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APPENDICES

Appendix A Calibration Curves

Table A1 Gas chromatograph's calibration curve for hydrogen (H₂)

Volume of hydrogen (ml)	Peak area
0.02	1,101,005
0.04	2,016,179
0.08	3,680,042
0.1	5,675,328
0.2	11,471,761
0.4	22,832,569

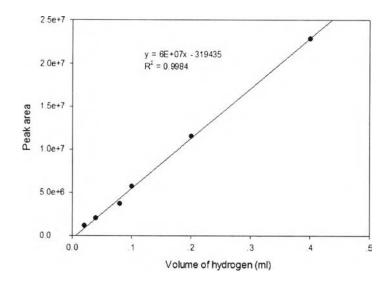


Figure A1 The relationship between amount of hydrogen (H₂) and peak area.

Amount of hydrogen =
$$\frac{\text{Peak area} + 319,435}{6 \times 10^7}$$

Table A2 Gas chromatograph's calibration curve for nitrogen (N2)

Volume of nitrogen (ml)	Peak area
0.02	69,431
0.04	188,161
0.08	426,068
0.1	478,146
0.2	1,008,515
0.4	2,155,800
0.6	3,309,337

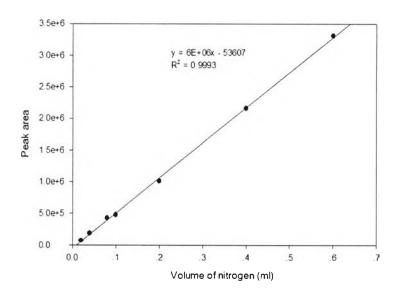


Figure A2 The relationship between amount of nitrogen (N₂) and peak area.

Amount of nitrogen =
$$\frac{\text{Peak area} + 53,607}{6 \times 10^6}$$

Table A3 Gas chromatograph's calibration curve for oxygen (O2)

Volume of oxygen (ml)	Peak area
0.02	81,122
0.04	233,918
0.08	514,527
0.1	662,766
0.2	1,366,208
0.4	2,738,126

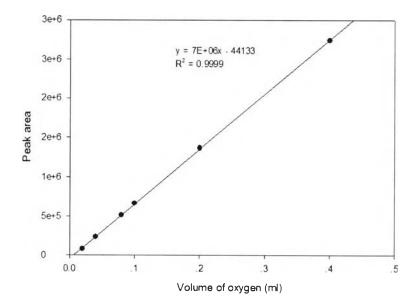


Figure A3 The relationship between amount of oxygen (O_2) and peak area.

Amount of oxygen =
$$\frac{\text{Peak area} + 44,133}{7 \times 10^6}$$

Table A4 Gas chromatograph's calibration curve for methane (CH₄)

Volume of methane (ml)	Peak area
0.02	151,094
0.04	523,919
0.08	998,851
0.1	1,366,651
0.2	2,898,103
0.4	5,880,444

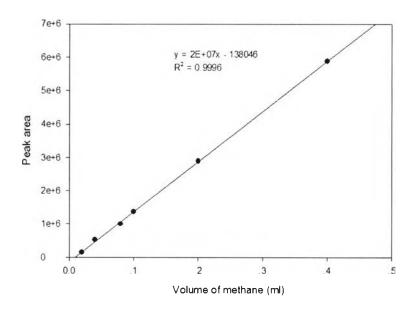


Figure A4 The relationship between amount of methane (CH_4) and peak area.

Amount of methane =
$$\frac{\text{Peak area} + 138,046}{2 \times 10^7}$$

Table A5 Gas chromatograph's calibration curve for carbon dioxide (CO₂)

Volume of carbon dioxide (ml)	Peak area
0.02	4,238
0.04	188,166
0.08	293,029
0.1	354,304
0.2	747,872
0.4	1,515,064

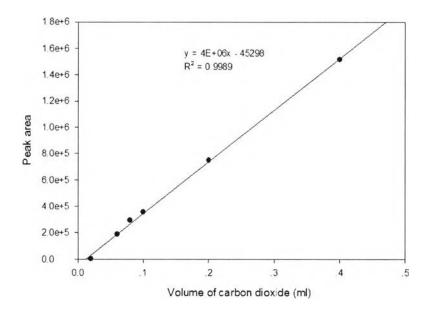


Figure A5 The relationship between amount of carbon dioxide (CO₂) and peak area.

