ADSORPTIVE REMOVAL OF SULFUR COMPOUNDS FROM TRANSPORTATION FUELS BY USING ZEOLITIC ADSORBENTS

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ABSTRACT

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This research work was conducted to study the modification of NaY zeolite by ion-exchanging with selected transition metal ions (Cu2+, Ni2+) in order to enhance the capacities of adsorbents for adsorptive removal of refractory sulfur compounds which are difficult to remove by using conventional methods. The efficiencies of the Cu(II)Y and NiY zeolites in removing model sulfur compounds (3-methylthiophene, benzothiophene and dibenzothiophene) from simulated transportation fuels such as isooctane and decane were examined and systematically related to type and amount of metal loading by batch method at ambient conditions. The amount of metal loading on both CuY and NiY zeolites was varied by using different amount of metal solution to NaY zeolite ratio. The results showed that the adsorption isotherms were well fitted with Langmuir isotherm. From the results, CuY zeolite showed markedly high adsorptive capacities in adsorbing 3-MT, BT and DBT than NiY and NaY zeolites. The adsorption capacity of CuY zeolite was directly proportional to the amount of Cu2+ loading instead of NiY zeolite which had low Ni2+ dependency. The difference in adsorption capacities was probably due to the effect of pore size of zeolite after exchanged with transition metals.

บทคัดย่อ

ทรงพล พริ้งประยงค์ : การกำจัดสารประกอบกำมะถั่นออกจากน้ำมันเชื้อเพลิงโดยการ ดูคซับบนใช้ซีโอไลท์เป็นตัวดูคซับ (Adsorptive Removal of Sulfur Compounds from Transportation Fuels by Using Zeolitic Adsorbents) อ. ที่ปรึกษา : ผศ. คร. ปมทอง มาลากุล ณ อยุธยา และคร. โซฟี จูเลียน 82 หน้า

งานวิจัยนี้จัดทำขึ้นเพื่อมุ่งเน้นในการศึกษาการปรับปรุงโซเคียมวายซีโอไลท์โดยใช้การ เช่น โลห**ะนิค**เกิล และโลหะคอปเปอร์ เพื่อเพิ่ม แลกเปลี่ยนไอออนกับโลหะทรานซิชัน ประสิทธิภาพของตัวดูคซับในการกำจัคสารประกอบกำมะถัน ที่กำจัดได้ยากโคยใช้กระบวนการที่ ใช้อยู่ในปัจจุบัน โคยประสิทธิภาพของคอปเปอร์วายซืโอไลท์ (CuY zeolite) และ นิคเกิลวายซื โอไลท์ (NiY zeolite) ในการกำจัดแบบจำลองสารประกอบกำมะถัน เช่น 3-เมทิลไทโอฟีน เบน โซไทโอฟีน และ ไคเบนโซไทโอฟีน ออกจากแบบจำลองน้ำมันเชื้อเพลิงแก๊ซโซลิน และคีเซล เช่น ใอโซออกเทน และเคคเคน ตามลำคับ จะทำการศึกษาจากผลของชนิดของโลหะทรานซิชัน และ ปริบาณของโลหะทรานซิชันที่แลกเปลี่ยนกับโซเดียมวา**ยซี**โอไลท์โดยใช้การทดลองแบบกะ (batch method) ที่สภาวะบรรยากาศ ผลของปริมาณสารละลายโลหะทรานซิชันต่อปริมาณตัวดูด ซับปริมาณที่ส่งผลต่อปริมาณของโลหะทรานซิชันที่ทำการแลกเปลี่ยนกับโซเดียมไอออนของ โซเดียมวายซีโอไลท์จะทำการศึกษา โคยกราฟแสดงผลของปริมาณกำมะถันที่ถูกดูคซับที่อุณหภูมิ คงที่สามารถทำนายได้โดยใช้สมการของแลงเมียร์ (Langmuir isotherm) โดยคอปเปอร์วายซี โอไลท์สามารถดูดซับ 3-เมทิลไทโอฟีน เบนโซไทโอฟีน และไดเบนโซไทโอฟีนได้สูงกว่านิกเกิล วายซีโอไลท์และโซเคียมวายซีโอไลท์ และความสามารถในการคูคซับของคอปเปอร์วายซีโอไลท์ เป็นสัคส่วนโดยตรงกับปริมาณคอปเปอร์บนตัวดูดซับ ซึ่งแตกต่างกับนิกเกิลวายซีโอไลท์ที่ไม่ได้ ขึ้นอยู่กับปริมาณนิกเกิลบนตัวคูคซับ ความสามารถในการคูคซับที่แตกต่างกันอาจจะมีผลมาจาก ขนาคของรูพรุนของซีโอไลท์หลังจากทำการแลกเปลี่ยน**ไอ**อน

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LIST OF SYMBOLS

SYMBOL

<i>a</i> , <i>b</i>	parameter in the equation of state
\boldsymbol{B}	Langmuir constant
C_e	equilibrium concentration (mol/l)
E_{A}	equivalent fraction of metal ion in zeolite
$E_{A(S)}$	equivalent fraction of metal ion in solution phase
f	fugacity
h_2^{IG}	molar enthalpy of ideal gas
\hbar_2^m	infinite-dilution partial molar enthalpy of solute in the mobile phase
\hbar_2^s	infinite-dilution partial molar enthalpy of solute in the stationary
phase	
K_2	adsorption equilibrium constant of solute (m³/mol)
k_{ij}	binary interaction parameter
l_{ij}	binary interaction parameters in the Peng-Robinson equation of state
N_0	avogadro's number
ND	number of data points
n	total number of moles
ni	number of moles of ith species
OBJ	objective function
p	pressure (bar)
p_c	critical pressure (bar)
q	equilibrium adsorption capacity (mol/l)
q_2^*	solid-phase concentration of species adsorbed in the stationary phase
	(mol/l)
q_{max}	saturation capacity (mol/l)
R	universal gas constant
	·

RMSD	root-mean-squared relative deviation
S_g	specific surface area (m ² /kg)
T	temperature (K)
T_c	critical temperature (K)
V	molar volume (m³/mol)
x_i, x_j	partial molar of component i and j

GREEK LETTERS

$ ho_{\scriptscriptstyle B}$	bulk density of the solid phase as packed (g/cm ³)
$ ho_{\scriptscriptstyle m}$	molar density of the mobile phase as packed (g/cm ³)
ε	bed porosity
α^m	volume expansivity
κ^m	isothermal compressibility
$\overline{\upsilon_2^m}$	infinite-dilution partial molar volume of solute in the mobile phase