

REFERENCES

1. Weber , W.F., and Bowman , W. 1986. Membranes Replacing Other Separation Technologies. *Chemical Engineering Progress* 34: 23-28.
2. สิทธินันท์ ท่อแก้ว. 2539. ตัวกรองเซรามิกชนิดไฮอะลูมีนาสำหรับการแยกทางชีวภาพ. วิทยานิพนธ์ปริญญามหาบัณฑิต. จุฬาลงกรณ์มหาวิทยาลัย.
3. Yoldas, B.E. 1975. Alumina Sol Preparation from Alkoxides. *Journal of the American Ceramic Society Bulletin* 54(3): 289-290.
4. Yoldas, B.E. 1982. Effect of Variations in Polymerized Oxides on Sintering and Crystalline Transformations. *Journal of the American Ceramic Society* 65(8): 387-393.
5. Leenaars, A.F.M., Keizer, K., and Burggraaf, A.J. 1986. Porous Alumina Membranes. *Chemtech* (9): 560-564.
6. Terpstra, R.A., Bonekamp, B.C., and Veringa, H.J. 1988. Preparation, Characterization and Some Properties of Tubular Alpha Alumina Ceramic Membranes for Micro-filtration and as a Support for Ultrafiltration and Gas Separation Membranes. *Desalination* 70: 395-404.
7. Anderson, M.A., Gieslmann, M.J., and Xu, Q. 1988. Titania and Alumina Ceramic Membranes. *Journal of Membrane Science* 39: 243-258.

8. Yu, C., and Klein, L.C. 1992. Supported Alumina Membranes by an in-Situ Sol-Gel Method. *Journal of the American Ceramic Society* 75(9): 2613-2614.
9. Anderson, M.A., and Sheng, G. 1993. Microporous alumina ceramic membranes. US patent 5,208,190.
10. พิเชฐ อิสุกอ. 2527. การผลิตและฟื้นฟูอะไมเลสจาก *Bacillus amyloliquefaciens* KA 63 วิทยานิพนธ์ปริญญามหาบัณฑิต. จุฬาลงกรณมหาวิทยาลัย.
11. Tsvetkov, V.T., and Emanuilova, E.I. 1989. Purification and Properties of heat stable α -amylase from *Bacillus brevis*. *Applied Microbiology and Biotechnology* 31(3): 246-248.
12. Bealin-Kelly, F.J., Kelly, C.T., and Fogarty, W.M. 1990. The α -amylase of the caldoactive bacterium *Bacillus caldovelox*. *Biochemical Society Transactions* 66(2): 310-311.
13. Shah, N.K., Upadhyay, C.M., Nehete, P.N., Kothari, R.M., and Hegde, M.V. 1990. An economical, upgraded, stabilized and efficient preparation of α -amylase. *Journal of Biotechnology* 16(1-2): 97-108.
14. Draijer , W. 1984. Preparation, structure and separation characteristics of Ceramic Alumina Membranes.
15. Peterson , R.A., Webster , E.T., Niezyniecki , G.M., Anderson , M.A. and Hill Jr. , C.G. 1995. Ceramic membranes for novel separations. *Separation science and technology* 30(7-9): 1689-1709.

16. Brinker , C.J., and Scherer , G.W. 1990. *Sol-Gel Science, The Physics and Chemistry of Sol-Gel Processing*. San Diego:Academic Press,Inc.
17. Gitzen , W.H. 1970. *Alumina as a Ceramic Material*. Ohio: The American Ceramic Society.
18. Poisson, R., Brunelle, J.P., and Nortier, P. Alumina. In Stiles, A.B. (ad.). *Catalyst Supports and Supported Catalysts*. Boston:Butterworth Publishers.
19. Larbot, A., Fabre, J.P., Guizard, C., and Cot, L. 1988. Inorganic membranes obtained by sol-gel techniques. *Journal of Membrane Science* 39: 203-212.
20. Lee, J.M. 1992. Enzyme Kinetics. *Biochemical Engineering*. New Jersey: Prentice-Hall, Inc.
21. ดวงพร คันธ์โชคิ. 2530. ผลิตภัณฑ์เอนไซม์จากจุลินทรีย์. จุลชีววิทยาอุดสาหกรรม: สำหรับผลิตภัณฑ์จากจุลินทรีย์. กรุงเทพมหานคร: สำนักพิมพ์โอดี้ยนส์เตอร์.
22. Windish, W.W., and Mhatre, N.S. Microbial Amylase. in Umbreit, W.W. (ed.). 1960. *Advance in Applied Microbiology vol. 7*. New York and London: Academic Press, Inc.
23. อนุรักษ์ ปิติรักษ์สกุล. 2532. จนศาสตร์ของการไฮโดรไลซ์แบ่งด้วยเอนไซม์แอลfa อะไมแลตในกระบวนการการลอกแบ่งจากผ้า. วิทยานิพนธ์ปริญามหาบัณฑิต. สถาบันเทคโนโลยีพระจอมเกล้าธนบุรี.

