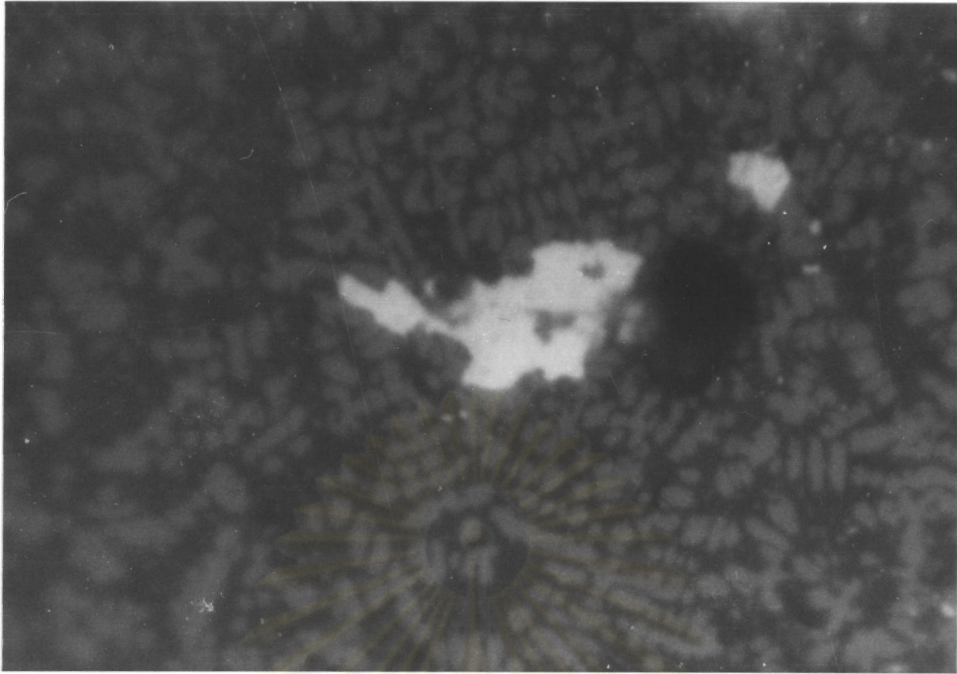


Figure B5 Dendritic structure of  $\text{Fe}_3\text{O}_4$  spinel of G-4 sample, x500.



Figure B6 Ternary eutectic structure of  $\text{FeO-Fe}_2\text{SiO}_4\text{-Fe}_2\text{O}_3$  and dendritic structure in H-32 sample, x500.

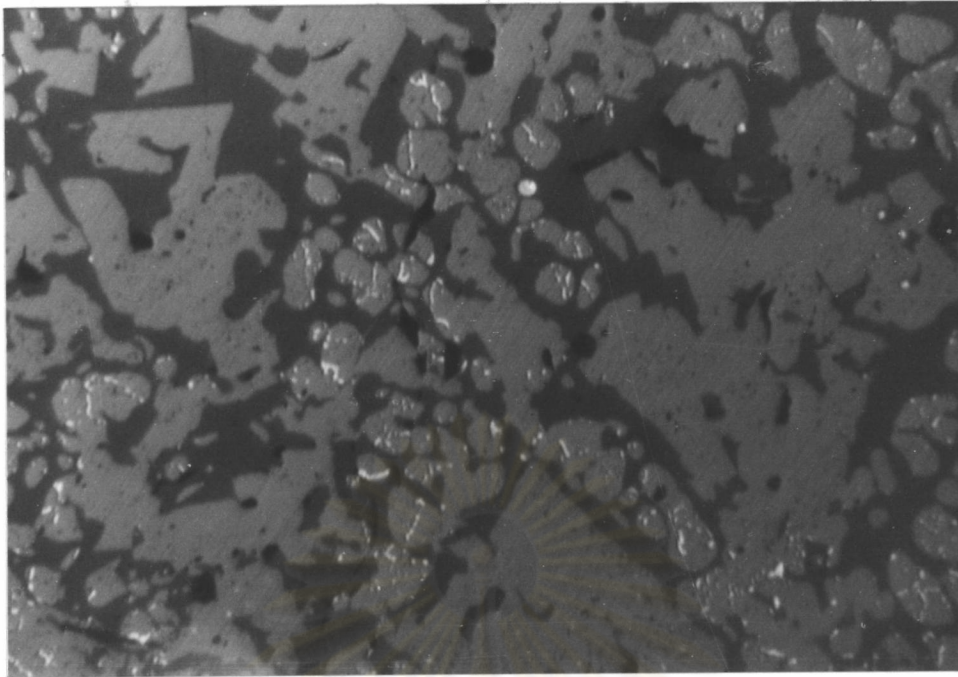


Figure B7 Nickel metal form rims around  $\text{Fe}_3\text{O}_4$  spinel, H-34 sample, x100.

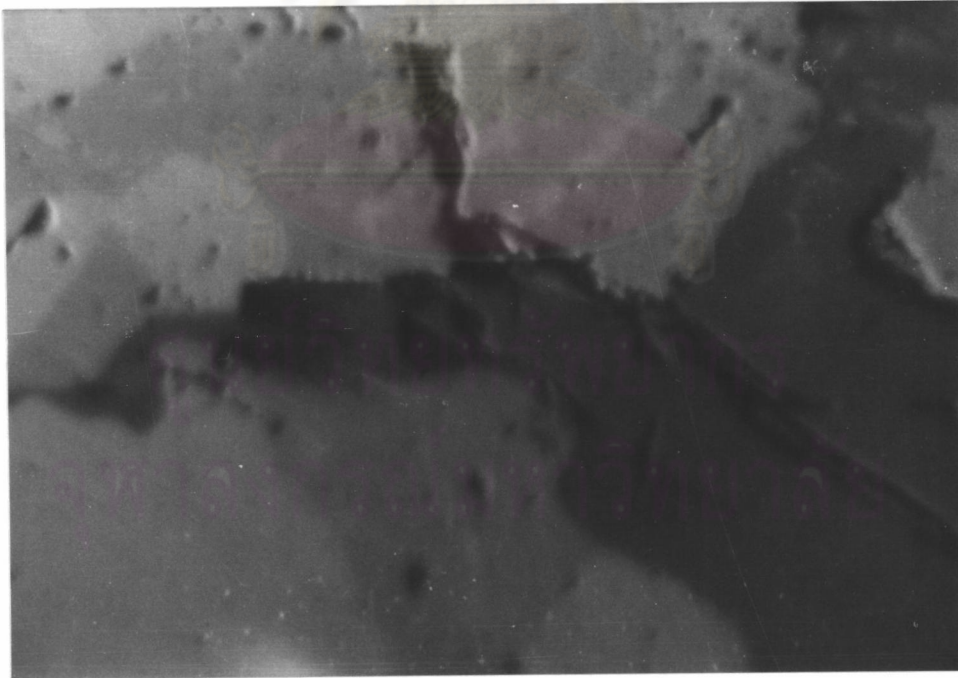


Figure B8 Wustite (light phase) was found in the  $\text{Fe}_3\text{O}_4$  spinel, H-34 sample, x 500.

## BIOGRAPHY

Mr. Maetee Sujiwatthana was born on September 15, 1969 in Bangkok, Thailand. He received his B. Eng. in Metallurgical Engineer from Chulalongkorn University in 1991. He has 4 year experiences in metal melting. He has been working for master degree in Metallurgical Engineer at Chulalongkorn University since 1992.



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