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# **APPENDICES**

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### APPENDIX A

### CALCULATION OF CATALYST PREPAPATION

# Calculation for the preparation of the silica-modified aluminas

The silica-modified aluminas in the thesis have 5 weight ratios. AS1, AS2, AS8, AS15, AS30 mean the AIP/TEOS weight ratios that can calculate as follow. Aluminum isopropoxide (AIP, Aldrich,98%+) and tetraethyl orthosilicate (TEOS,Aldrich,99+%) is used as the reactant

If the AS8 is the product, AIP 12.5 g is used for every preparation.

The amount of AIP	=	12.5*0.98	g
	=	12.25	g
The amount of TEOS in the reaction	=	12.25/8	g
	-	1.53	g
The amount of TEOS in this preparation		1.53/0.99	g
	5225	1.55	g

### APPENDIX B

### CALCULATION OF CATALYST PROPERTIES

### BET surface area calculation

From BET equation:

$$\frac{X}{V(1-X)} = \frac{1}{VmC} + \frac{(C-1)(X)}{VmC}$$
 (A.1.1)

Where : X = relative partial pressure of  $N_2$ , P/Po

Po = saturated vapor pressure of  $N_2$  (or adsorbed gas) at the

experimental temperature

P = equilibrium vapor pressure of N<sub>2</sub>

V = volume of gas adsorbed at pressure P, ml. at the NTP/gram

of sample

Vm = volume of gas adsorbed at monolayer, ml. at the NTP/gram

of sample

 $C = \exp(E_1 - E_2/RT)$ 

Where :  $E_1$  = heat of adsorption at the first layer

 $E_2$  = heat of condensation of adsorbed gas on all other layers

Assume  $C \longrightarrow \infty$ , then

$$\frac{X}{V(1-X)} = \frac{1(X)}{VmC} \tag{A.1.2}$$

Let: Vm = Vm'

Vm' = volume of gas adsorbed to form the  $N_2$  complete monolayer

V = volume of gas adsorbed measured by G.C.

X = P/Po

$$\frac{PbV}{273} = \frac{PtV}{T} \tag{A.1.3}$$

Where: V = constant volume

Pb = pressure at 0 C

Pt = pressure at t C

T = 273.15 + t, K

Pb = (273.15/T)Pt = 1 atm

Partial pressure

(A.1.4) 
$$P = [Flow of (He+N_2) - Flow of He] \cdot Pb$$

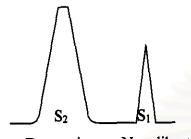
$$Flow of (He+N_2)$$

$$= 0.3 atm$$

 $N_2$  saturated vapor pressure, Po = 1.1 atm = 836 mm.Hg

$$X = P/Po = P/1.1$$

# How to measure V



1 ml./1atm at room temperature

Desorption N<sub>2</sub> calibration area of N<sub>2</sub> area

$$V = \underline{S_2} \cdot \underline{1} \cdot \underline{273.15} \text{ ml./g of catalyst}$$

$$(A.1.5)$$

$$S_1 \quad W \quad T$$

Where: W = weight of sample

$$Vm' = V[1 - [Flow of (He+N2) - Flow of He] / 1.1]$$

$$Flow of (He+N2)$$
(A.1.5)

Where : S = Surface area from literature of  $N_2$ =  $4.373 \text{ m}^2/\text{ml.}$  of  $N_2$ 

So that : Sb =  $4.373.\text{Vm}^{/} \text{ m}^{2}/\text{g cat}$ 

### **VITA**

Mr. Okorn mekasuvandamrong was born on May 29, 1977 in Bangkok, Thailand. He received the Bachelor Degree of Chemical Engineering from Faculty of Engineering, Chulalongkorn University in 1998. He continued his Master's Study at Chulalongkorn University in June, 1998.