24. Tutunjian, R.S. Ultrafiltration Processes in Biotechnology. In Moo-Young,M.(ed.). 1985. *Comprehensive Biotechnology Vol 2: The Principle of Biotechnology: Engineering Considerations*. Exeter, England: A.Wheaton & Co. Ltd.
25. Kulkarni, S.S., Funk, E.W., and Li, N.N. Ultrafiltration. In Winston Ho, W.S. and Sirkar, K.K. (eds.). *Membrane Handbook*. New York: Van Nostrand Reinhold.
26. Heck, R.M., and Farrauto, R.J. 1995. The Preparation of Catalytic Materials. *Catalytic Air Pollution Control*. New York: Van Nostrand Reinhold.
27. Finch, C.A. 1992. Analytical Methods for Polyvinyl Alcohol. *Polyvinyl Alcohol-Developments*. England: John Wiley & Sons. Ltd.
28. Colowick, S.P., and Kaplan, N.O. 1955. Amylases, α and β . *Methods in Enzymology VI*. New York: Academic Press, Inc.

APPENDIX

APPENDIX A

SUPPORT PROPERTIES DETERMINATION

Apparent Porosity

$$p, \% = [(W-D)/V]*100$$

Water Absorption

$$A, \% = [(W-D)/D]*100$$

Bulk Density

$$B, g/cm^3 = D/V$$

where D is dry weight, g

W is saturated weight, g

S is suspended weight, g

V is exterior volume, cm³ = W - S

Shrinkage

$$\text{shrinkage , \%} = [(L_B - L_A)/L_B] * 100$$

where L_B is the length of specimen before sintering, cm.

L_A is the length of specimen after sintering, cm.

Modulus of Rupture

$$M, \text{ MPa} = 8PLD/\pi (D^4 - d^4)$$

where P is load at rupture, N

L is distance between supports, mm.

D is outside diameter of specimen, mm.

d is inside diameter of specimen, mm.

APPENDIX B

POLYVINYL ALCOHOL DETERMINATION [27]

Procedure

20 ml of sample is diluted to 25 ml and then treated with 15 ml of 4 % boric acid solution and 3 ml of iodine solution (prepared from 1.27 g of iodine and 25 g of KI/I). The resulting solution is diluted to 50 ml and kept at 25 °C and its absorbance measured at 690 nm.

Note

Beer's law applies in the concentration range of 0-20 mg of polyvinyl alcohol/l of solution.

