การแยกสิ่งเจือปนจากน้ำในหอทคลองแบบฟลูอิไคซึ่งคอลัมน์



นางสาว กัลยา วิริยะศิริวัฒนะ

วิทยานิพนธ์นี้เป็นส่วนหนึ่งของการศึกษาตามหลักสูตรปริญญาวิทยาศาสตร์มหาบัณฑิต ภาควิชาเคมีเทคนิค บัณฑิตวิทยาลัย จุฬาลงกรณ์มหาวิทยาลัย พ.ศ. ๒๕๒๓

REMOVAL OF IMPURITIES FROM WATER IN FLUIDIZING COLUMN

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การแยกสิ่งเจือปนจากน้ำในหอทคลองแบบฟลูอิไดซึ่งคอลัมน์ นางสาว กัลยา วิริยะศิริวัฒนะ รองศาสตราจารย์ คร.พล สาเกทอง

ภาควิชา

เคมีเหคนิค

ปีการศึกษา

belob

บทคัดยอ

งานวิจัย เป็นการใช้ เทคนิคของฟลูอิได เซชั่นในการศึกษาการดูคซับในสาร ละลาย สารละลายที่ใช้ มีทั้งสารละลายที่มีตัวถูกทำละลายเคี่ยว และผสม สารดูคซับ ที่ใช้คือ แอกติเว เทคการ์บอนซนิด เอส จี แอล และสารถูกคูดซับที่ใช้ในการหคลองคือ ฟอร์บอลดีไฮด์ โซเดียมไฮดรอกไซด์ โซเดียมคาร์บอเนต และสารผสมระหว่างโซเดียม ไฮดรอกไซด์ กับโซเดียมคาร์บอเนต

รากการทคลองพบว่า ความเข้มข้นของสารละลายความเร็วของสารละลาย ที่ไหลเข้าสู่ระบบ และชนาคของสารดูคซับจะมีความสัมพันธ์กับอัตราการถายเทมวลของ สารถูกดูคซับ และคำสัมประสิทธิ์การถายเทมวลสาร

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ABSTRACT

The technique of fluidization was applied to a study of adsorption in liquid phase. Adsorption of both single-solute solution and multi-solute solution were studied. Granular activated carbon SGL type was chosen as adsorbent, formaldehyde, sodium hydroxide, Sodium carbonate and mixture of sodium hydroxide and sodium carbonate as adsorbates.

By experimental investigation, concentration of aqueous solution, velocity of liquid stream and particle size of accorbent are related to mass transfer rate and mass transfer coefficient. Moreover the ralation between Reynolds number and mass transfer coefficient for each adsorbate is also presented graphically.

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CONTENTS

				Pag
Abstrac	t (Th	nai)		iv
Abstrac	t (Er	nglish)		v
Acknowl	edgen	nent		vi
List of	Tabl	es	अविभाजा ने रे	vi
List of	Figu	res	A STATE OF THE STA	x
				xv
Chapter			Townsoaman and the state of the	
I	INTE	ODUCTIO	N	1
II	LITE	RATURE	REVIEWS AND THEORETICAL CONSIDERATION	
	2.1	Adsorb	ents	4
	2.2	Adsorp	tion	11
		2.2.1	Equilibrium Adsorption	11
		2.2.2	Adsorption in Liquid Phase	19
		2.2.3	Kinetic Adsorption	23
	2.3	Fluidi	zation	25
		2.3.1	Definition	25
		2.3.2	Phenomenon of Fluidization	25
		2.3.3	Pressure Drop	28
		2.3.4	Minimum Fluidizing Velocity	29
			2.3.4.1 Definition	29
			2.3.4.2 Calculation of Minimum	
			Fluidizing Velocity	29
		2.3.5	Adsorption in Fluidized Column	32