Amount of carbon dioxide =
$$\frac{\text{Peak area} + 45,298}{4 \times 10^6}$$

Table A6 Liquid chromatograph's calibration curve for acetic acid

Concentration of acetic acid (mg/l)	Peak area
1,000	0.04
2,000	0.15
3,000	0.29
4,000	0.37
5,000	0.48

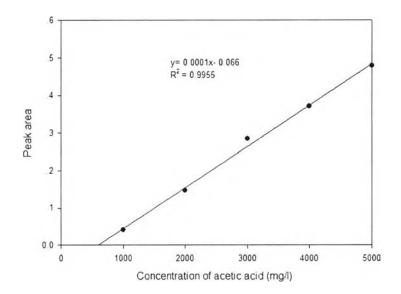


Figure A6 The relationship between concentration of acetic acid and peak area.

Amount of acetic acid =
$$\frac{Peak\ area + 0.066}{0.0001}$$

Table A7 Liquid chromatograph's calibration curve for propionic acid

Concentration of propionic acid (mg/l)	Peak area
1,000	0.14
2,000	0.36
3,000	0.59
4,000	0.77
5,000	0.95

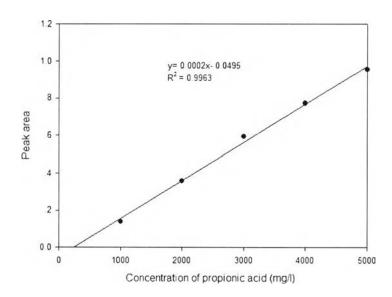


Figure A7 The relationship between concentration of propionic acid and peak area.

Amount of propionic acid =
$$\frac{Peak \ area + 0.0495}{0.0002}$$

Table A8 Liquid chromatograph's calibration curve for butyric acid

Concentration of butyric acid (mg/l)	Peak area
1,000	0.23
2,000	0.48
3,000	0.83
4,000	1.11
5,000	1.31

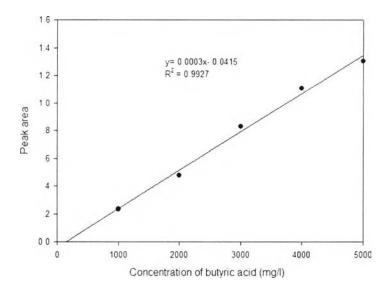


Figure A8 The relationship between concentration of butyric acid and peak area.

Amount of butyric acid =
$$\frac{Peak\ area +\ 0.0415}{0.0003}$$

Table A9 Liquid chromatograph's calibration curve for valeric acid

Concentration of valeric acid (mg/l)	Peak area
1,000	0.21
2,000	0.51
3,000	0.80
4,000	1.19
5,000	1.36

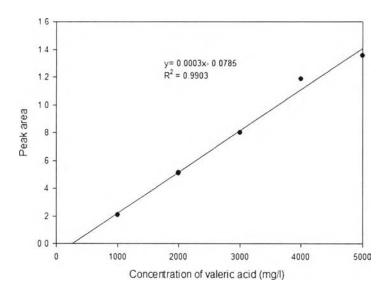


Figure A9 The relationship between concentration of valeric acid and peak area.

Amount of valeric acid =
$$\frac{Peak \ area + 0.0785}{0.0003}$$

Table A10 Liquid chromatograph's calibration curve for ethanol

Concentration of ethanol (mg/l)	Peak area
1,000	0.21
2,000	0.53
3,000	0.78
4,000	1.05
5,000	1.35

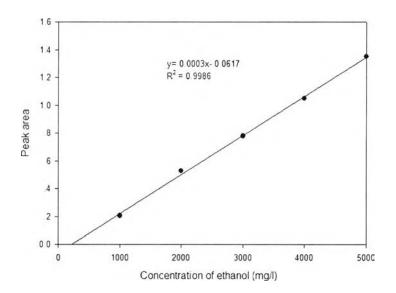


Figure A10 The relationship between concentration of ethanol and peak area.