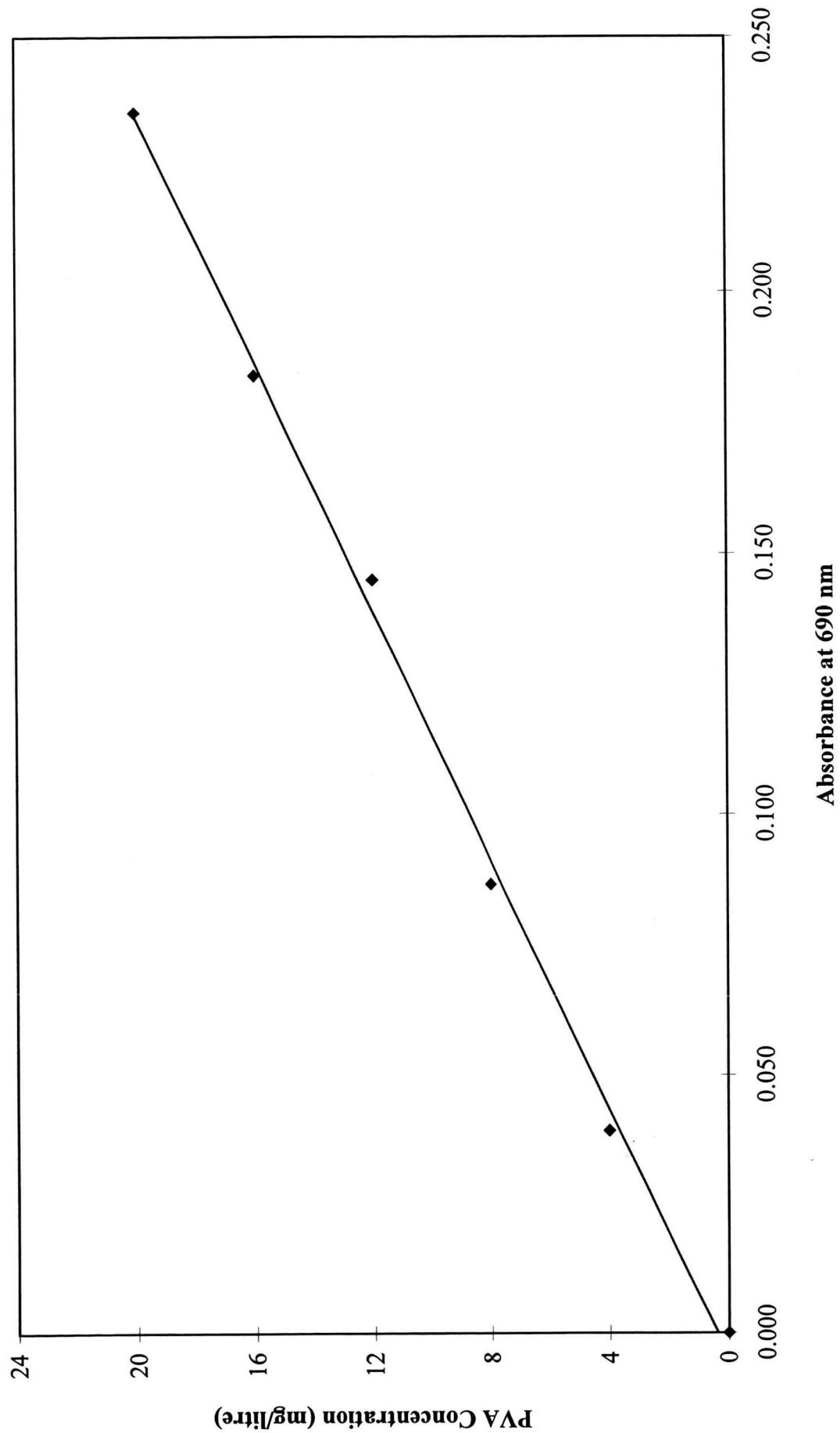


Figure B1 Polyvinyl Alcohol (MW 70,000-100,000) Standardization Curve

APPENDIX C

SACCHARIFYING AMYLASE DETERMINATION [28]

Reagents

0.02 M Phosphate buffer, pH 6.9

45.0 ml of 0.02 M sodium dihydrogen phosphate is mixed with 55.0 ml of 0.02 M disodium hydrogen phosphate. Store in the refrigerator.

Substrate solution

2 g of soluble starch is dissolved in 100 ml of 0.02 M phosphate buffer, pH 6.9

Dinitrosalicylic acid reagent

1 g of 3,5-dinitrosalicylic acid is dissolved in 20 ml of 2 M sodium hydroxide and 50 ml of distilled water, then 30 g sodium potassium tartrate is added, and diluted to 100 ml with distilled water. Keep this solution in the brown bottle.

Procedure

0.5 ml of properly diluted enzyme is incubated for 3 minutes at 50 °C with 0.5 ml of substrate solution. The enzyme reaction is interrupted by the addition of 1 ml of DNSA reagent. The tube containing this mixture is heated for 5 minutes in boiling water and then cooled in running tap water. After addition of 10 ml of H₂O, the absorbance of the solution is measured at 540 nm.

Note

The unit of enzyme is amount of enzyme saccharify 1 mg of glucose within 1 minute at 50 °C, pH 6.9.