Chapter			Pag
III	APPI	ARATUS AND EXPERIMENTAL METHODS	34
	3.1	Apparatus	34
	3.2	Equilibrium Adsorption	37
		3.2.1 Equilibrium Adsorption of Formaldehyde	37
		3.2.2 Equilibrium Adsorption of Sodium Hydroxide	
		3.2.3 Equilibrium Adsorption of Sodium Carbonate	
		3.2.4 Equilibrium Adsorption of the Mixture of Sodium Hydroxide and Sodium	
		Carbonate	38
	3.3	Preparing of Adsorbent	
		3.3.1 Sieve Analysis	39
		3.3.2 Soaking of Activated Carbon	40
	3.4	Determination of Calibration Curve	40
	3.5	Determination of Minimum Velocity of Fluidization	40
	3.6	The Effect of Variables on Adsorption	41
IV	EXPE	CRIMENTAL RESULTS	
	4.1	Mass Transfer Rate	44
		4.1.1 Effect of Concentration of Solute	44
		4.1.2 Effect of Particle Size of Activated	
		Carbon	44
		4.1.3 Effect of Feed Rate	45
	4.2	Mass Transfer Coefficient	l.e

е

Chapter			Page
		4.2.1 Effect of Modified Reynolds Number	48
		4.2.2 Effect of Surface Area	48
V	DISC	USSION	
	5.1	Some Considerations on the Selection of	,
		Adsorbent and Adsorbates	86
	5.2	Equilibrium Adsorption	86
		5.2.1 Equilibrium Adsorption of	
		Formaldehyde	87
		5.2.2 Equilibrium Adsorption of Sodium	
		Hydroxide and Sodium Carbonate in	
		Single-Solute Aqueous Solution	87
		5.2.3 Equilibrium Adsorption of Mixture	
		of Sodium Hydroxide and Sodium	
		Carbonate	87
	5.3	Effect of Variables on Cumulative Uptake	
		of Solute on Activated Carbon and Mass	
		Transfer Rate	88
		5.3.1 Effect of Concentration of Solute	88
		5.3.2 Effect of Size of Activated Carbon	90
		5.3.3 Effect of Feed Rate	91
	5.4	Variation of External Mass Transfer	
		Coefficient with Some Variables	92
		5.4.1 Effect of 1/s	92
		5.4.2 Effect of Rep	93
		5.4.3 Effect of Co	93
VI	CONC	LUSION	94
REFERENC	E		97
APPENDIX			103

		Page
A	EQUILIBRIUM ISOTHERM AND SOME CHARACTERISTICS	
	OF FLUIDIZED BED	103
В	EXPERIMENTAL DATA FOR ADSORPTION	113
C	NUMERICAL RESULTS	123
D	SAMPLE OF CALCULATION	127
VITA .		130

LIST OF TABLE

Tabl	Le	
		Page
2.1	Industrial Adsorbents	4
2.2	Economic Consideration of Activated Carbon	10
2.3	Heat of Physical Adsorption and Chemisorption	12
3.1	Distribution Size of Activated Carbon	39
3.2	Experimental Schedule of Formaldehyde	42
3.3	Experimental Schedule of Sodium Hydroxide	42
3.4	Experimental Schedule of Sodium Carbonates	43
3.5	Experimental Schedule of the mixture of Sodium	.,
	Hydroxide and Sodium Carbonate	43
A-1	Equilibrium Isotherm of Formaldehyde	103
A-2	Equilibrium Isotherm of Sodium Hydroxide	105
A-3	Equilibrium Isotherm of Sodium Carbonate	107
1-4	Equilibrium Isotherm of the Mixture of Sodium	107
	Hydroxide and Sodium Carbonate	109
A-5	Data for Calibration Curve of Rotameter	111
A-6	Variation of Pressure Drop with Velocity	112
B-1	Experimental Data for Adsorption of Formaldehyde at	
	Various Concentrations of Feed for q = 1,260 cm ³ /min,	
	$d_p = 0.100 \text{ cm}$	113
B-2	Experimental Data for Adsorption of Formaldehyde at	
	Various Concentrations of Feed for q = 1,600 cm/min,	
	$d_{p} = 0.076 \text{ cm}$	113