Amount of et
$$\square$$
 ano $l = \frac{Peak\ area + 0.0617}{0.0003}$

Appendix B Preparation of 1 M NaOH Solution for pH-controlled System

Preparation of NaOH at concentration of 1 M (Molecular weight of acetic acid = 60)

$$= \frac{1 \ mol}{1 \ l} \times \frac{40 \ g}{1 \ mol}$$

$$= 40 \frac{g}{l}$$

Appendix C Volatile Fatty Acids (VFA) Quantification by Distillation Method

C 1. Acetic Acids Stock Solution Preparation for Recovery Factor (f) Determination

Concentration of fresh acetic acid (liquid) = 99.7%

Density of acetic acid = 1.07 g/ml

Molecular weight of acetic acid = 60

Determination of fresh acetic acids concentration in term of molar

$$= \frac{0.997 \text{ L of acetic acid}}{\text{L of solution}} \times \frac{1.07 \text{ g of acetic acid}}{\text{mL of acetic acid}} \times \frac{1 \text{ mol of acetic acid}}{60 \text{ g of acetic acid}}$$

$$= 17.78 \text{ M}$$

Preparation of acetic acid at concentration of 2,000 mg/L

= 2,000
$$\frac{\text{mg of acetic acid}}{\text{L of solution}} \times \frac{1 \text{ mole of acetic acid}}{60 \text{ g of acetic acid}}$$

= 0.0333 M

Dilution of acetic acid

$$N_1V_1$$
 = N_2V_2
 V_1 = N_2V_2/N_1
= $(0.0333x1)/17.78$
= $1.873x10^{-3}$ L

C 2. Standard Sodium Hydroxide (0.1 M) Preparation

Concentration of fresh NaOH (solid) = 99%

Molecular weight of acetic acid = 40

Preparation of acetic acid at concentration of 0.1 M

$$= \frac{0.1 \,\text{mol}}{1 \,\text{L}} \times \frac{40 \,\text{g}}{1 \,\text{mol}} \times \frac{100}{99}$$
$$= 4.04 \,\text{g}$$

C 3. Recovery Factor (f) Determination

Distill 150 ml of 0.0333 M of acetic acid in distillation apparatus Calculate the recovery factor

$$f = \frac{a}{b}$$

where

a = volatile acid concentration recovered in distillate, mg/L

b = volatile acid concentration in standard solution used, mg/L

Find volatile acid concentration recovered in distillate by titration with 0.1 M of NaOH (MW of acetic acid = 60.5)

1)	Distillate	50 ml	NaOH	11.7 ml		
	Used NaOH			=	$11.7x10^{-3}x$	0.1
				4	1.17×10^{-3}	mol
	Acetic acid in	n distillate		=	1.17×10^{-3}	mol
				=	$1.17 \times 10^{-3} \times 10^{-3}$	60.5
				=	0.07	g
	Concentration	n of acetic acid	in distilla	te		
				=	0.07/50	
				=	1.405×10^{-3}	g/ml
				=	1,405	mg/l
2)	Distillate	25 ml	NaOH	5.7 ml		
	Used NaOH			=	$5.7x10^{-3}x0$.1
				₩)	$5.7x10^{-4}$ m	ol
	Acetic acid in	n distillate		=	5.7x10 ⁻⁴ m	ol
				=	$5.7x10^{-4} x$	60.5
				= 1	0.034	g
Concentration of acetic acid in distillate						
				=	0.034/25	
				#	1.368x10 ⁻³	g/ml
				=	1,368	mg/l
	Average			=	1,387	mg/l
	Recovery fac	tor (f)		= 1	1,387/2,00	0
				=	0.693	

CURRICULUM VITAE

Name: Ms. Tasanee Wangmor

Date of Birth: September 03, 1990

Nationality: Thai

University Education:

2008-2012 Bachelor Degree of Engineering in Petrochemical and Polymeric Materials, Faculty of Engineering, Silpakorn University, Nakhon Pathom,

Thailand

Proceedings:

Wangmor, T.; Intanoo, P.; Rangsunvigit, P.; and Chavadej, S. (2014, April 22)
 Effect of Added Cassava Residue on Hydrogen and Methane Production from
 Cassava Wastewater Using a Two-Stage UASB System. <u>Proceedings of the 5nd
 Research Symposium on Petrochemical and Materials Technology and the 20th
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 Thailand.

</u>

Presentation:

Wangmor, T.; Intanoo, P.; Rangsunvigit, P.; and Chavadej, S. (2014,May 7-8)
 Optimization of two-stage UASB system for H₂ and CH₄ production from cassava wastewater with added cassava residue. Paper presented at <u>2014 International</u>
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