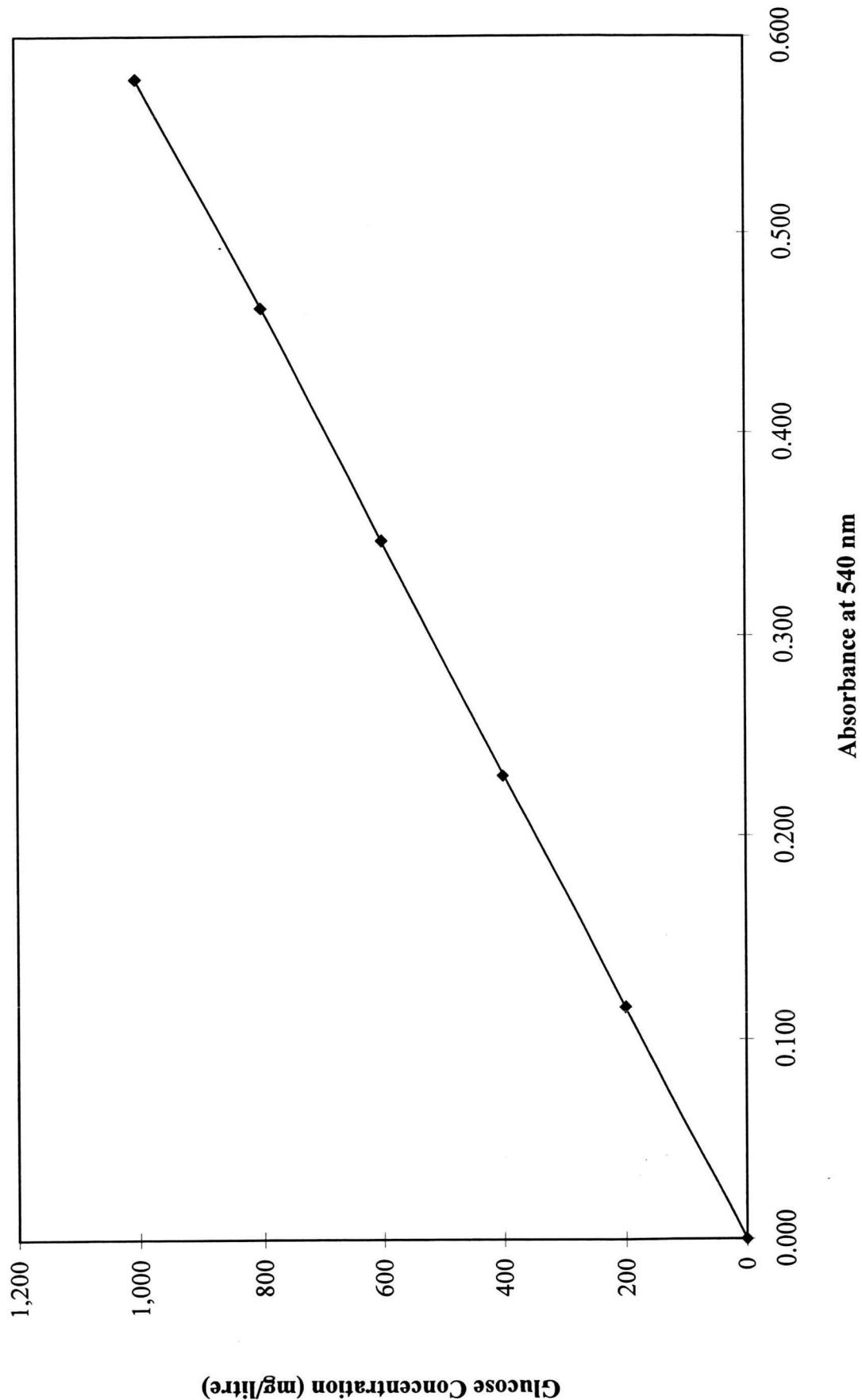


Figure C1 Glucose Standardization Curve

APPENDIX D

EXPERIMENTAL DATA

Table D1 Pore Size Distribution of Support Layers

Average Pore Diameter (A)	Pore Volume (cc/g)
839,279	0.0000
337,729	0.0000
187,484	0.0000
136,743	0.0019
92,287	0.0000
67,819	0.0000
53,134	0.0000
43,143	0.0000
35,240	0.0000
24,858	0.0000
16,946	0.0000
15,105	0.0013
13,047	0.0562
10,929	0.0264
9,494	0.0042
8,524	0.0065
7,508	0.0000
6,537	0.0035
5,269	0.0000
4,176	0.0004
3,242	0.0000
2,241	0.0054
1,748	0.0023
1,250	0.0078
902	0.0091
754	0.0002
652	0.0374
552	0.0000
452	0.0130
352	0.0107
251	0.0000
160	0.0000

Table D2 Membrane Thickness VS. Coating Time

Dipping Time (sec)	Membrane Thickness (micron)
10	4.50
20	8.10
30	12.14

Table D3 Properties of Membranes in Various Calcination Temperature

Calcination Temperature (C)	Avg. Pore Diameter (A)	Porosity (%)	Pore Volume (cc/g)
300	37.0989	41.94	0.066379
400	48.8029	45.96	0.092650
500	57.3716	47.20	0.112047
600	69.4301	48.21	0.132123
700	78.5873	46.74	0.118447
800	95.4350	46.65	0.113336

Table D4 Properties of Membranes in Various Calcination Time

Calcination Time (minute)	Avg. Pore Diameter (A)	Porosity (%)	Pore Volume (cc/g)
5	72.5049	48.02	0.132381
30	74.4301	48.21	0.132423
120	75.5479	46.70	0.125879
240	76.0133	45.61	0.123125

Table D5 Permeation Flux of Support and Intermediate at Recirculation Velocity 1.66 m/sec in Various Transmembrane Pressure

Transmembrane Pressure (bars)	Permeation Flux (cc/min-sq.cm)	
	Support	Intermediate
0.3	1.56	0.13
0.4	2.03	0.18
0.5	2.53	0.22

Table D6 Permeation Flux of Bi-Layer Membrane in Various Transmembrane Pressure

Transmembrane Pressure (bars)	Permeation Flux (cc/min-sq.cm)		
	v = 1.66 m/sec	v = 1.43 m/sec	v = 1.04 m/sec
0.3	0.016	0.014	0.010
0.4	0.022	0.018	0.013
0.5	0.028	0.023	0.016