е

Table	e	Pag
B-3	Experimental Data for Adsorption of Formaldehyde at	
	Various Concentrations of Feed for q = 1,780 cm ³ /min,	
	$d_{p} = 0.076 \text{ cm}$	11
B-4	Experimental Data for Adsorption of Formaldehyde	
	at Various Concentrations of Feed for q = 1,260 cm ³ /mi	n.
	$d_{p} = 0.076 \text{ cm}$	114
B-5	Experimental Data for Adsorption of Formaldehyde	
	at Various Concentrations of Feed for q = 1,440 cm/min	in the second
	$d_{p} = 0.076 \text{ cm}$	114
B-6	Experimental Data for Adsorption of Formaldehyde	777
	at Various Sizes of Activated Carbon	
B-7		115
,	Experimental Data for Adsorption of Sodium Hydroxide at Various Concentrations of Feed	
D 0		116
B-8	Experimental Data for Adsorption of Sodium Hydroxide	
	at Various Sizes of Activated Carbon	116
B-9	Experimental Data for Adsorption of Sodium Hydroxide	
	at Various Feed Rates	117
B-10	Experimental Data for Adsorption of Sodium Carbonate	
	at Various Concentrations of Feed for q = 1,600 cm/min	,
	$d_{p} = 0.119 \text{ cm}$	118
B-11	Experimental Data for Adsorption of Sodium Carbonate	
	at Various Concentrations of Feed for q = 1,600 cm ³ min	
	$d_{p} = 0.100 \text{ cm}$	118
B-12	Experimental Data for Adsorption of Sodium Carbonate	
	at Various Sizes of Activated Carbon	119
3-13	Experimental Data for Adsorption of Sodium Carbonate	
	at Various Feed Rates	119
3-14	Experimental Data for Adsorption of the Mixture of	
	Sodium Hydroxide and Sodium Carbonate at Various	
	Concentrations of Feed	120

Table		Page
B-15	Experimental Data for Adsorption of the Mixture of	
	Sodium Hydroxide and Sodium Carbonate at Various	
	Sizes of Activated Carbon	121
B-16	Experimental Data for Adsorption of the Mixture of	
	Sodium Hydroxide and Sodium Carbonate at Various	
	Feed Rates	122
C-1	Numerical Results for Adsorption of Formaldehyde	123
C-2	Numerical Results for Adsorption of Sodium	
	Hydroxide	124
C-3	Numerical Results for Adsorption of Sodium	
	Carbonate	125
C-4	Numerical Results for Adsorption of the Mixture	
	of Sodium Hydroxide and Sodium Carbonate	126

विश्वतिभाषान्त्र

LIST OF FIGURES

Figure	NO DELINIAL SALVE	
		Page
2.1	Effect of Adsorbent Preparation on Adsorption Isotherm	
2 2		15
2.2	Effect of Carbon Dosage on Uptake of Phenol	15
2.3	The Five Types of Adsorption Isotherm in the	
	Classification of BET	15
2.4	The Four Types of Adsorption Isotherm for	
	Liquid Phase	17
2.5	Adsorption Isotherm of Krypton on Carbon	
	Graphitized at 2700°C	17
2.6	Constant Concentration Uptake of Dye	20
2.7	Isotherms for p-Nitrophenol Adsorption from	
	a Mixture	20
2.8	Various Kinds of Contacting of a Batch of Solids	
	by Fluid	27
2.9	Experimental Determination of Minimum Fluidizing	
	Velocity U _{mf}	200
3.1	Experimental Equipment	27
3.2		35
	Schematic Diagram of Adsorption Unit	36
4.1a-4.	To capacity (m) with	
	Time (t) for Adsorption of Formaldehyde at Various	
	Concentrations of Feed	49
+.2	Variation of Adsorptive Capacity (m) with Time (t)	
	for Adsorption of Sodium Hydroxide at Various	
	Concentrations of Feed	54

