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เทคนิคทางโคมาราโถกราฟี



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**DETERMINATION OF ADSORPTION OF TOLUENE AND ACETONE  
VAPORS ON PERLITE AND PUMICE VOLCANIC ROCKS USING THE  
CHROMATOGRAPHIC TECHNIQUE**

**Miss Vorawan Norasucha**

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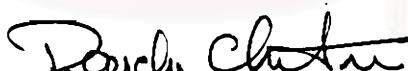
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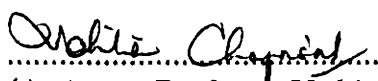
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การศึกษาการดูดซับไอเจือจากของโกลูอินและอะซิโตน บนหินภูเขาไฟชนิดเพอร์ลิต ที่ขยายตัวแล้วและหินพัมมิชที่อุณหภูมิ 40-110 องศาเซลเซียส โดยวิธีทางโครงมาโทกราฟี สามารถคำนวณค่าคงที่สมดุลการดูดซับและค่าคงที่อัตราการดูดซับของระบบจากการวิเคราะห์โครงสร้างที่ได้ด้วยวิธีทางโมเมนต์ ค่าคงที่สมดุลการดูดซับของอะซิโตนบนเพอร์ลิตและพัมมิชมีค่ามากกว่าการณ์ของโกลูอินบนตัวดูดซับชนิดเดียวกัน นอกจากนี้ยังพบว่า ค่าคงที่สมดุลการดูดซับจะแปรผกผันกับขนาดของตัวดูดซับ ในขณะที่ค่าคงที่อัตราการดูดซับของโกลูอินบนตัวดูดซับทั้งสองชนิดจะมีค่ามากกว่าอะซิโตน ปริมาณความร้อนของการดูดซับของอะซิโตนมีค่าสูงกว่าความร้อนแผงของทำความบนและอาจมีค่าสูงถึงสองเท่าของค่าความร้อนแผงของทำความบนแน่น ในขณะที่ค่าปริมาณความร้อนของการดูดซับของโกลูอินจะน้อยกว่าความร้อนแผงของทำความบนแน่น โดยอาจมีค่าเหลือเพียงครึ่งหนึ่งของค่าความร้อนแผงของทำความบนแน่น

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Adsorption of dilute toluene vapor and acetone vapor on expanded perlite and pumice was carried out with chromatographic method at 40-110°C. The adsorption equilibrium constant and the adsorption rate constant for each adsorbent-adsorbate system was determined from the first absolute moment and the second central moment of the corresponding chromatogram, respectively. The equilibrium constants for acetone on both perlite and pumice were greater than that for toluene on the same adsorbents. In addition, the equilibrium constant varied inversely with the particle sizes. While the adsorption rate constants for toluene on both adsorbents were greater than that for acetone. The heats of adsorption for acetone were greater than the heat of condensation up to two folds. While the heats of adsorption for toluene were than the condensation heat down to a half of it.



สถาบันวิทยบริการ  
จุฬาลงกรณ์มหาวิทยาลัย

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## NOMENCLATURE

$a_s$	specific surface area, ( $\text{cm}^2/\text{g}$ )
$c$	sorbate concentration ( $\text{mol}/\text{cm}^3$ )
$C$	constant value
$c_0$	initial sorbate concentration ( $\text{mol}/\text{cm}^3$ )
$d$	pore diameter, (cm)
$d_p$	particle diameter, (cm)
$D_{AB}$	binary molecular diffusivity ( $\text{cm}^2/\text{sec}$ )
$D_K$	Knudsen diffusivity, ( $\text{cm}^2/\text{sec}$ )
$D_L$	axial dispersion ( $\text{cm}^2/\text{sec}$ )
$D_m$	molecular diffusivity ( $\text{cm}^2/\text{sec}$ )
$D_p$	pore diffusivity, ( $\text{cm}^2/\text{sec}$ )
$\Delta H$	heat of adsorption (J/mol)
$\Delta P$	pressure of packed column
$k_0$	overall mass transfer coefficient ( $\text{cm/sec}$ )
$k_f$	external fluid film mass transfer coefficient ( $\text{cm/sec}$ )
$K$	adsorption equilibrium constant defined in term of sorbate pressure
$K_a$	adsorption equilibrium constant for unsaturation isotherm
$K_i$	adsorption equilibrium constant defined in term of sorbate pressure of component i
$K_L$	langmuir adsorption equilibrium constant
$L$	adsorbent bed length (cm)
$M$	molecular weight
$p_i$	partial pressure of component i
$P$	total pressure
$P_c$	critical pressure
$q_i$	amount of adsorbate adsorbed of component i
$\bar{q}$	value of q average over crystal and pellet
$q^*$	equilibrium value of q
$q_{s,i}$	saturated limit of $q_i$
$r$	radius of particle, (cm)
$R$	gas constant
$R_p$	adsorbent pellet radius (cm)
$t_R$	weighted mean residence time (sec)
$T$	temperature, (K)
$T_c$	critical temperature, (K)
$v$	interstitial velocity of carrier gas, (cm/min)
$v_0$	superstitial velocity, (cm/min)
$y_i$	mole fraction

## GREEK LETTERS

$\epsilon$	porosity of adsorbent bed
$\lambda$	mean free path,
$\mu$	viscosity of fluid, ( $\text{g}/\text{cm}\cdot\text{sec}$ )
$\rho$	fluid density, ( $\text{g}/\text{cm}^3$ )

$\rho_b$	bulk density of adsorbent bed, (g/cm <sup>3</sup> )
$\rho_p$	particle density, (g/cm <sup>3</sup> )
$\rho_s$	solid density, (g/cm <sup>3</sup> )
$\sigma^2$	second moment of chromatogram
$\tau$	tortuosity factor

#### DIMENSIONLESS GROUPS

Pe	Peclet Number
Re	Reynolds Number
Sc	Schmidt Number
Sh	Sherwood Number