Table D7 Pore Size Distribution of One and Bi-Layer Membrane

Pore Diameter Range (Å)	One Layer Membrane		Bi-Layer Membrane	
	Pore Diameter Range (Å)	Pore Volume (cc/g)	Pore Diameter Range (Å)	Pore Volume (cc/g)
10517.9-1650.1	0.008131	1.92	35117.7-1438.1	0.005126
1650.1-653.5	0.001211	0.29	1438.1-624.1	0.000794
653.5-348.4	0.001412	0.33	624.1-340.6	0.001010
348.4-256.3	0.001251	0.30	340.6-253.3	0.000916
256.3-184.3	0.002124	0.50	253.3-179.1	0.001558
184.3-134.8	0.003642	0.86	179.1-125.3	0.004732
134.8-100	0.003511	0.83	125.3-103	0.019137
100-79.4	0.105864	25.02	103-77.1	0.118647
79.4-58.2	0.132123	31.22	77.1-57.3	0.132215
58.2-43.9	0.066654	15.75	57.3-43.8	0.066517
43.9-33.7	0.033678	7.96	43.8-34.9	0.032091
33.7-27.3	0.015952	3.77	34.9-27.1	0.021374
27.3-22.4	0.009559	2.26	27.1-22.2	0.009644
22.4-17.4	0.006443	1.52	22.2-17.2	0.006499

Table D8 Experimental Data of Filtration at Enzyme Concentration and Recirculation Velocity of 2.4 g/litre and 1.66 m/sec

Time (min)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Pressure = 0.3 bar			Pressure = 0.4 bar			Pressure = 0.5 bar		
			Glucose Conc. (mg/litre)	Rejection (%)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)	Rejection (%)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)
0	0.0	0.0000	3,634.22	0.00	0.0	0.0000	3,634.22	0.00	0.0	0.0000	4283.16
4	19.3	0.0144	54.76	54.76	25.7	0.0192	49.3	0.0176	1,341.31	63.09	31.6
8	37.5	0.0136	1,644.14	54.76	95.4	0.0166	73.2	0.0178	1,696.06	53.33	61.4
12	55.9	0.0137	1,678.75	53.81	118.6	0.0173	141.6	0.0172	1,730.67	52.38	88.9
16	73.6	0.0132	1,747.97	51.90	163.3	0.0162	185.5	0.0166	1,678.75	53.81	116.4
20	91.5	0.0134	1,782.58	50.95	207.5	0.0164	230.6	0.0172	1,782.58	50.95	144.1
24	109.4	0.0134	1,817.19	50.00	250.7	0.0150	270.3	0.0146	1,730.67	52.38	172.1
28	125.7	0.0122	1,851.80	49.05	321.0	0.0154	311.6	0.0154	1,652.80	54.52	200.8
32	141.2	0.0116	1,879.89	50.47	395.7	0.0163	415.2	0.0166	1,696.06	53.33	226.6
36	158.1	0.0126	1,904.00	49.52	468.9	0.0138	490.3	0.0145	1,765.28	51.43	253.4
40	173.5	0.0115	1,934.50	50.00	575.5	0.0159	596.8	0.0159	1,644.14	54.76	280.2
44	187.3	0.0103	1,964.14	50.00	639.4	0.0159	618.1	0.0159	1,644.14	54.76	305.3
48	201.7	0.0107	1,994.00	49.52	709.4	0.0172	735.7	0.0159	1,687.41	53.57	331.4
52	218.5	0.0125	2,023.50	50.00	762.0	0.0160	794.0	0.0160	1,644.14	54.76	359.0
56	236.9	0.0137	2,053.00	49.52	825.2	0.0175	856.0	0.0175	1,687.41	53.57	384.7
60	252.2	0.0114	2,082.50	50.00	889.0	0.0166	921.0	0.0166	1,644.14	54.76	410.2
64	269.0	0.0125	2,112.00	49.52	953.8	0.0150	984.0	0.0150	1,687.41	53.57	435.4
68	285.8	0.0125	2,141.50	50.00	1,017.0	0.0148	1,048.0	0.0148	1,687.41	53.57	460.4
72	300.7	0.0111	2,171.00	50.00	1,081.0	0.0163	1,113.0	0.0163	1,670.10	54.05	485.0
76	317.4	0.0125	2,200.50	49.52	1,145.0	0.0145	1,176.0	0.0145	1,670.10	54.05	509.4
80	331.9	0.0108	2,230.00	48.57	1,209.0	0.0123	1,241.0	0.0123	1,696.06	53.33	533.6
84	346.3	0.0107	2,259.50	49.52	1,273.0	0.0139	1,304.0	0.0139	1,687.41	53.57	557.4
88	362.8	0.0123	2,289.00	49.52	1,337.0	0.0138	1,369.0	0.0138	1,765.28	51.43	584.0
92	376.2	0.0100	2,318.50	49.52	1,401.0	0.0160	1,443.0	0.0160	1,644.14	54.76	607.4
96	392.5	0.0122	2,348.00	50.95	1,465.0	0.0159	1,507.0	0.0159	1,730.67	52.38	633.8
100	408.9	0.0122	2,377.50	50.95	1,529.0	0.0159	1,571.0	0.0159	1,687.41	53.57	656.9
104	425.2	0.0122	2,407.00	53.81	1,593.0	0.0159	1,644.14	0.0159	1,687.41	53.57	683.2
108	441.6	0.0122	2,436.50	53.81	1,657.0	0.0159	1,716.0	0.0159	1,644.14	54.76	709.4
112	457.9	0.0122	2,466.00	53.81	1,721.0	0.0159	1,784.0	0.0159	1,644.14	54.76	735.7
116	474.3	0.0122	2,495.50	54.76	1,785.0	0.0159	1,851.0	0.0159	1,644.14	54.76	762.0
120	490.7	0.0122	2,525.00	54.76	1,849.0	0.0159	1,918.0	0.0159	1,644.14	54.76	788.3