Figur	е	Page
4.3a-	4.3b Variation of Adsorptive Capacity (m) with	
	Time (t) for Adsorption of Sodium Carbonate	
	at Various Concentrations of Feed	55
4.4	Variation of Adsorptive Capacity (m) with	
	Time (t) for Adsorption of the Mixture of	
	Sodium Hydroxide and Sodium Carbonate at	
	Various Concentrations of Feed	57
4.5	Variation of Adsorptive Capacity (m) with Time(t)	
	for Adsorption of Formaldehyde at Various Sizes	
	of Activated Carbon	58
4.6	Variation of Adsorptive Capacity (m) with	
	Time (t) for Adsorption of Sodium Hydroxide	
	at Various Sizes of Activated Carbon	50
4.7		59
(Variation of Adsorptive Capacity (m) with	
	Time (t) for Adsorption of Sodium Carbonate	
1, 0	at Various Sizes of Activated Carbon	60
4.8	Variation of Adsorptive Capacity (m) with	
	Time (t) for Adsorption of the Mixture of	
	Sodium Hydroxide and Sodium Carbonate at Various Si	zes of Carbon
4.9	Variation of Adsorptive Capacity (m) with	61
	Time (t) for Adsorption of Formaldehyde at	
	Various Feed Rates.	62
4.10	Variation of Adsorptive Capacity (m) with	
	Time (t) for Adsorption of Sodium Hydroxide	
	at Various Feed Rates	63
+.11	Variation of Adsorptive Capacity (m) with	
	Time (t) for Adsorption of Sodium Carbonate	
	at Various Feed Rates	64

Figur	re	Page
4.12	Variation of Adsorptive Capacity (m) with Time (t) for Adsorption of the Mixture of Sodium Hydroxide and Sodium Carbonate at	
	Various Feed Rates	65
4.13	Effect of Concentration (C _o) on Mass Transfer Rate (M) for Adsorption of Formaldehyde on Activated Carbon	66
4.14	Effect of Concentration (C) on Mass Transfer Rate (M) for Adsorption of Sodium Hydroxide on	
4,15	Activated Carbon Effect of Concentration (C _o) on Mass Transfer Rate (M) for Adsorption of Sodium Carbonate	67
4.16	on Activated Carbon Effect of Concentration (C ₀) on Mass Transfer Rate (M) for Adsorption of the Mixture of Sodium Hydroxide and Sodium Carbonate on	68
4.17	Activated Carbon Effect of Size of Activated Carbon (d _p) on Mass Transfer Rate (M) for Adsorption of Formaldehyde on Activated Carbon	69
4.18	Effect of Size of Activated Carbon (dp) on Mass Transfer Rate (M) for Adsorption of Sodium	70
4.19	Hydroxide on Activated Carbon Effect of Size of Activated Carbon (dp) on Mass Transfer Rate (M) for Adsorption of Sodium	71
4.20	Carbonate on Activated Carbon Effect of Size of Activated Carbon (dp) on Mass Transfer Rate (M) for Adsorption of the Mixture	72
	of Sodium Hydroxide and Sodium Carbonate on Activated Carbon	73

Figure		Page
4.21	Effect of Velocity (u) on Mass Transfer Rate (M) for Adsorption of Formaldehyde on Activated Carbon	mi
4.22	Effect of Velocity (u) on Mass Transfer Rate (M)	74
	for Adsorption of Sodium Hydroxide on Activated Carbon	75
4.23	Effect of Velocity (u) on Mass Transfer Rate (M) for Adsorption of Sodium Carbonate on Activated	
4.24	Effect of Velocity (u) on Mass Transfer Rate (M)	7.6
	for Adsorption of the Mixture of Sodium Hydroxide and Sodium Carbonate on Activated Carbon	
4.25	Effect of Rep on Mass Transfer Coefficient (k) for	77
4.26	Adsorption of Formaldehyde on Activated Carbon Effect of Rep on Mass Transfer Coefficient (k) for	.78
	Adsorption of Sodium Hydroxide on Activated Carbon	79
4.27	Effect of Rep on Mass Transfer Coefficient (k) for Adsorption of Sodium Carbonate on Activated Carbon	80
4.28	Effect of Rep on Mass Transfer Coefficient (k) for Adsorption of the Mixture of Sodium Hydroxide and	
	Sodium Carbonate on Activated Carbon	8,1
4.29	Effect of 1/S on Mass Transfer Coefficient (k) for Adsorption of Formaldehyde	8.2
4.30	Effect of 1/S on Mass Transfer Coefficient (k) for Adsorption of Sodium Hydroxide on Activated Carbon	83
4.31	Effect of 1/S on Mass Transfer Coefficient (k) for	0,2
4.32	Adsorption of Sodium Carbonate on Activated Carbon Effect of 1/S on Mass Transfer Coefficient (k) for	84
	Adsorption of the Mixture of Sodium Hydroxide and Sodium Carbonate on Activated Carbon	- 85

