

REFERENCES

- Gonzalez, D.L., Hirasaki, G.J., Creek, J. & Chapman, W.G. (2007). Modeling of Asphaltene Precipitation Due to Changes in Composition Using the Perturbed Chain Statistical Associating Fluid Theory Equation of State. Energy & Fuels 21, 1231-1242.
- Haskett, C.E., and Tartera, M. (1965). A practical solution to the problem of asphaltene deposits Hassi Messaoud field, Algeria. <u>Journ al of Petroleum Technology</u>, 17(4), 387-391.
- Hoepfner, M. (2009) Determination of asphaltene deposition mechanism by capillary flow experiments. <u>Preliminary Report</u>, Department of Chemical Engineering, University of Michigan.
- Hoepfner, M. (2010) Understanding Asphaltene Deposition at Low Degrees of Destabilization. presented at 11th Annual International Conference Petroleum Phase Behavior and Fouling, Jun 13-17, 2010
- Hoepfner, M. (2011) Asphaltene Deposition Occurs at Low Degrees of Destabilization. <u>Manuscript in Preparation</u>, Department of Chemical Engineering, University of Michigan.
- Jamialahmadi, M., Soltani, B., Muller-Steinhagen H., and Rashtchian, D. (2009). Measurement and prediction of the rate of deposition of flocculated asphaltene particles from oil. <u>International Journal of Heat and Mass</u> Transfer, 52(19-20), 4624-4634.
- Kaminski, T.J., Fogler, S.H., Wolf, N., Wattana, P., and Mairal, A. (2000).

 Classification of Asphaltenes via Fractionation and the Dffect of Heteroatom content on Dissolution Kinetics. Energy and Fuels, 14(1), 25-30.
- Leontaritis, K. J.; Amaefule, J. O.; Charles, R. E. SPE Prod. Facil. (1994), 157–164.
- Maqbool, T. (2006) Investigations into Asphaltene Deposition. Chulalongkorn University
- Maqbool, T., Balgoa, A.T. and Fogler, S. H. (2009) Revisiting Asphaltene Precipitation from Crude Oils: A Case of Neglected Kinetic Effects. Energy & Fuels, 23(7), 3681-3686.

- Maqbool, T., Raha, S., Hoepfner, P.M. And Fogler, S.H. (2011) Modelling the Aggregation of Asphaltene Nanoaggregates in Crude Oil-Precipitant Systems. Energy & Fuels, 25(4), 1585-1596.
- Mullins, O.C., Sheu, E.Y., Hammami, A. and Marshall, A.G. (2007).

 <u>Asphaltenes, Heavy Oils, and Petroleomics</u>. New York: Springer.
- Nabzar, L., and Aguilera, M.E. (2008). The colloidal approach. A promising route for asphaltene deposition modeling. Oil and Gas Science and Technology Revue De Linstitut Francias Du Petrole, 63(1), 21-35.
- Roux, J., Broseta, D. & Deme, B. (2001). SANS Study of Asphaltene Aggregation: Concentration and Solvent Quality Effects. <u>Langmuir</u> 17, 5085-5092.
- Vafaie-Sefti, M., and Mousavi-Dehghani, S. (2006). Application of association theory to the prediction of asphaltene deposition: Deposition due to natural depletion and miscible gas injection processes in petroleum reservoirs. Fluid Phase Equilibria, 247(1-2), 182-189.
- Vargas, F.M., Creek, J.L., and Chapman, W.G. (2010). On the development of an asphaltene deposition simulator. <u>Energy and Fuels</u>, 24(4), 2294-2299.
- Wang, J., Buckley, J.S., and Creek, J.L. (2004). Asphaltene deposition on metallic surfaces. Journal of Dispersion Science and Technology, 25(3), 287-297.
- Wattana, P. <u>Precipitation and Characterization of Petroleum Asphaltenes.</u>
 (2004) Ph.D. Dissertation. University of Michigan, Ann Arbor, MI.

APPENDICES

Appendix A Onset Point of Oil W

As mention in 4.4, the onset point of Oil W was around 25% heptanes at 25°C and 35 vol% heptanes at 60°C. Micrographs of WY can be seen is Figure A1.

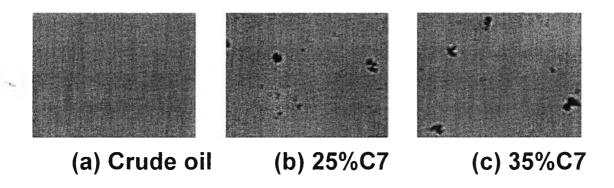


Figure A1 Micrographs showing the pictures of Oil W and precipitant's solution effluent of different concentrations.

Appendix B Shear Rate Calculation

In order to calculate shear rate, we need to know the flow rate and the radius of the capillary tube. The properties of our apparatus can be seen in Table B1.

Table B1 Capillary properties and experiment condition

Properties	Connecting line	Capillary	
Diameter (in)	0.03 0.02		
Radius (in)	0.015	0.01	
Flow rate (mL/hr)	5	5	

Example of shear rate calculation:

Shear rate =
$$4 * \frac{\text{Flow rate}}{\pi r^3}$$

Shear rate = $4 * \left(\frac{5}{\pi * 0.02^3}\right) \frac{mL}{in^3 \cdot hr} * \frac{1}{2.54^3} \frac{in^3}{cm^3} * \frac{1}{1} \frac{cm^3}{mL}$

Shear rate =
$$48561 \frac{1}{hr} * \frac{1}{3600} \frac{hr}{s} = 13.5 \frac{1}{\text{sec}}$$

Appendix C Residence Time Calculation

In order to calculate residence time, we need to know the details of every part in apparatus to calculate the residence time. The properties of our apparatus can be seen in Table C1.

Table C1 Properties of components in apparatus

Properties	Frit	Connecting line	Capillary
Shape	Cylinder	Cylinder	Cylinder
Radius (in)	0.031	0.015	0.005
Long (in)	0.062	2	12
Porosity	0.35	1	1

Example of frit's residence time calculation:

Residence time =
$$\frac{\text{Volume of mixing section}}{\text{Volumetric Flow Rate (Q)}}$$

Residence Time = Porosity * $\frac{(\pi r^2 L)}{\text{Flow Rate}}$
Residence Time = $0.35 * \frac{(\pi * 0.031^2 * 0.062)}{5} \frac{in^3 \cdot hr}{mL} * \frac{2.54^3}{1} \frac{cm^3}{in^3} * \frac{1}{1} \frac{mL}{cm^3}$
Residence Time = $0.000215 hr * \frac{3600}{1} \frac{s}{hr} = 0.773 \text{sec}$

CURRICULUM VITAE

Name: Ms. Vipawee Limsakoune

Date of Birth: April 27, 1988

Nationality: Thai

University Education:

2006-2010 Bachelor Degree of Chemical Engineering, King Mongkut's

Institute of Technology Ladkrabang, Bangkok, Thailand

Work Experience:

2009 Position: Student Internship

Company name: Thailand Institute of Scientific and

Technological Research, Thailand

Proceedings:

Limsakoune, V.; Malakul, P.; Hoepfner, M. and Fogler, H.S. (2012, April 24)
 Studying Asphaltene Instability by Capillary Deposition. <u>Proceedings of The 3rd Research Symposium on Petroleum, Petrochemicals, and Advanced Materials and The 18th PPC Symposium on Petroleum, Petrochemicals, and Polymers. Queen Sirikit National Convention Center, Bangkok, Thailand

</u>