Table D9 Experimental Data of Filtration at Enzyme Concentration and Recirculation Velocity of 2.4 g/litre and 1.43 m/sec

Time (min)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Pressure = 0.3 bar			Pressure = 0.4 bar			Pressure = 0.5 bar		
			Glucose Conc. (mg/litre)	Rejection (%)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)	Rejection (%)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)
0	0.0	0.0000	4079.72	0.00	0.0	0.0000	4105.83	0.00	0.0	0.0000	3986.45
4	17.5	0.0131	1835.06	55.02	23.5	0.0175	1887.86	54.02	29.9	0.0223	0.00
8	34.6	0.0128	1827.31	53.21	46.1	0.0169	1812.31	55.86	57.9	0.0209	52.83
12	49.9	0.0114	1908.90	89.2	68.4	0.0166	1861.58	54.66	86.5	0.0213	
16	65.4	0.0116	1910.53	53.17	111.3	0.0155	191.8	0.0151	113.1	0.0198	1848.92
20	80.4	0.0112	2039.86	50.00	131.9	0.0165	210.5	0.0154	140.8	0.0207	53.62
24	94.9	0.0108	2182.24	46.51	151.1	0.0143	230.0	0.0145	167.3	0.0198	1800.68
28	108.9	0.0104	2249.15	44.87	249.3	0.0144	1690.37	53.96	193.3	0.0194	54.83
32	123.3	0.0107	2261.80	44.56	270.1	0.0155	1809.44	55.93	219.9	0.0198	1848.12
36	136.3	0.0097	2249.15	44.87	289.0	0.0141	1560.22	62.00	246.1	0.0195	53.64
40	150.1	0.0103	2249.15	44.87	307.7	0.0139	1762.22	57.08	272.1	0.0194	1882.80
44	163.7	0.0101	2249.15	44.87	328.2	0.0153	1690.37	58.83	297.9	0.0192	52.77
48	177.0	0.0099	2048.84	49.78	346.4	0.0136	1560.22	62.00	321.7	0.0178	2018.34
52	191.7	0.0110	2249.15	44.87	364.4	0.0134	1985.17	51.65	346.8	0.0187	49.37
56	204.6	0.0096	2039.86	50.00	384.6	0.0151	1949.04	52.53	373.5	0.0199	1975.29
60	217.2	0.0094	2249.15	44.87	404.9	0.0151	2092.74	49.03	473.0	0.0179	1884.79
64	231.7	0.0108	2249.15	44.87	422.3	0.0130	2113.68	48.52	499.2	0.0195	50.45
68	243.9	0.0091	2249.15	44.87	442.4	0.0150	2092.74	49.03	522.8	0.0182	1884.79
72	255.8	0.0089	2216.92	45.66	459.4	0.0127	2092.74	49.03	549.0	0.0197	52.72
76	270.0	0.0106	2182.24	46.51	479.4	0.0149	2113.68	48.52	572.2	0.0173	2031.10
80	284.2	0.0106	2249.15	44.87	499.4	0.0149	2092.74	49.03	598.2	0.0194	49.05
84	295.6	0.0085	2249.15	44.87	519.3	0.0148	2092.74	49.03	621.0	0.0170	1926.65
88	309.7	0.0105	2249.15	44.87	539.3	0.0149	2092.74	49.03	646.8	0.0192	48.32
92	320.7	0.0082	2182.24	46.51	559.3	0.0149	2092.74	49.03	672.7	0.0193	1926.65
96	334.6	0.0104	2182.24	46.51	579.3	0.0149	2092.74	49.03	698.6	0.0193	51.67
100	348.6	0.0104	2249.15	44.87	599.3	0.0149	2092.74	49.03	724.4	0.0192	1926.65
104	362.5	0.0104	2249.15	44.87	579.3	0.0148	2092.74	49.03	750.3	0.0193	51.67
108	376.4	0.0104	2182.24	46.51	599.3	0.0149	2092.74	49.03	776.2	0.0193	1926.65
112	390.4	0.0104	2182.24	46.51	599.3	0.0149	2092.74	49.03	796.5	0.0193	51.67
116	404.3	0.0104	2182.24	46.51	599.3	0.0149	2092.74	49.03	816.5	0.0193	
120	418.3	0.0104	2182.24	46.51	599.3	0.0149	2092.74	49.03	836.5	0.0193	