		xiv
Figur	re	Page
A-1	Equilibrium Adsorption of Formaldehyde	104
A-2	Equilibrium Adsorption of Sodium Hydroxide	,
A-3	Equilibrium Adsorption of Sodium Carbonate	106
A-4	Equilibrium Adsorption of the Mixture of Sodium Hydroxide and Sodium Carbonate	108
A-5	Calibration Curve of Rotameter	110
A-6		111
	Variation of Pressure Drop (\triangle P) with Velocity (u)	112

NOMENCLATURE

Symbols	Definitions	Dimensions
a	Constant in Langmuir Equation for Liquid phase	-
(a _v) _c	Surface area of adsorbent per volume of bed	L^2/L^3
A	Constant in Freundlich equation for Liquid phase	-
b	Constant in Langmuir equation for Liquid phase	_
C	Bulk concentration of Liquid phase	ML-3
Co	Concentration of solute in influent to bed	ML-3
c _s	Saturated concentration	ML-3
C*	Concentration of solute at solid surface side of interfacial film	ML ⁻³
d _p	Average diameter of particle	L
ā	Constant in BET equation	
fm	Friction factor, a function of Rep	- 130
G	Fluid superficial mass velocity base on emp	oty MT ⁻¹ L ⁻²
Ga	Galileo number	
g	Accereration of gravity	LT-2
kf	Mass transfer coefficient by external diffusion	LT-1
k _p	Mass transfer coefficient by internal diffusion	LT-1
L	Height of bed	L
L _{mf}	Bed height at minimum fluidizing condition	L

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Symbols	Definitions	Dimensions
M	Mass transfer rate	$_{\mathrm{MM}}$ -l $_{\mathrm{T}}$ -l
m	Mass adsorbate per unit mass of adsorbent	M/M
^m c	Mass of adsorbent	M
m _{H2} O	Mass of water	M
m*	Mass adsorbate per unit mass of adsorbent at equilibrium with c*	M/M
N	Normality	ML-3
n	Constant in Frundlich equation	_
n*	Exponent a function of the modified	- 10 <u>-</u> 15 -
	Reynolds number Rep, dimensionless	_1 _2
þ	Fluid pressure	$ML^{-1}T^{-2}$ $ML^{-1}T^{-2}$
ΔP	Pressure drop	ML-1T-5
po	Vapor pressure	ML ⁻¹ T ⁻²
q	Volumetric flow rate	L3T-1
Rep	Modified Reynolds number	-
Remf	Modified Reynolds number at minimum fluidizing condition	7 -
r	Radius of spherical particle	L
F p	The mean pore radius A°	L
S	Surface area per unit mass of adsorbent	LM-1
T	Absolute temperate	t
t	Time	T
u	Velocity of fluid	LT-1
umf	Velocity of fluid at minimum fluidizing condition	LT-1
Vp	Pore Volume of adsorbent	L ³

Symbols	Definitions	Dimensions
Vpores	Volume of pore in fluidized bed	L ³
E	Void fraction in a bed	
€ mf	Void fraction in a bed at minimum fluidizing conditions	-
M	Viscosity of fluid	_{ML} -1 _T -1
f	Density of fluid	ML-3
ſs	Density of solid	_{ML} -3
Ø	Shape factor	_