Table D10 Experimental Data of Filtration at Enzyme Concentration and Recirculation Velocity of 2.4 g/litre and 1.04 m/sec

Time (min)	Pressure = 0.3 bar			Pressure = 0.4 bar			Pressure = 0.5 bar					
	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)	Rejection (%)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)	Rejection (%)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)	Rejection (%)
0	0.0	0.0000	3634.22	0.00	0.0	0.0000	4085.67	0.00	0.0	0.0000	4389.63	0.00
4	12.9	0.0096			16.2	0.0121			20.5	0.0153		
8	24.7	0.0088	372.14	89.76	31.1	0.0111	1488.00	63.58	39.7	0.0143	1628.11	62.91
12	37.0	0.0092			45.4	0.0107			57.1	0.0130		
16	47.9	0.0081	1445.33	60.23	58.9	0.0101	1603.63	60.75	75.0	0.0134	1718.10	62.91
20	59.3	0.0085			73.1	0.0106			92.6	0.0131		
24	70.8	0.0086	1471.13	59.52	88.4	0.0114	1556.64	61.9	109.4	0.0125	2560.91	60.86
28	82.6	0.0088			102.3	0.0104			127.2	0.0133		
32	93.1	0.0078	1502.02	58.67	116.9	0.0109	1680.84	58.86	145.3	0.0135	2175.06	41.66
36	105.0	0.0089			128.5	0.0087			161.4	< 0.0120		
40	115.3	0.0077	1471.13	59.52	142.8	0.0107	1551.74	62.02	177.1	0.0117	2560.91	50.45
44	126.8	0.0086			155.7	0.0096			196.1	0.0142		
48	138.3	0.0086	1502.02	58.67	169.9	0.0106	1682.07	58.83	211.1	0.0112	2202.72	41.66
52	149.9	0.0087			184.0	0.0105			227.3	0.0121		
56	161.4	0.0086	1471.13	59.52	196.7	0.0095	1887.99	53.79	242.1	0.0110	2103.51	49.82
60	172.9	0.0086			207.1	0.0078			257.4	0.0114		
64	184.5	0.0087	1471.13	59.52	220.9	0.0103	1847.95	54.77	274.6	0.0128	2103.51	52.08
68	196.0	0.0086			234.7	0.0103			291.7	0.0128		
72	207.5	0.0086	1644.12	54.76	248.5	0.0103	1847.95	54.77	306.5	0.0110	2194.82	52.08
76	216.5	0.0067			259.8	0.0084			323.5	0.0127		
80	227.9	0.0085	1676.83	53.86	273.5	0.0102	1887.99	53.79	340.5	0.0127	2113.17	50.00
84	239.3	0.0085			287.2	0.0102			357.5	0.0127		
88	250.7	0.0085	1773.86	51.19	300.8	0.0101	1810.36	55.69	374.6	0.0128	2542.47	51.86
92	262.1	0.0085			314.5	0.0102			391.6	0.0127		
96	273.5	0.0085	1618.32	55.47	328.2	0.0102	1861.84	54.43	405.4	0.0103	1810.72	42.08
100	284.9	0.0085			341.8	0.0101			422.3	0.0126		
104	296.3	0.0085	1618.32	55.47	355.5	0.0102	1810.36	55.69	439.2	0.0126	1810.72	58.75
108	307.7	0.0085			369.2	0.0102			456.1	0.0126		
112	319.1	0.0085	1618.32	55.47	382.9	0.0102	1810.36	55.69	473.0	0.0126	1810.72	58.75
116	330.5	0.0085			396.5	0.0101			489.8	0.0125		
120	341.9	0.0085	1618.32	55.47	410.2	0.0102	1810.36	55.69	506.7	0.0126	1810.72	58.75

Table D11 Experimental Data of Filtration at Transmembrane Pressure and Recirculation Velocity of 0.5 bar and 1.66 m/sec

Time (min)	Enzyme Concentration = 1.2 g/litre			Enzyme Concentration = 1.8 g/litre			Enzyme Concentration = 2.4 g/litre						
	ACC. Volume (cc)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)	Rejection (%)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)	Rejection (%)	ACC. Volume (cc)	Flux (cc/min-sq.cm)	Glucose Conc. (mg/litre)	Rejection (%)
0	0.0	0.0000	1176.91	0.00	0.0	0.0000	2215.21	0.00	0.0	0.0000	4283.16	0.00	
4	42.1	0.0314	1055	99.10	0.00	35.7	0.0266	69.39	96.87	31.6	0.0236	1488.40	65.25
8	82.0	0.0298	1055	99.10	0.00	68.1	0.0242	100.5	0.0242	61.4	0.0222	1644.14	61.61
12	120.3	0.0286	1055	99.10	0.00	129.2	0.0214	173.22	92.18	116.4	0.0205	0.0205	0.0207
16	156.6	0.0271	1055	99.10	0.00	158.2	0.0216	189.0	0.0230	144.1	0.0207	1834.50	57.17
20	193.0	0.0272	1055	99.10	0.00	189.0	0.0230	294.35	86.71	172.1	0.0209	1903.72	55.55
24	230.8	0.0282	1055	99.10	0.00	219.6	0.0228	346.27	84.37	226.6	0.0192	1869.11	56.36
28	268.4	0.0280	1055	99.10	0.00	248.8	0.0218	307.0	0.0220	253.4	0.0200	1946.98	54.54
32	305.7	0.0278	1055	99.10	0.00	277.5	0.0214	581.62	73.74	280.2	0.0200	1955.63	54.34
36	343.9	0.0285	1055	99.10	0.00	337.7	0.0229	605.84	72.65	331.4	0.0195	1817.19	57.57
40	380.7	0.0275	1055	99.10	0.00	366.8	0.0217	640.45	71.09	359.0	0.0206	1860.46	56.56
44	415.8	0.0262	1055	99.10	0.00	399.1	0.0241	458.5	0.0214	384.7	0.0192	1946.98	54.54
48	453.7	0.0283	1055	99.10	0.00	429.8	0.0229	489.0	0.0228	410.2	0.0190	1955.63	54.34
52	491.5	0.0282	1055	99.10	0.00	447.2	0.0228	519.6	0.0228	460.4	0.0186	1903.72	55.55
56	527.4	0.0268	1055	99.10	0.00	473.2	0.0228	550.2	0.0228	485.0	0.0184	1946.98	54.54
60	565.1	0.0281	1055	99.10	0.00	500.0	0.0229	578.2	0.0209	509.4	0.0182	1955.63	54.34
64	600.6	0.0265	1055	99.10	0.00	527.0	0.0227	597.89	64.84	533.6	0.0181	1817.19	57.57
68	638.1	0.0280	1055	99.10	0.00	554.8	0.0228	608.6	0.0227	557.4	0.0178	1860.46	56.56
72	675.7	0.0280	1055	99.10	0.00	582.0	0.0228	639.1	0.0228	584.0	0.0198	1946.98	54.54
76	713.2	0.0280	1055	99.10	0.00	608.6	0.0227	669.5	0.0227	607.4	0.0175	1955.63	54.34
80	748.0	0.0260	1055	99.10	0.00	635.0	0.0227	727.1	0.0203	633.8	0.0197	1817.19	57.57
84	785.4	0.0279	1055	99.10	0.00	662.2	0.0226	757.4	0.0226	656.9	0.0172	1860.46	56.56
88	822.8	0.0279	1055	99.10	0.00	689.5	0.0226	787.7	0.0226	683.2	0.0196	1946.98	54.54
92	857.2	0.0257	1055	99.10	0.00	716.8	0.0227	818.0	0.0226	709.4	0.0195	1955.63	54.34
96	894.4	0.0277	1055	99.10	0.00	744.0	0.0227	848.3	0.0226	735.7	0.0196	1817.19	57.57
100	931.7	0.0278	1055	99.10	0.00	771.2	0.0226	878.6	0.0226	762.0	0.0196	1860.46	56.56
104	969.0	0.0278	1055	99.10	0.00	808.4	0.0226	908.9	0.0226	800.0	0.0196	1946.98	54.54
108	1006.2	0.0277	1055	99.10	0.00	845.6	0.0227	939.1	0.0227	831.2	0.0195	1955.63	54.34
112	1043.5	0.0278	1055	99.10	0.00	882.8	0.0226	970.0	0.0226	864.0	0.0196	1817.19	57.57
116	1080.8	0.0278	1055	99.10	0.00	919.0	0.0226	1000.2	0.0226	895.2	0.0196	1860.46	56.56
120	1118.1	0.0278	1055	99.10	0.00	956.2	0.0226	1027.4	0.0226	941.4	0.0196	1946.98	54.54

BIOGRAPHY

Miss Veerawan Vajanapornsan was born on August 26, 1971 in Bangkok, Thailand. In 1990, she graduated high school level from St. Joseph Convent. She received her Bachelor Degree in Chemical Engineering, Khon Kaen University in May 1994. She continued her Master's Study at Chulalongkorn University in June 1994.